

Basis of Design Report for Fence Line Groundwater Extraction, Treatment, and Discharge System at Site 6A - Southern Area

Naval Weapons Industrial Reserve Plant Calverton, New York



Mid-Atlantic Division Naval Facilities Engineering Command

Contract Number N62470-08-D-1001 Contract Task Order WE63

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BASIS OF DESIGN REPORT FOR FENCE LINE GROUNDWATER EXTRACTION, TREATMENT, AND DISCHARGE SYSTEM AT SITE 6A – SOUTHERN AREA

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ACRONYMS AND ABBREVIATIONS

bgs below ground surface CFM cubic feet per minute

CLEAN Comprehensive Long-Term Environmental Action Navy

CMS Corrective Measures Study

CTO Contract Task Order
DCA 1,1-Dichloroethane
DCE 1,1-Dichloroethene

ERP Environmental Restoration Program

gpm gallon per minute

GWTP Groundwater Treatment Plant

HP horsepower

in-WC inches water column

MCL Maximum Contaminant Level

mg/L milligrams per liter
msl mean sea level

µg/L microgram per liter

NAVFAC Naval Facilities Engineering Command
NWIRP Naval Weapons Industrial Reserve Plant

NYSDEC New York State Department of Environmental Conservation

OU5 Operable Unit No. 5

PRAP Proposed Remediation Action Plan

PVC Polyvinyl chloride

RCRA Resource Conservation and Recovery Act

ROD Record of Decision

SOB Statement of Basis for Remedy Selection

TCA 1,1,1-Trichloroethane
Tetra Tech Tetra Tech, Inc.

UIC Underground Injection Control

USEPA United States Environmental Protection Agency

VOC volatile organic compound

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1.0 INTRODUCTION

This Basis of Design Report was prepared to develop and identify the components for a groundwater extraction, treatment, and discharge system (Fence Line Treatment System) for reducing or eliminating the flow of volatile organic compound (VOC)-impacted groundwater migrating from the Site 6A – Fuel Calibration Area to beyond the current facility property line (Fence Line) at Naval Weapons Industrial Reserve Plant (NWIRP) Calverton, Suffolk County, Long Island, New York (Figures 1-1 and 1-2.) This report was prepared by Tetra Tech Inc., (Tetra Tech) for Naval Facilities Engineering Command (NAVFAC) – Mid-Atlantic under the U.S. Navy's Comprehensive Long-Term Environmental Action Navy (CLEAN) Contract No. N62470-08-D-1001, Contract Task Order (CTO) WE63. This project is being conducted in accordance with the Navy Environmental Restoration Program (ERP) Operable Unit No. 5 (OU5) Record of Decision (ROD) and the New York State Department of Environmental Conservation (NYSDEC) Resource Conservation and Recovery Act (RCRA) permit number 1-4730-00013/00001-0 Statement of Basis for Remedy Selection (SOB) that is expected to be finalized in May 2012.

1.1 BACKGROUND

The Site 6A-Southern Area Groundwater consists of chlorinated VOC-impacted groundwater that originated at Site 6A – Fuel Calibration Area on NWIRP Calverton property and extends southeast to the Peconic River. The primary site-related chlorinated VOCs consist of 1,1,1-trichloroethane (TCA), 1,1-dichloroethane (DCA), 1,1-dichloroethene (DCE), and chloroethane. Other VOCs are also present, but at lower concentrations and/or are not detected as frequently. The isoconcentration contour map for DCA is presented in Figure 1-3 and a cross section for the DCA plume is presented in Figure 1-4. DCA is typically the highest concentration VOC detected at each location and represents approximately 62 to 75 percent of the total VOCs in groundwater. Also, the limits of the DCA contours define the extent of other site-related VOC contamination. This data is based on temporary and permanent groundwater sampling events conducted between 1994 and December 2011.

In 2009 and 2010, source area excavations were conducted at Sites 6A - Fuel Calibration Area and 10B – Engine Test House that removed most or all of the petroleum- and solvent-contaminated soil. Groundwater monitoring is currently in progress to determine the effectiveness of the remedial action, and if additional action is required. If the Site 6A and 10B excavations are not effective in mitigating a continuing source of groundwater contamination, the operation of the Fence Line Treatment System identified in this report would be extended. The Operable Unit No. 5 ROD includes a provision for supplemental treatment at the source area(s) that would be addressed under a separate action.

In 2010 and 2011, the Navy conducted a pilot-scale pumping test and a pilot-scale BioStudy in the Fence Line Area to support the development of a Corrective Measures Study (CMS) (Tetra Tech 2011). The results of these studies and supplemental groundwater investigations conducted from April to June 2011 are presented in the March 2012 Data Summary Report, Enhanced Bioremediation Pilot Test (Tetra

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Tech, 2012). Because this testing was being conducted in the planned area of the Fenceline Groundwater Treatment System and could interfere with the operation of the planned treatment system, the biostudy testing was ended early.

In March 2011, the Navy presented a CMS that included alternatives for the Southern Area Groundwater. For the evaluation, the CMS divided the plume into five areas including two on-property areas (Source Area and Fence Line Area), and three off-property, downgradient areas (Offsite High Concentration Area, Offsite Low Concentration Area, and Peconic River Area) (Figure 1-5). For the OU5 ROD, the term "Offsite" was deleted from the two off-property area descriptions. In October 2011, the public comment period for the Navy's Proposed Plan, and in November 2011, the public comment period for the NYSDEC RCRA Permit Modification request were initiated. The public comment period for both the Proposed Plan and RCRA Permit Modification request ended on January 17, 2012. The Navy's OU5 ROD and NYSDEC RCRA Permit Modification are being prepared with an estimated completion date in May 2012. These decision documents identify a groundwater extraction, treatment, and discharge system to be installed at the Fence Line Area. A long-term monitoring plan for this system and other portions of the Site 6A-Southern Area Groundwater are being conducted under a separate action.

1.2 OBJECTIVE

The objective of the groundwater extraction, treatment, and discharge system is as follows:

• Reduce or eliminate the migration of VOC-impacted groundwater from Site 6A at the southern boundary of the current NWIRP Calverton property line (Fence Line Area).

1.3 REPORT ORGANIZATION

This report is divided into five sections. Section 1.0 is this introduction. Section 2.0 provided the design basis. The process description is provided in Section 3.0. Permitting requirements are presented in Section 4.0 and the schedule is presented in Section 5.0.

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2.0 DESIGN BASIS

This section provides the development of the extraction well capture zone, design of the extraction well network, and development of extracted water quality and treatment goals.

2.1 CAPTURE ZONE DEVELOPMENT

The location of the groundwater extraction well network is based on the isoconcentration contour maps presented in Figures 1-3 and 1-4 and potentiometric surface maps that indicate a southeasterly groundwater flow in this area (Appendix A). Since groundwater flow is to the southeast, the design width of the plume is based on the line perpendicular to the groundwater flow at its approximate center line where the plume crosses the southern property fence line (Fence Line Area).

The VOC-impacted groundwater at the fence line is estimated to be approximately 800 to 1,000 feet wide and 40 feet thick (5 micrograms per liter [μ g/L] isoconcentration contour. Variability in the width of the overall plume is based primarily on the estimated northeastern edge of the 5 and 50 μ g/L DCA isoconcentration contours. VOC groundwater data in this area is limited and the data is from temporary wells installed in 2008 and 2009 and monitoring wells along River Road. The core of the plume (VOCs greater than 500 μ g/L DCA) is approximately 200 feet wide and 10 feet thick. An evaluation of groundwater data collected in 2011 indicates that the axis of the core plume has shifted approximately 100 feet to the west.

2.2 EXTRACTION WELL NETWORK

The design groundwater extraction rate for the containment system is developed using target capture zones, the hydraulic gradient, and the aquifer characteristics. The estimated average width and thickness of the plume in this area are 900 feet and 40 feet, respectively. An evaluation of 2008 to 2011 quarterly water level measurements in the area was used to develop the hydraulic gradient. The hydraulic gradient was measured to vary from 0.002 to 0.004, which appeared to correlate with seasonal precipitation events, and the annual average hydraulic gradient is 0.003. Pumping tests conducted in the Fence Line Area in 2010 were used to develop the aquifer characteristics. The calculated hydraulic conductivity of the aquifer was 186 feet per day (Tetra Tech, 2011). Under these conditions, the average calculated groundwater flow through rate through the Fence Line Area is 104 gallons per minutes (gpm). For design purposes, an average flow rate through the Fence Line Area of 100 gpm will be used.

To account for uncertainty with the groundwater flow through rate, a 40 percent factor will be applied or a potential maximum hydraulic rate of 140 gpm. For design purposes, two extraction wells (EW-01 and -02), approximately 100 feet apart, will pump at a combined rate of 100 to 140 gpm. These wells will be located on the east-west perimeter road and north-south dirt road (Appendix E - Drawing C-3). During operation, if a shift in the plume occurs, the pumping rate from each of the wells can be varied to best intercept the plume. As discussed below, the infiltration galleries will be located side gradient of the extraction wells so as to not interfere with the extraction wells.

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A summary of the hydraulic properties is presented in Table 2-1.

Table 2-1 Hydraulic Calculation Summary

Parameter	Value
Plume Width (feet)	900 (800 to 1,000)
Plume Thickness (feet)	40
Hydraulic Conductivity (feet/day)	186
Hydraulic Gradient (foot-V/foot-H)	0.003 (0.002 to 0.004)
Calculated Plume Flow Through Rate	104
(gallons per minute)	104
Design Extraction Rate (Mean/Max)	100/140
(gallons per minute)	100/140
Number of Extraction Wells	2

2.3 EXTRACTION WELL QUALITY AND TREATMENT GOALS

Estimated groundwater contaminant concentrations are based on monitoring well data and the location of groundwater extraction wells, see Table 2-2. Additional well-specific detail is provided in Appendix A. The DCA plume has been extensively characterized and provides a method for evaluating VOC mass flux rate through the area. The estimated annual average DCA mass flux rate is 22 pounds per year. The DCA mass flux is used as the basis for determining the mean concentration of VOCs to be captured by the Fence Line Treatment System extraction wells.

To estimate the concentration of other VOCs present in the groundwater extraction wells, data from the December 2010 sampling event for monitoring well SA-PZ-138I1 was used (see Appendix A). In this well, DCA represents approximately 63 percent of the total VOCs, and TCA, DCE, and chloroethane represent approximately 15 percent, 3.6 percent, and 18 percent of the total VOCs, respectively. In other areas wells, DCA represents up to approximately 75 percent of the total VOCs, and in several wells, chloroethane is absent. Treatment goals for the site-related VOCs are based on discharge to a Class GA groundwater aquifer, a potential current and future source of potable water and associated goals of New York State Department of Health maximum concentration levels (MCLs). The highest of July, October, and December 2010 data from monitoring well SA-PZ-138I1 is also used as the design basis for the maximum concentration of VOCs in the groundwater extraction wells.

Iron and manganese are also naturally present in site groundwater. The Site 6A-Southern Area includes a series of wetland and subsurface peat formations, which allow the formation of reduced pH and anaerobic conditions in the groundwater. Under these conditions, iron, manganese, and arsenic naturally found in site soils can become soluble. In the Fence Line Area, iron concentrations in the groundwater range from approximately 200 μ g/L to 3,300 μ g/L and manganese concentrations range from approximately 200 μ g/L. Near the Peconic River, the ultimate discharge point for site groundwater, natural iron and manganese concentrations are approximately 13,700 μ g/L and 185 μ g/L, respectively (Tetra Tech, 2011).

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During the pumping test conducted in the Fence Line Area in 2010, iron and manganese concentrations in the extracted groundwater were approximately 750 µg/L and 1,300 µg/L, respectively (Tetra Tech 2011). The higher iron and manganese concentrations are generally in the areas of higher VOC concentrations, but a direct correlation between these metals and VOCs is not apparent. For design purposes, the average iron and manganese concentrations of approximately 1,200 to 1,500 µg/L will be used, respectively. At these concentrations, if the iron and manganese are allowed to oxidize and precipitate in the treatment system, some interference (silting and plugging) to the treatment units and infiltration galleries/injection wells would be anticipated. The maximum average and manganese concentrations are assumed to be twice the average concentrations. Because iron and manganese is naturally present in the groundwater and is present at higher concentrations in downgradient groundwater, the design assumes that there will be no discharge requirements for soluble iron and manganese.

The groundwater extraction, treatment, and discharge system is intended to operate until the mass of VOCs leaving the NWIRP facility property line has been eliminated or significantly reduced. The treatment duration will be in part based on the effectiveness of the 2009/2010 Source Area remedial actions in reducing or eliminating a continuing source of contamination, the groundwater seepage velocity, VOC retardation on soils, and biodegradation. Based on these factors, the treatment system is estimated to operate for two to eight years, with a geometric mean estimate of four years.

Shutdown criteria for the treatment system are as follows:

• The concentration of individual site-related chlorinated VOCs entering the treatment system extraction wells is less than 10 µg/L and the maximum concentration of individual site-related chlorinated VOCs in fence line monitoring wells is less than 50 µg/L. This condition corresponds to an approximate 90 percent reduction in total VOCs and 95 percent reduction in individual VOCs leaving the property over current conditions.

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TABLE 2-1 DESIGN BASIS FENCE LINE GROUNDWATER EXTRACTION, TREATMENT, AND DISCHARGE SYSTEM NWIRP CALVERTON, NEW YORK

Design Parameter	Daily Maximum or Range	Annual Mean	Treatment Goal
Design Flow rate, gpm	100 to 140	100	
Temperature, C	8 to 15	11	
pH, S.U.	5.5 to 6.5	6.5	5.5 to 9.0
Constituents (µg/L)			
Iron	200 to 2,400	1,200	
Manganese	200 to 3,000	1,500	
1,1,1-Trichloroethane	260	11	5
1,1-Dichloroethane	1,100	51	5
1,1-Dichloroethene	65	3	5
Chloroethane	320	13	5
Benzene	4.4	0.2	5
1,4-Dichlorobenzene	16	1	5
1,3-Dichlorobenzene	4	0.2	5
1,2-Dichlorobenzene	6.4	0.3	5
Isopropylbenzene	11	0.4	5
1,2,4-Trichlorobenzene	14	1	5
Total VOC	1,801	80	
Organic Loading	(pounds/day)	(pounds/year)	
DCA Mass Flux Rate	1.3	22	
Total VOC Mass Flux Rate	2.2	35	

--- No value or goal.

μg/L – micrograms per liter.

VOC – volatile organic compound.

DCA – 1,1-dichloroethane.

gpm – gallons per minute.

S.U. – Standard Unit.

C – Celsius.

3.0 PROCESS DESCRIPTION

This section describes the processes that will be used for the treatment of groundwater at the site and presents the design basis for these processes.

3.1 GENERAL DESCRIPTION

The Groundwater Treatment Plant (GWTP) consists of extraction wells, a treatment system, and a discharge system that will be located adjacent to the southern property line. A GWTP building will be located on the perimeter road, north of the intersection of Grumman Boulevard and River Road and near the middle of the groundwater extraction network. See Drawings G-0 and C-1 (Appendix E) for GWTP location and site layout plans. The treatment system will consist of air stripping and pressure filtration, and will be housed in a pre-fabricated metal building. The groundwater extraction system will consist of two recovery wells, and the treated effluent will be returned to the aquifer via two infiltration galleries with injection wells.

3.2 GWTP SYSTEM OVERVIEW

The process flow diagram is presented on Drawing PFD (Appendix E). Design flow rates and stream-specific VOC concentrations through the groundwater treatment processes are also presented. VOC-contaminated groundwater will be pumped from the two groundwater extraction wells CA-FL-EW-01 and -02 (EW-01 and -02) to the top of the tray air stripper AS-200 using two self-priming horizontal extraction pumps P-110 and P-120. In the tray air stripper, the VOCs will be removed from the groundwater by a countercurrent flow of air from blower B-200 and be transferred to the vapor phase. Based on a comparison of annual and maximum loadings of VOCs with annual and short-term NYSDEC DAR-1 analysis, off-gas treatment will not be required (See Appendix B).

Groundwater will cascade down the air stripper trays and will collect at the bottom of the air stripper in a sump that is integral to the air stripper equipment. Horizontal centrifugal pumps P-210 and -220 will transfer the treated water from the air stripper to dual 25-micron cartridge pressure filters PF-310 and -320, for removal of precipitates (oxidized iron). The filtered water will be discharged to infiltration galleries and injection wells CA-FL-IW-01 and -02 (IW-01 and -02).

The iron and manganese in the raw groundwater are in a soluble, reduced oxidation state (ferrous iron and divalent manganese) consistent with the anaerobic condition and reduced pH characteristic of site groundwater. The rate of oxidation of iron and manganese is a function of pH of the process water. The optimal pH for the oxidation for iron is greater than 7.5 SU iron and for manganese is greater than 9.5 SU. Therefore, air stripping may result in some oxidation of iron from the ferrous to the ferric state and subsequent precipitation as iron hydroxide, but minimal oxidation of manganese should occur.

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To minimize the formation of iron hydroxide precipitates, a polyphosphate will be metered into the incoming groundwater to sequester the soluble iron. The effectiveness of the metal sequestering in completely preventing precipitate formation is uncertain.

During operation of the GWTP, quarterly cleaning of the air stripper trays, monthly changeout of the cartridge filters, and annual cleaning of the infiltration galleries/injection wells are assumed. The air stripper will be designed to allow access to the trays and the infiltration gallery and injection wells will also be equipped with cleanouts. Any water that is collected in the building sump will be filtered and treated in the air stripper.

3.3 DESIGN FLOW AND INFLUENT CONCENTRATIONS

The groundwater treatment system is designed to process an average flow of 100 gpm and a maximum flow of 140 gpm. Table 3-1 summarizes the design influent and effluent concentrations and serves as the basis for design of the treatment system. The Maximum Influent Design concentrations are potential short-term (e.g., 1 to 3 months) conditions that may occur during startup. The maximum flow rate at this time would be 70 to 100 gpm and the system must achieve the Maximum Design Effluent Criteria. Over the long-term, the VOC concentrations are anticipated to decrease to the Mean Design Influent concentrations. At that time, the system flow rate may be increased to 140 gpm, and the system must achieve the Mean Design Effluent Criteria.

Table 3-1 Design Parameters

Parameter	Design Influer	nt Conditions	Design Effluent Criteria	
	Maximum	Mean	Maximum	Mean
Temperature, C	11	11	NA	NA
pH	6	6	NA	NA
Iron Total, μg/L	2,400	1,200	NA	NA
Manganese Total, μg/L	3,000	1,500	NA	NA
1,1,1-Trichloroethane, µg/L	260	11	2.5	1
1,1-Dichloroethane, µg/L	1,100	51	2.5	1
1,1-Dichloroethene, µg/L	65	3	2.5	1
Chloroethane, µg/L	320	13	2.5	1
Benzene, µg/L	4.4	0.2	2.5	1
1,4-Dichlorobenzene, µg/L	16	1	2.5	1
1,3-Dichlorobenzene, µg/L	4	0.2	2.5	1
1,2-Dichlorobenzene, µg/L	6.4	0.3	2.5	1
Isopropyl Benzene, μg/L	11	0.4	2.5	1
1,2,4-Trichlorobenzene, µg/L	14	1	2.5	1
Total Target VOC, μg/L	1,801	80	NA	NA

NA – Not Applicable

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3.4 GROUNDWATER EXTRACTION SYSTEM

The groundwater extraction system consists of two 10-inch stainless steel casing extraction wells, CA-FL-EW-01 and -02, with 20-foot long, 30-slot (0.030 inch) stainless steel high flow screens and an approximate 14 by 20 US Sieve gravel pack. During installation of the wells, a pilot hole will be drilled, and the based on grain-size analysis of the formation material, the gravel pack design may be modified. The bottom of the well screens will be set to the top of the clay unit present at approximately 45 to 50 feet bgs. The wells will be completed with a bentonite seal, and bentonite/cement grout, and a stickup protective casing.

Low level switches will be provided in the wells to protect the extraction well pumps. The two wells, approximately 100 feet apart, will each be used to extract 50 to 100 gpm of groundwater. These wells will be located on the east-west perimeter road and north-south dirt road (Appendix E - Drawings C-2 and C-3). During operation, if a shift in the plume occurs, the pumping rate from each of the wells can be varied to optimally intercept the plume. Groundwater is present at a depth of approximately 1 to 4 feet bgs (34 to 36 feet mean sea level [MSL]). During operation, the water level within the wells will drop 4 to 6 feet (approximately 28 to 32 feet MSL). The piping within and from the extraction well will be carbon steel and then schedule 80 polyvinyl chloride (PVC). The piping will be sloped toward the extraction wells to prevent the buildup of gases within the piping. The ground surface over the transfer piping may be mounded to minimize trench excavation depth and maintain 3.5 feet of soil cover for freeze protection. The suction down pipe in the well will extend 20 feet below the static water table.

The groundwater will be extracted using a horizontal self-priming centrifugal pump (P-110) and inline spare (P-120), located within the treatment building (pump suction elevation of 40.5 feet MSL) (PID-1). Each pump will be capable of providing an operating lift of 18 feet (12.5 vertical feet plus an additional 5.5 feet to account for pressure drops within the suction piping). During startup, the static lift would be approximately 6.5 feet. Priming water will be available at the plant to assist with startup or after an extended shutdown. Operation of the pump will be on-off-auto. Normal operation will be in the auto mode, with the following interlocks:

- HOA P-110 and -120 (Hand-Off-Auto pump start, with push button start in Auto mode [overrides FSL-110], and pump selector switch)
- LSL-110 and LSL-120 (low-low level in the extraction wells, shuts down GWTP, alarm, manual restart) (20.5 feet MSL)
- FSL-110 (low flow at pump P-110/120 discharge, shuts down GWTP, alarm, manual restart) (15 gpm)
- B-200 (blower operation, starter interlock, blower must be running to operate P-110/120)

Within the treatment building, the suction piping will be plumbed so that groundwater can be extracted from both wells simultaneously by a single pump at a maximum combined flow rate of 100 gpm. Pumps P-110 and P-120 will be horizontal centrifugal self-priming configuration, with a 5 horsepower (HP), 460

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volt, 3-phase motor. The pumps will discharge to the top of the air stripping system. Full-port ball-valves will be provided on the suction piping of the pumps, the pressure drop across these valves will be minimal when the valves are fully open, and these valves will be primarily used as isolation valves, but will also provide minimal control for balancing the flow between the two extraction wells. Flow meter FM-110 will be used to monitor flow rates and shut down the system in the event of insufficient or no water flow. Manual Flow Control Valve (FCV-110) will be used to control the system flow rate.

3.5 AIR STRIPPING SYSTEM

The air stripper AS-200 will be of the tray-type unit, capable of effectively treating 100 gpm of groundwater at the maximum groundwater contaminant concentrations to achieve effluent concentrations equal to 50 percent of MCLs (PFD and PID-2). This unit will also be sized to provide a maximum hydraulic capacity of 140 gpm, but at reduced VOC concentrations in the groundwater. The air stripper (AS-200), the blower (B-200), and the effluent/injection pumps (P-210 and -220) will be mounted on a single skid. The treated groundwater that passes through the air stripper trays will collect in a sump (minimum 250 gallons) that is integral to the air stripper and will be subsequently pumped out. The water level in the air stripper sump will be used to control the horizontal centrifugal pumps P-210 and P-220, with variable frequency drive, 5.0 HP, 460 volts, 3-phase motors. One of these pumps will normally operate and the second pump will serve as an inline spare. Normal operation will be in the auto mode, with the following interlocks:

- HOA P-210 and -220 (Hand-Off-Auto pump start, with push button start in Auto mode and A/B selector switch)
- LSL-200 and LSH-200 (start and stop P-210 or -220)
- LSLL-200 and LSHH -200 (low-low or high-high level shut down the GWTP, alarm, manual restart)
- LC-200 (controls the frequency on P-210 or -220 drive units, operation based on level in the air stripper sump (corresponding minimum flow rate of 15 gpm and maximum flow rate of 150 gpm)

The air stripper blower B-200 will be a centrifugal-type with 7.5 HP, 460 volts, 3–phase motor. The blower will be equipped with an inlet silencer and filter. The blower will be capable of producing approximately 900 cubic feet per minute (CFM). The final speed rates will be determined during blower selection based on achieved short-term and long-term VOC removal goals. The blower discharge pressure will be monitored by high and low pressure switches and the flow rate will be monitored by a mass flow meter. This flow measurement will be transmitted to the control panel. The air stripper, blower, injection wells and associated controls will be a package system.

Normal operation will be in the auto mode, with the following interlocks:

HOA-B200 (Hand-Off-Auto, with push button start in Auto mode[overrides PSL 200])

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• PSL 200 and PSH 200 (low pressure and high pressure switches on B-200, shut down the GWTP, alarm, manual restart) (2 inches and 10 inches water column [in-wc])

3.6 PRESSURE FILTER SYSTEM

The water from the air stripper sump will be pumped through two parallel bag filter vessels (PF-310 and 320) and then injected into the aquifer via two infiltration gallery-injection well combination (PID-3). The bag filters will be sized for 25 microns and will be pleated to maximize the dirt holding capacity of the filter bags. The bag filters are sized based on solids loading and a bag change out frequency of once per month or less. The differential pressure across the multi-bag filter vessels will be automatically monitored using a differential pressure switch. When a high differential pressure is indicated (e.g., 15 PSI), the operator will be notified by an alarm and the GWTP will be shutdown in order to replace the spent bag filters. Based on an influent iron concentration of 1,200 µg/L and assuming all the soluble iron is converted and removed as iron hydroxide following oxidation, it is estimated that the bag filters have to be replaced every four weeks. As previously discussed, polyphosphates will be used to minimize iron oxidation and precipitation and less frequent change outs are anticipated. PF-310 and -320 operate as flow through units. Normal operation will be in the auto mode, with the following interlocks:

• PDSH-300 (Particulate Filter PF-310 and -320) high differential pressure, shut down the GWTP, alarm, manual restart) (15 PSI)

3.7 DISCHARGE SYSTEM

Treated groundwater will be discharged to one or both injection systems located approximately 500 feet east and west of the groundwater extraction wells (Appendix E - Drawing C-3). The injection systems will consist of dual 200-foot perforated pipe installed within a gravel bed and a 50-foot vertical injection well. Each system will normally be capable of discharging 100 gpm of treated groundwater. The injection wells will be equipped with a high level switch to indicate potential fouling of the injection piping and/or seepage of treated groundwater to the surface (PID-3). The ground surface over the transfer piping may be mounded to minimize trench excavation depth and maintain 3.5 feet cover depth. Normal operation will consist of the following interlock:

LSH –IW1 and –IW2 (high-high level in injection wells shuts down GWTP, alarm, manual restart)
 (38 feet MSL)

3.8 MISCELLANEOUS SYSTEMS

<u>Building Sump:</u> A 30-gallon sump and submersible pump (P-500) will be provided for the facility that will transfer any water that collects in the sump to the air stripper influent line. The submersible pump with be rated at 10 gpm at 15 feet TDH, with a ½ HP, 120 volts, single phase motor, and integral float switch will be provided. The pump discharge will be equipped with a filter to control the discharge of solids to the

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air stripper. The sump will be provided with a high-level switch which will shut down the treatment plant in the event of a sump high level condition. Normal operation is in auto mode, with the following interlock:

LSHH-500 (high-high level in sump, shut down the GWTP, alarm, manual restart)

Polyphosphate System: Polyphosphate will be injected to the incoming groundwater to sequester the soluble iron and minimize precipitation in the air stripper and reinjection systems. Approximately 2 milligrams per liter (mg/l) of the polyphosphate will be used to keep the iron and manganese sequestered. For a nominal treatment plant flow rate of 100 gpm, a dosage of 2 mg/L translates to a usage of 1.4 gallons per day (4 milliliters per minute) for a polyphosphate with a specific gravity of 1.39. Therefore, a 55-gallon drum of polyphosphate will last approximately 40 days. The quantity to be stored on-site can be decided based on usage during start-up (currently anticipated to be 4 drums). The drums will be stored on a spill pallet. The polyphosphate will be dosed with a diaphragm metering pump capable of a flow rate of up to 5 gallon per day (15 milliliter per minute), two pumps will be provided (P-510) of which one will be a shelf spare. The polyphosphate will be fed into the 3-inch air stripper feed line through an injection quill and static mixer setup. Operation of the pump will be interlocked with operation of the groundwater extraction pump.

<u>Priming System:</u> The treatment plant utilizes self-priming pumps to transfer groundwater from the recovery wells to the air stripper. A 175-gallon polyethylene tank will be provided to store water which can be used to prime the suction lines in the event of an extended pump shutdown or loss of pump prime.

3.9 PLANT LAYOUT

The layout plan for the GWTP is shown on Appendix E - Drawing M-1. The groundwater influent pipes from the recovery wells enter the GWTP building through the floor in the northwest corner. The groundwater is then pumped to the top of the shallow tray air stripper from where it is pumped through bag filters and ultimately back into the aquifer. The extraction well pumps, air stripper, and bag filters will be located on the north side of the building. The building will be provided with a sump and submersible pump. The polyphosphate feed system will be located adjacent to the extraction well pumps and the air stripper.

3.10 INSTRUMENTATION AND CONTROL

The components of the groundwater treatment system will be monitored by appropriate instrumentation. The system will be equipped with flow meters, pressure indicators, differential pressure transmitters and pressure and level switches. The pumps and blower will be monitored by local pressure indicators and pressure switches. The bag filters will be equipped with local pressure indicators and a differential pressure transmitter. The differential pressure transmitters will include a high pressure cutoff. A flow meter will be provided on the influent line to monitor and record the volume and flow rate of groundwater being processed through the plant. The entire system will be monitored by a PLC-auto-dialer system.

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The auto-dialer will be set to call out numbers based on a set hierarchy and for the following alarm conditions:

- Extraction Well Low Level
- Extraction Well Pump Low Flow
- Blower Low or High Pressure
- Bag Filter High Differential Pressure
- Air Stripper Sump Low and High Level
- Building Sump High Level
- Injection System High Level

In each of the above cases the system will be shut down and the auto-dialer will be activated.

The alarm has to be acknowledged at the control panel located at the building prior to restarting the system. The system is designed to be operated on a long-term basis as an unmanned operation equipped with an auto dialer. The system will operate as follows:

- 1. The water level in the extraction and injection wells will be monitored by a level element.
- 2. The extraction well flows will be monitored by a flow meter.
- 3. The air stripper unit will be skid mounted and is provided with the stripper trays, a blower, and injection pumps (with variable frequency drives), and control panel. Injection well pumps will be controlled by the water level in the air stripper sump.
- 4. Treated water will be pumped through particulate filters that are provided with a differential pressure indicator and transmitter.
- 5. In the event of an alarm condition or plant shutdown, the auto dialer will dial an on-call operator.
- 6. The following interlocks will be provided:
 - Influent pumps do not turn on prior to startup of the air stripper blower.
- 7. In the event of a blower failure, the entire system will be shutdown.

Local control panels will be provided with MAN-OFF-AUTO switches for the pumps and blower. The pumps and blowers can be run locally by setting and holding the switch in the MAN position. In the AUTO mode, push button start buttons will be used.

3.11 TREATMENT BUILDING DESCRIPTION

The treatment system equipment will be housed in a pre-fabricated building. Soil data for the foundation design is provided in Appendix D. The GWTP will be housed in a 35-foot long x 25-foot wide x 14-foot tall metal building. The east side of the building is equipped with an 8-foot wide overhead (roll-up) door and a 3-foot wide by 7-foot tall utility door. An electrical transformer installed in a vault will also be located outside the building – on the northwest corner. The building will be provided with lighting, security

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system, work space, telemetry system, electric heaters and vent fans. Equipment will be installed on a pad, and the building will be provided with a sump. The building floor will be sloped towards the sump. The building will be provided with a fire and burglary control panel. In the event of a break-in, the auto dialer will be activated.

3.12 MONITORING WELL PROGRAM

A monitoring well program to evaluate extraction well capture zones and groundwater cleanup will be prepared under separate cover. This program will evaluate the existing monitoring well network and the need to install additional monitoring wells, as well the frequency of testing and parameters to be monitored (e.g., water levels and VOC concentrations)

4.0 PERMITING REQUIREMENTS

The Navy will contact the NYSDEC and United States Environmental Protection Agency regarding permitting submittals. Since the work is being conducted on federal government property under CERCLA authority, permits are not required. Anticipated specific submittals and reporting activities are anticipated to consist of the following.

- Notifications to NYSDEC that construction is being conducted in the area of wetlands and the Peconic River.
- Notifications to NYSDEC that groundwater extraction and discharge activities will be conducted.
- Notification to NYSDEC that off gas containing VOCs will be discharged to the atmosphere.
- Notification to the United States Environmental Protection Agency (USEPA) that treated groundwater will be discharged under an Underground Injection Control (UIC) program.

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5.0 SCHEDULE

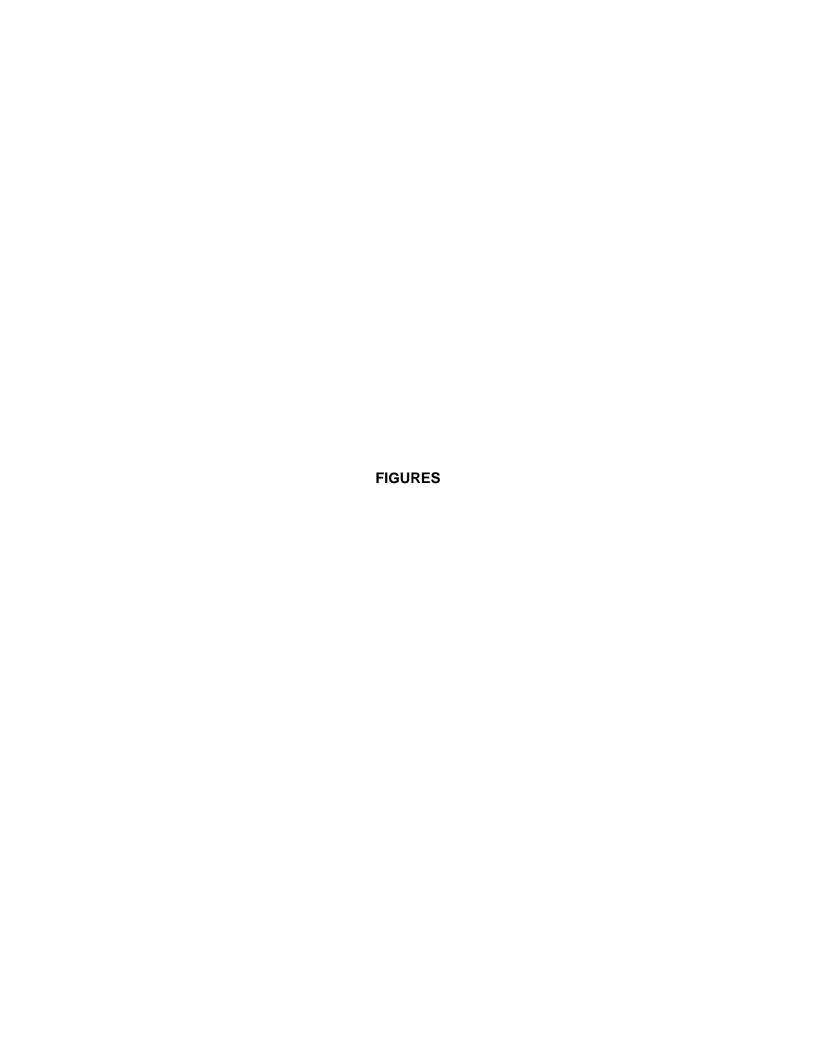
The estimated construction and startup schedule is dependent on finalizing the Navy's ROD and the NYSDEC RCRA Permit by April 30, 2012.

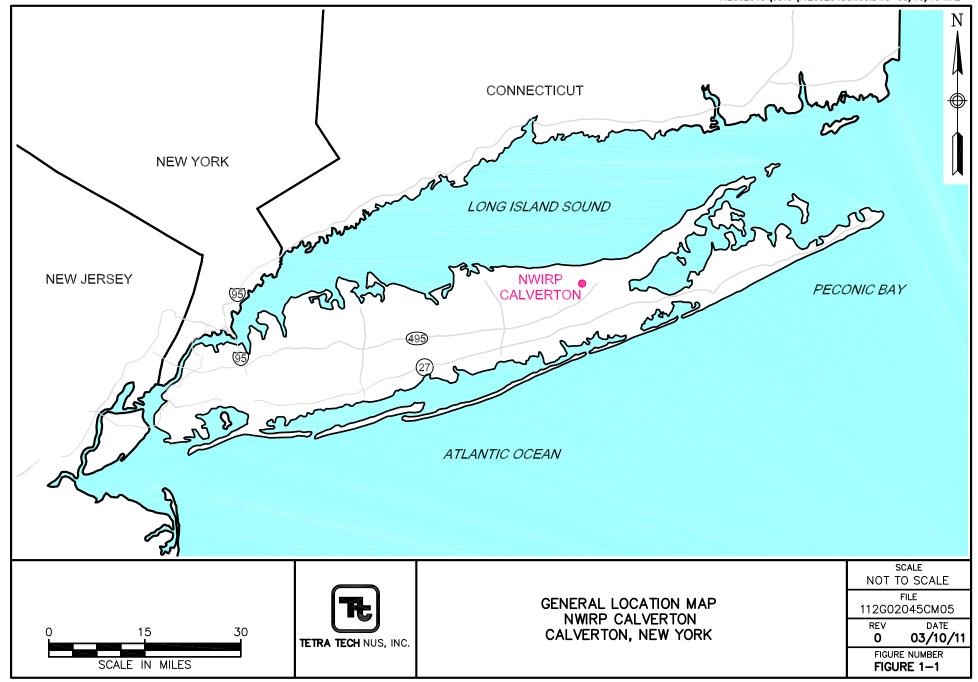
Activity	Schedule
Finalize Design	April 30, 2012
Solicit Bids	May 11, 2012
Award Contract	June 30, 2012
Planning Documents	July 30, 2012
Construction	November 30, 2012
Complete Start up	December 30, 2012

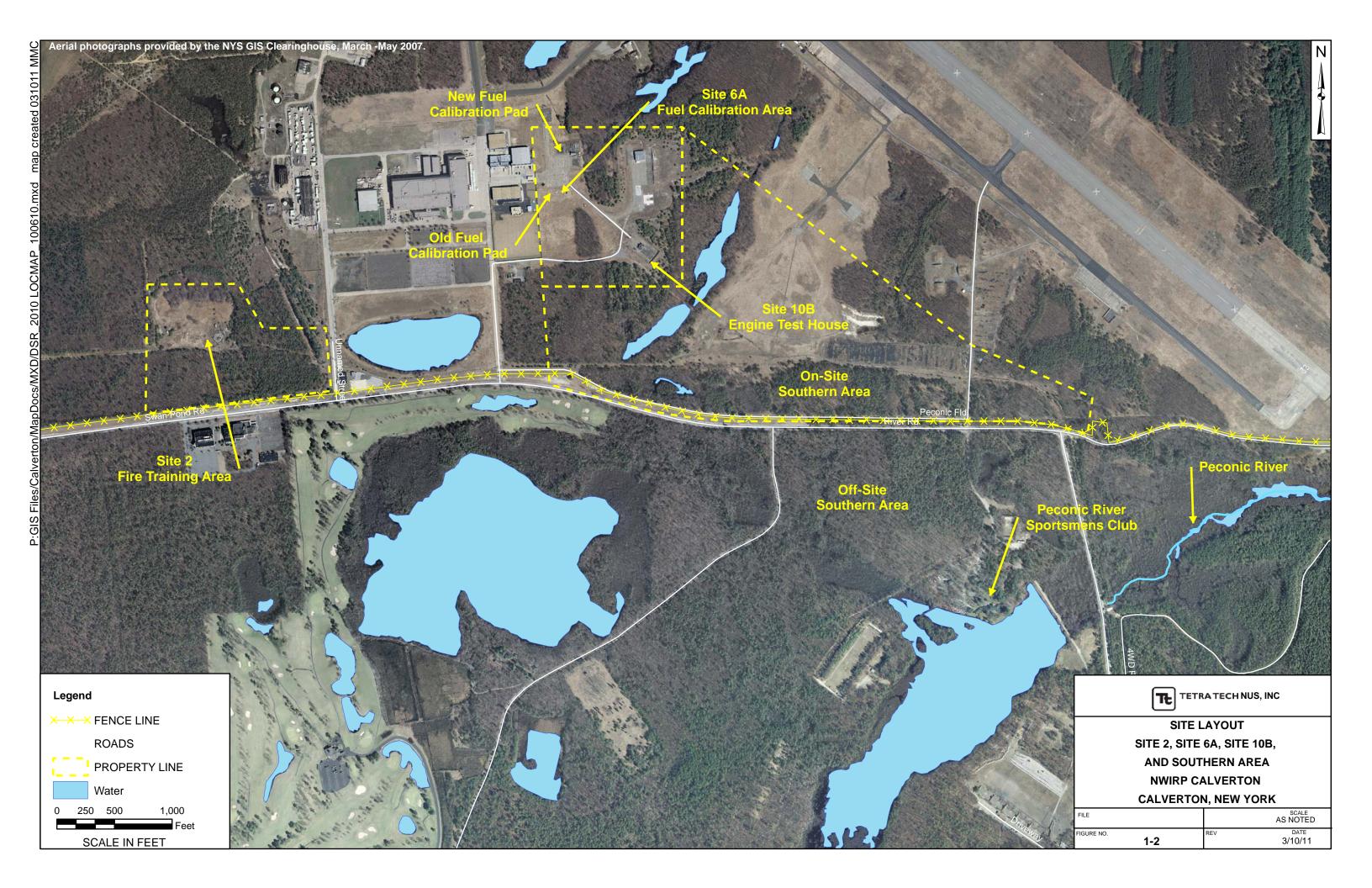
REFERENCES

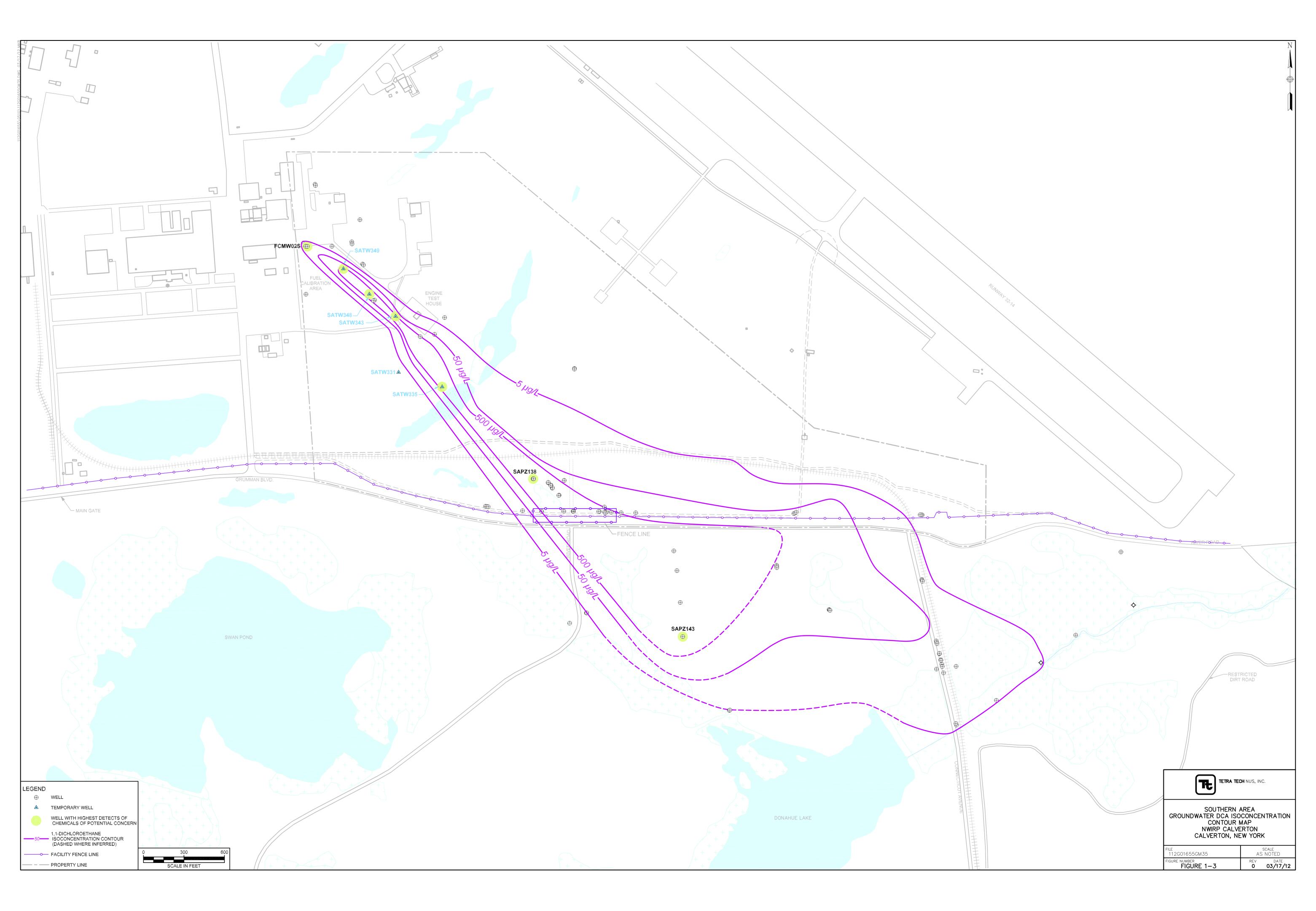
Tetra Tech, 2011. Corrective Measures Study (CMS)/Feasibility Study for Southern Area Groundwater Plume, prepared by Tetra Tech Inc. for Mid-Atlantic Division Naval Facilities Engineering Command, under Contract Number N62470-08-D-1001, Contract Task Order WE-08, March.

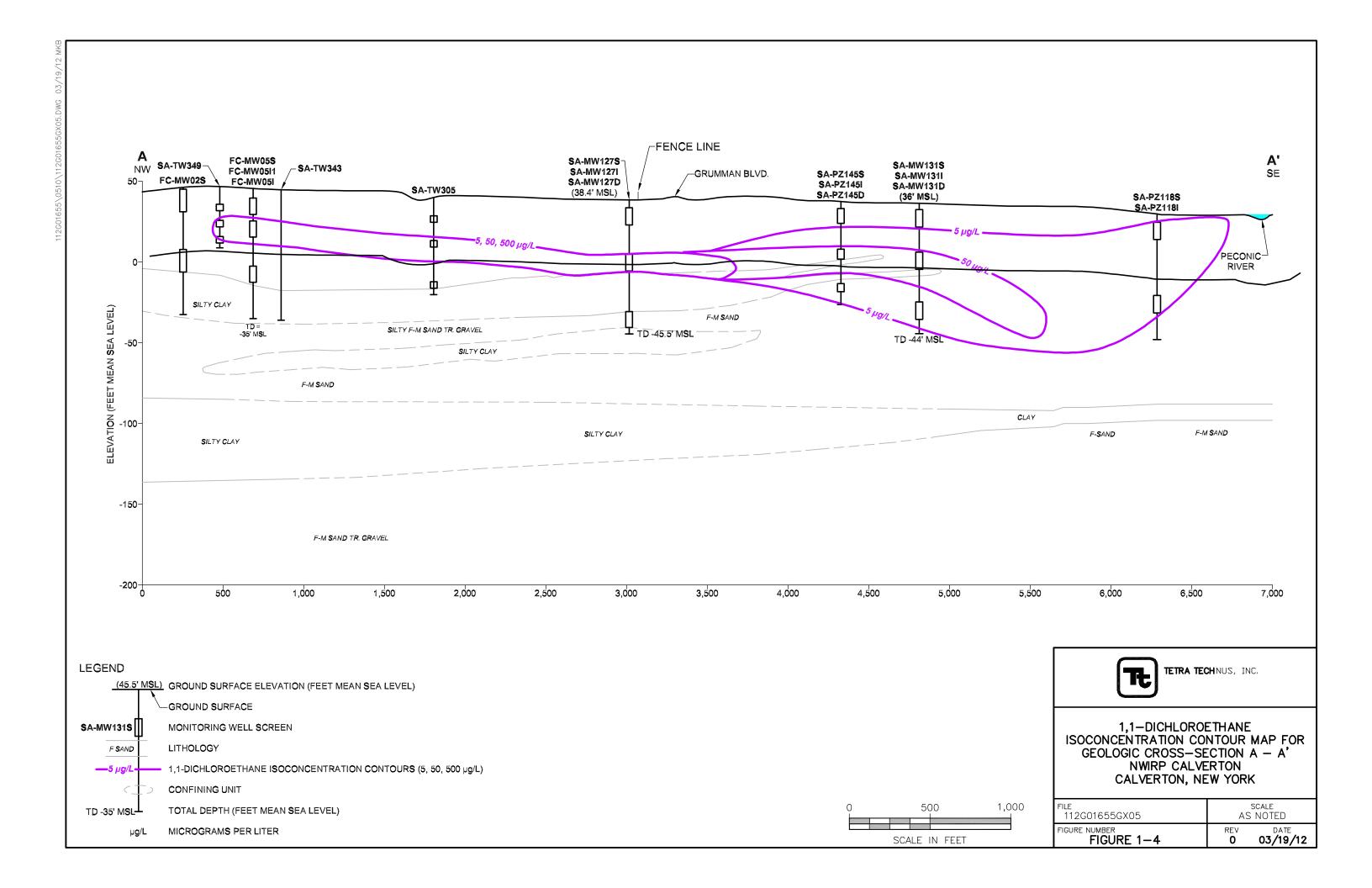
Tetra Tech, 2012. Data Summary Report, Enhanced In Situ Bioremediation Pilot Test, Southern Area prepared by Tetra Tech Inc. for Mid-Atlantic Division Naval Facilities Engineering Command, under Contract Number N62470-08-D-1001, Contract Task Order WE-08, March.

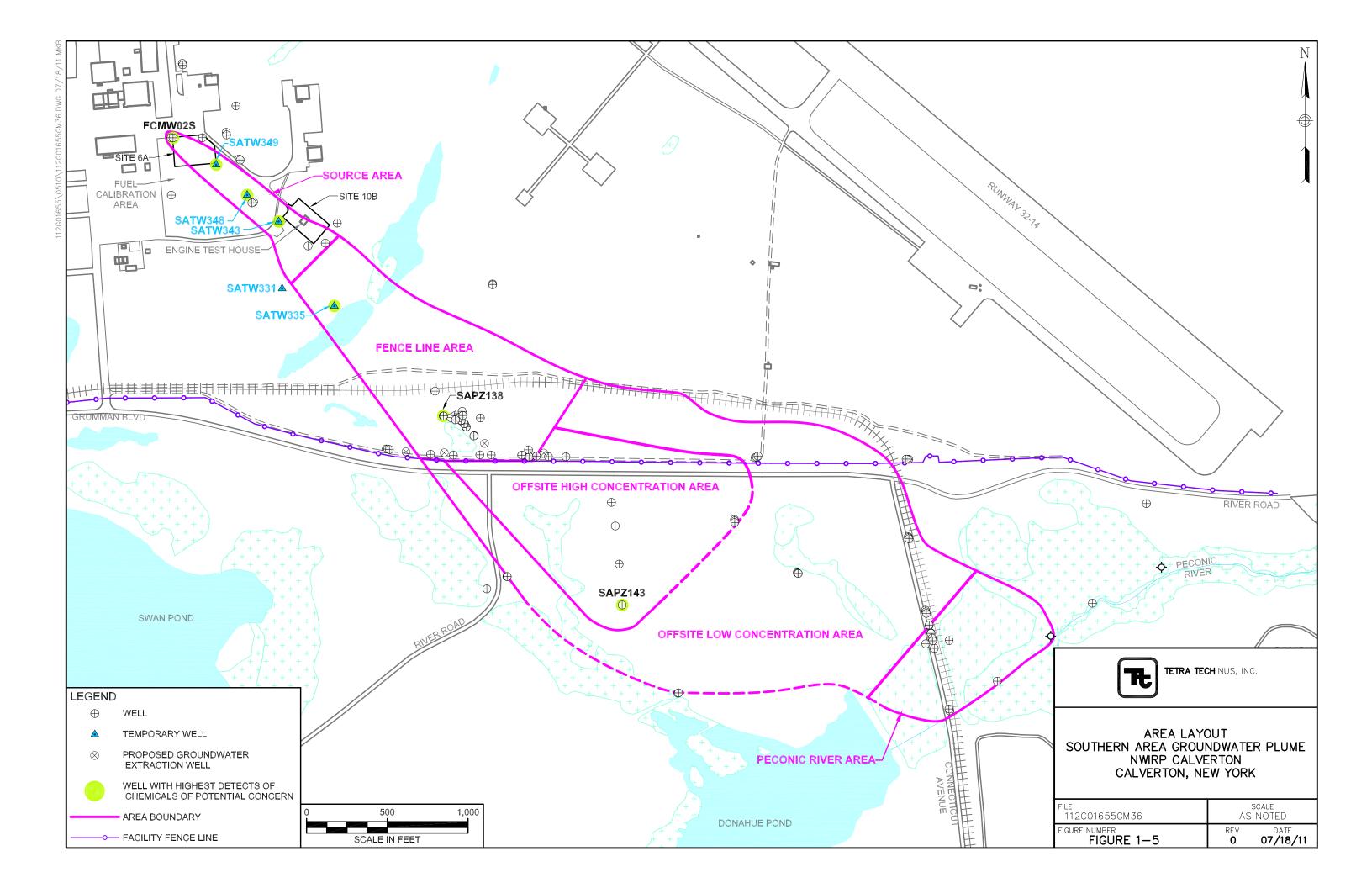




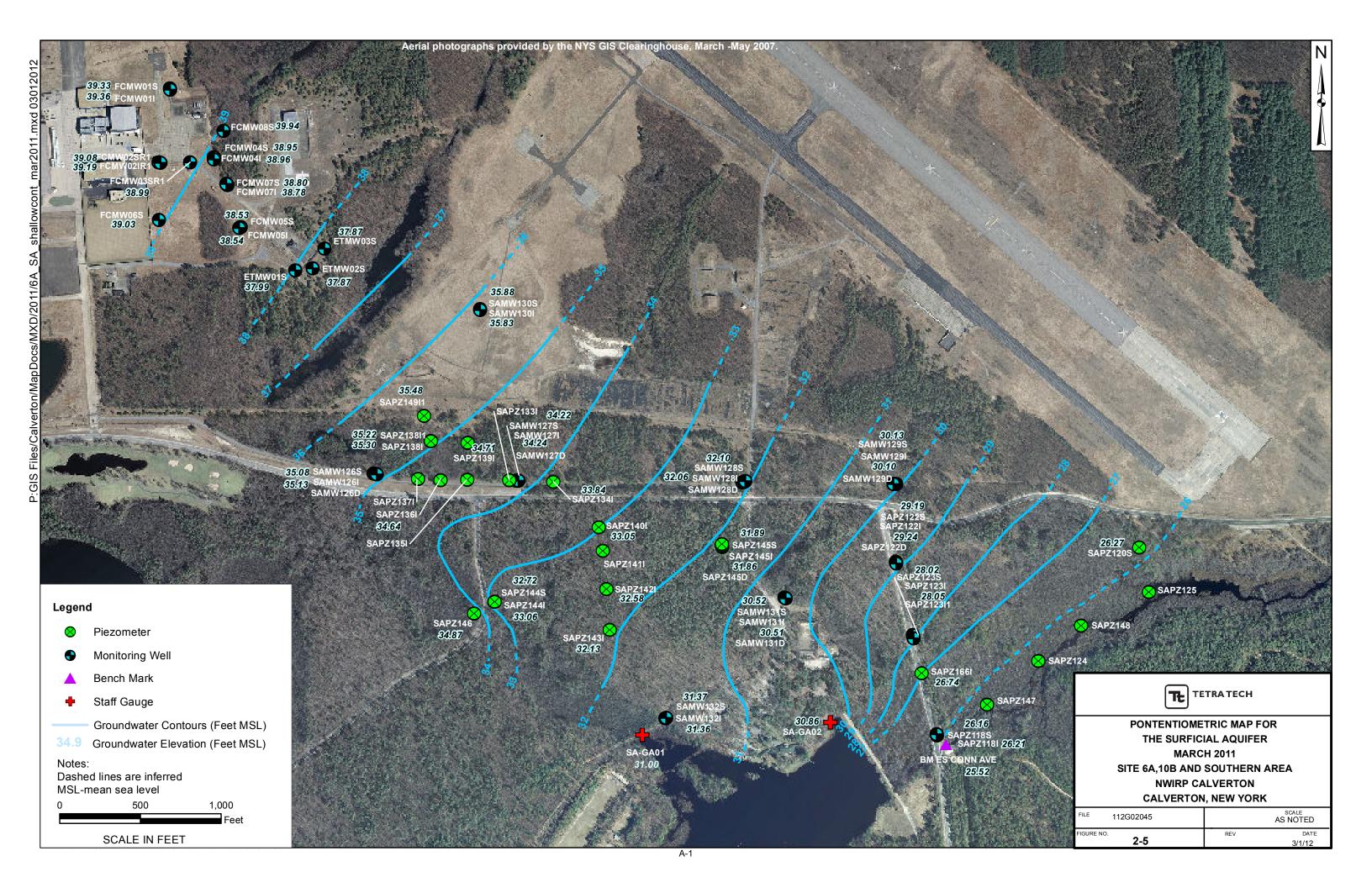


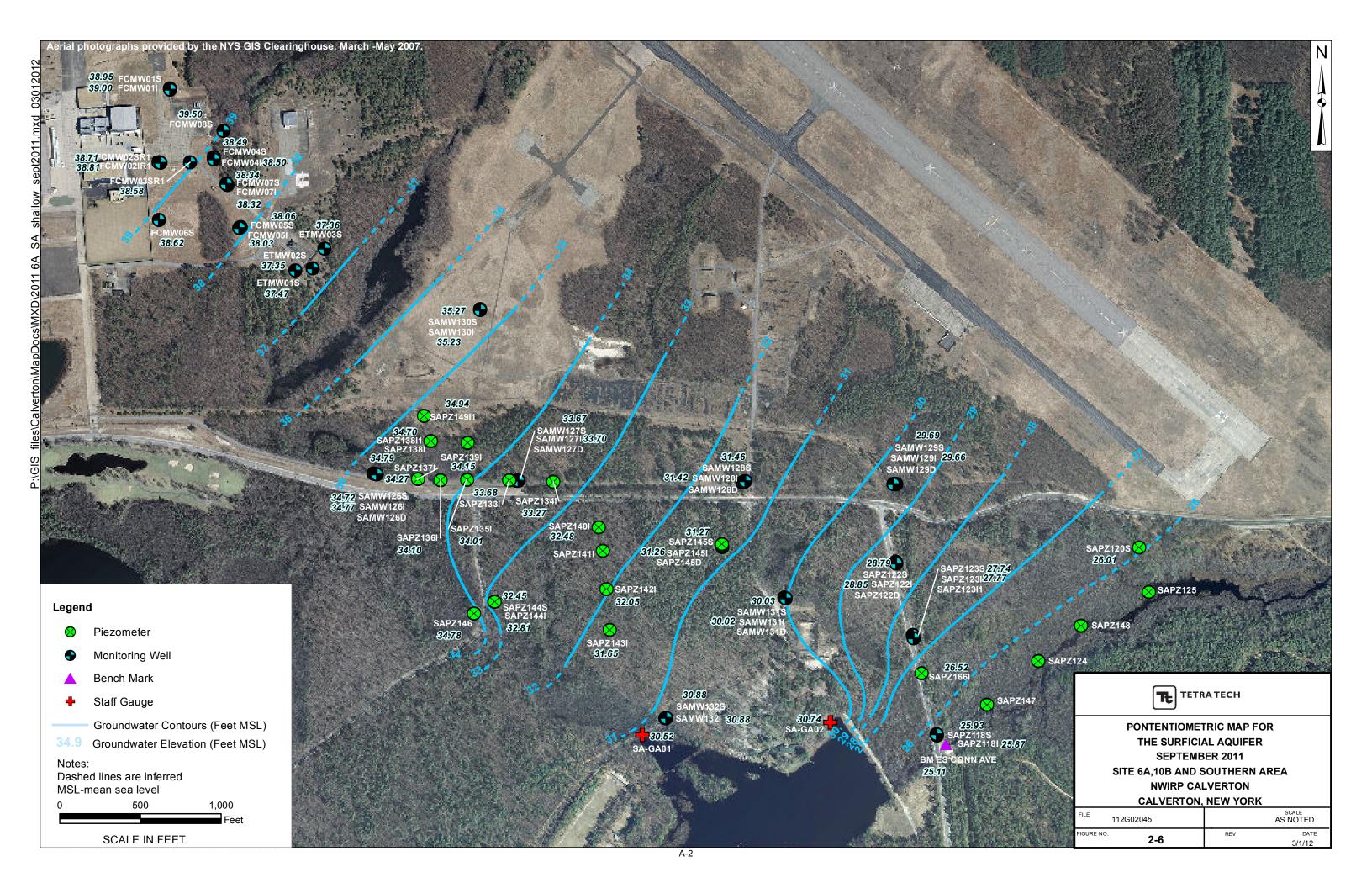


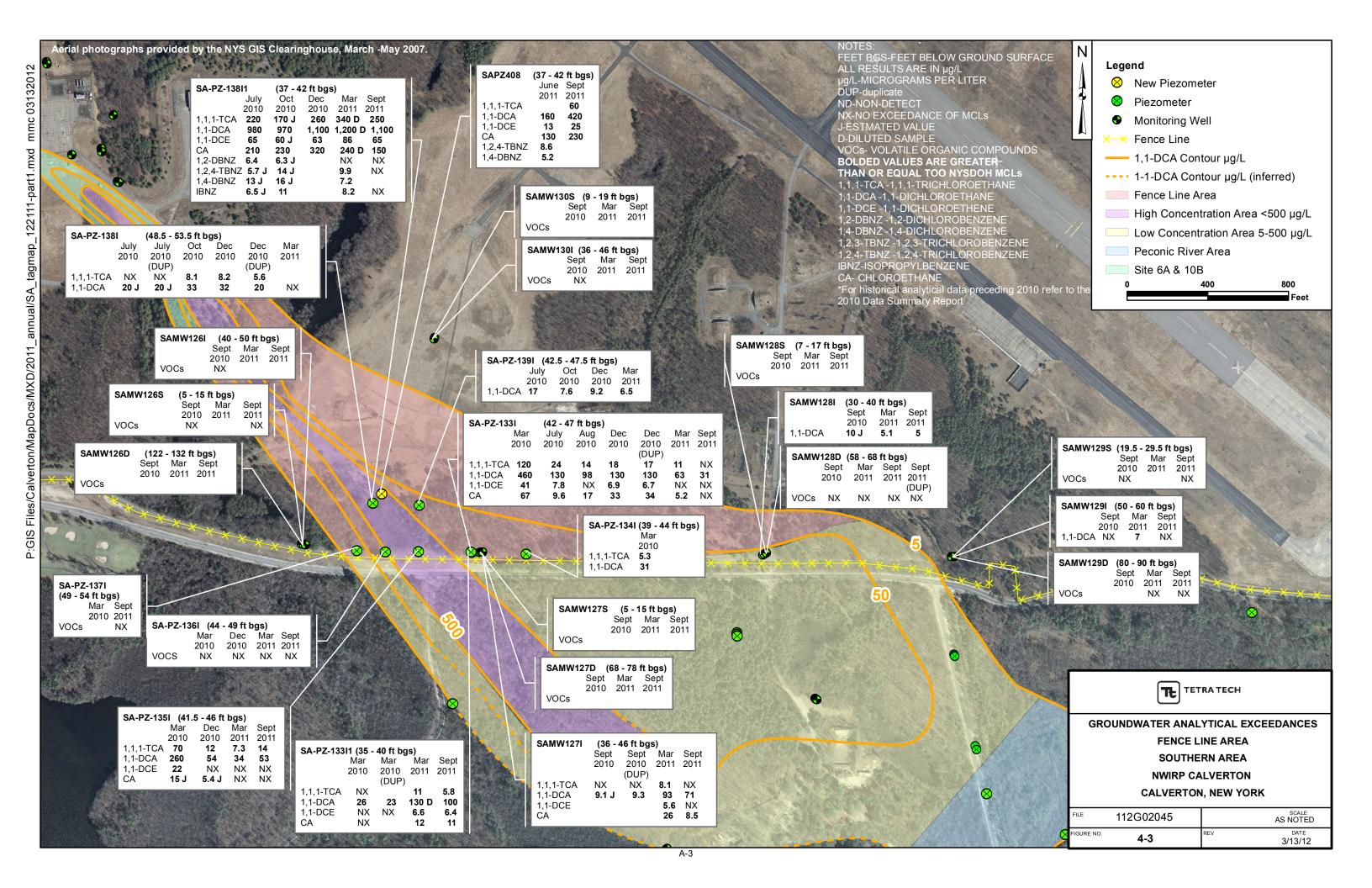




APPENDIX A BACKUP ANALYTICAL DATA AND POTENTIOMETRIC SURFACE MAPS







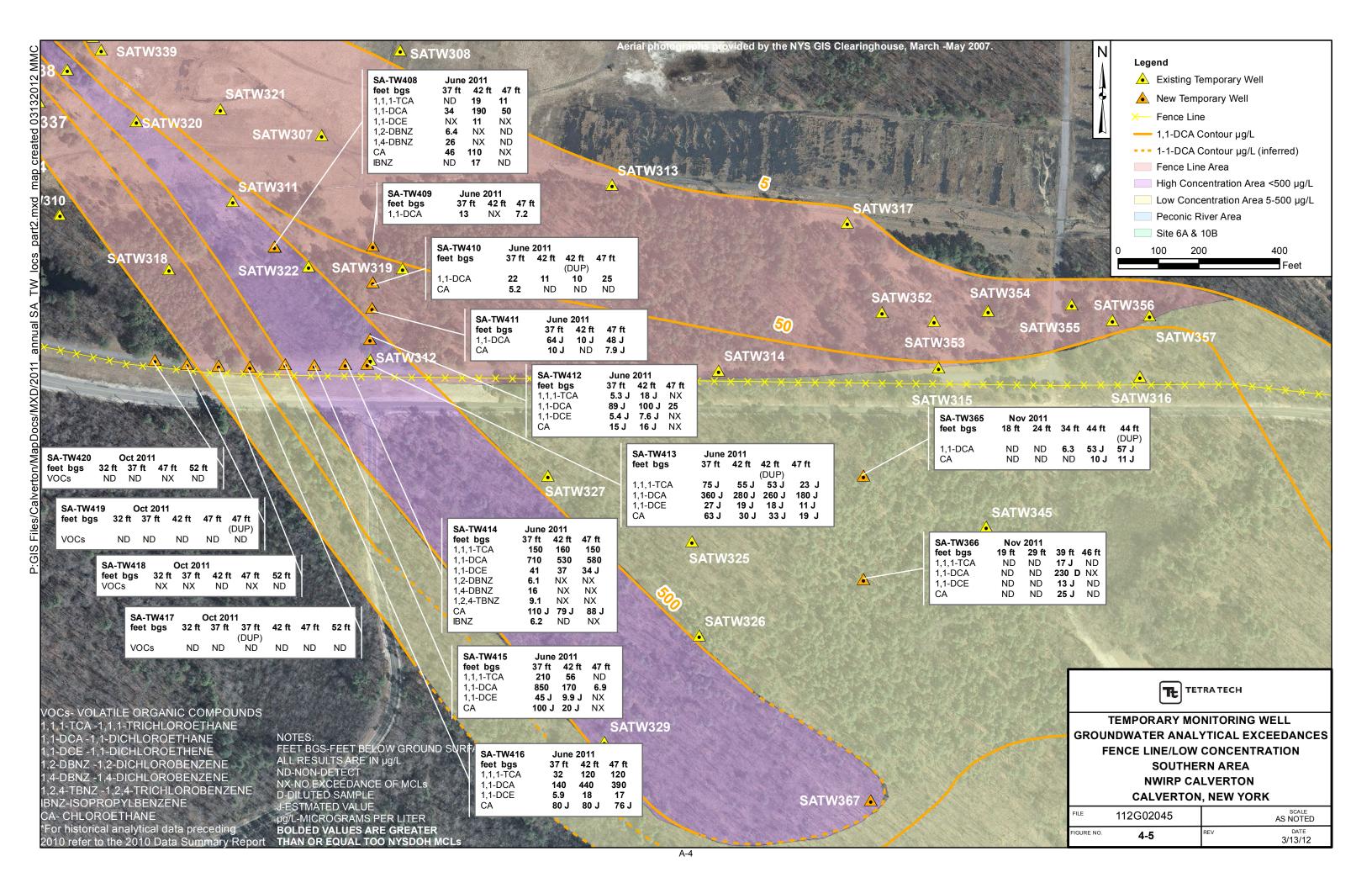


TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 1 OF 15

Purpose / Note Location	NYSDOH				Cross	-gradient Reference V SA-PZ-133I (42-47 ft bgs)	Vell					Cross-gradient I SA-PZ (35-40	-133I1	
Sample Date	– MCLs ⁽¹⁾	3/31/2010	7/8/2010	10/12/2010	12/15/2010	12/15/2010 (duplicate)	3/8/2011	6/9/2011	6/21/2011	9/19/2011	3/31/2010	6/9/2011	6/21/2011	9/19/2011
VOCs (µg/L)														•
1,1,1-Trichloroethane (TCA)	5	120	24	14	18	17	11	9.5	10 J	4.2	2 J	22 J	14	5.8
1,1-Dichloroethane (DCA)	5	460	130	98	130	130	63	76	90 J	31	26	120	170	100
1,1-Dichloroethene (DCE)	5	41	7.8	4.9 J	6.9	6.7	3.9	4.3	4.2 J	2	1.6 J	13 J	8.3	6.4
Chloroethane (CA)	5	67	9.6	17	33	34	5.2	6.7	7.4 J	1.9	4.9 J	22 J	15	11
Benzene	5	1.1 J	ND	ND	0.35 J	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,4-Dichlorobenzene	5	2.2 J	ND	ND	ND	ND	ND	ND	ND	ND	1.2 J	ND	ND	ND
1,3-Dichlorobenzene	5	0.65 J	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dichlorobenzene	5	0.91 J	0.70 J	ND	ND	ND	ND	ND	ND	ND	0.36 J	ND	ND	ND
Isopropyl Benzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2,4-Trichlorobenzene	5	3 J	0.98 J	ND	ND	ND	0.84 J	ND	ND	0.89 J	0.75 J	ND	ND	0.62 J
Chlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Napthalene	50	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		688	171	134	188	188	83	96.5	111.6	39.1	34.5	177	207.3	123.2
DCA/TCA Ratio		3.8	5.4	7.0	7.2	7.6	5.7	8.0	9.0	7.4	13.0	5.5	12.1	17.2
CA/DCA Ratio		0.15	0.07	0.17	0.25	0.26	0.08	0.09	0.08	0.06	0.19	0.18	0.09	0.11
CA/TCA Ratio		0.56	0.40	1.21	1.83	2.00	0.47	0.71	0.74	0.45	2.45	1.00	1.07	1.90
Dissolved Gases (µg/L)		0.00	0.70	1.21	7.00	2.00	0.77	0.7 7	0.7 7	0.70	2.70	7.00	7.07	7.00
Methane	none													
Ethane	none													
Ethene	none													
Dechlorinating Bacteria (cells/mL)	Hone	1	<u> </u>		L	L				l				
Dehalococcoides sp.	none													
Dehalobacter sp.	none													
Metals (µg/L)	Hone													
Iron	300 ⁽²⁾								45.1 J				46.1 J	
Fe ²⁺ (Ferrous Iron)	none						0		40.1 0				40.1 3	
Manganese	300 (2)								870				2,760	
Wet Chemistry (mg/L)	300								670				2,700	
Nitrate (as N)	10		I			I				ı				
Nitrate (as N) Nitrite (as N)	10													
	250													
Chloride	250													
Sulfide	none													
TOC	none													
Water Quality Parameters		500 1	I		5 00 T	Т	F 70	5.00	2.22	224	0.07	5.00	0.00	0.44
pH	none	5.98	5.87	6.41	5.62		5.79	5.68	6.62	6.24	6.27	5.92	6.92	6.41
Specific Conductivity (mS/cm)	none	0.120	0.134	0.103	0.079		0.107	0.119	0.082	0.101	0.098	0.107	0.025	0.093
Dissolved Oxygen (mg/L)	none	0		0	0		/ 0.6	1.49	0 / 1.0	0.74 / 0.80		1.40	0 / 1.0	1.13 / 0.60
Temperature (°C)	none	11.21	14.72	14.93	10.56		7.18	12.16	12.63	12.58	11.21	12.44	13.38	13.73
Oxygen Reduction Potential (mV)	none	104	163	156	-12		125	116	81	172	2	70	29	62
Turbidity (NTU)	none	1.53	0	0	0		0.35	1.4	35.5	0.91	2.59	0.5	44.9	0.43

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 2 OF 15

Purpose / Notes	NYSDOH				Cros	ss-gradient Reference V	Vell			
Location	MCLs (1)					(41.5-46.5 ft bgs)				
Sample Date	020	3/31/2010	12/14/2010	3/8/2011	6/7/2011	6/21/2011	8/3/2011	8/3/2011	8/4/2011	9/19/2011
VOCs (μg/L)						•	•		•	•
1,1,1-Trichloroethane (TCA)	5	70	12	7.3	5.6	4.6	0.52 J	6.3	4.0	14
1,1-Dichloroethane (DCA)	5	260	54	34	35	27	19	31	29	53
1,1-Dichloroethene (DCE)	5	22	3.3 J	2.6	2.8	1.9	1.1	2.0	1.8	3.5
Chloroethane (CA)	5	15 J	5.4	1.2	1.8	2.1	ND	ND	1.3	2.8
Benzene	5	0.35 J	ND	ND	ND	ND	ND	ND	ND	ND
1,4-Dichlorobenzene	5	0.38 J	ND	ND	ND	ND	ND	ND	ND	ND
1,3-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dichlorobenzene	5	0.91 J	ND	ND	ND	ND	ND	ND	ND	ND
Isopropyl Benzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2,4-Trichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND
Chlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND
Napthalene	50	ND	ND	ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		367	74.7	45.1	45.2	35.6	20.62	39.3	36.1	73.3
DCA/TCA Ratio		3.7	4.5	4.7	6.3	5.9	37	4.9	7.3	3.8
CA/DCA Ratio		0.06	0.10	0.04	0.05	0.08			0.04	0.05
CA/TCA Ratio		0.21	0.45	0.16	0.32	0.46			0.33	0.20
Dissolved Gases (μg/L)		, , , , , , , , , , , , , , , , , , ,								
Methane	none									
Ethane	none									
Ethene	none									
Dechlorinating Bacteria (cells/mL)						<u> </u>			<u>I</u>	<u>.l</u>
Dehalococcoides sp.	none									
Dehalobacter sp.	none									
Metals (µg/L)			ı			1			I	
Iron	300 ⁽²⁾					26.7 J				
Fe ²⁺ (Ferrous Iron)	none			0						
Manganese	300 (2)					927				
Wet Chemistry (mg/L)			<u>I</u>			021			<u>I</u>	
Nitrate (as N)	10									
Nitrite (as N)	1									
Chloride	250									
Sulfide	none									
TOC	none									
Water Quality Parameters	HOHE									
pH	none	5.75	4.75	5.77	4.99	7.02	5.28	6.18	4.99	5.82
Specific Conductivity (mS/cm)	none	0.123	0.090	0.109	0.122	0.088	0.108	0.105	0.098	0.101
Dissolved Oxygen (mg/L)		0.123	0.080	/ 1.0	1.56	0.088	0.106	0.105	0.098	0.101
Temperature (°C)	none	10.83	10.8	11.14	13.01	14.12	13.41	14.55	13.56	13.83
. , ,	none									
Oxygen Reduction Potential (mV)	none	109	169	116	160	75	226	219	338	116
Turbidity (NTU)	none	3.52	0	0.77	0.5	85.6	0	0.55	0.32	0.01

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 3 OF 15

Purpose / Notes					Cros	ss-gradient Reference	Well				Cros	s-gradient Reference	Well
Location	NYSDOH MCLs ⁽¹⁾					SA-PZ-136 (44-49 ft bgs)						SA-PZ-137 (49-54 ft bgs)	
Sample Date		3/31/2010	12/14/2010	3/8/2011	6/7/2011	6/21/2011	8/3/2011	8/3/2011	8/4/2011	9/19/2011	3/31/2010	6/8/2011	9/19/2011
VOCs (μg/L)								<u>. </u>		1			
1,1,1-Trichloroethane (TCA)	5	ND	ND	ND	ND	ND	14	12	23	ND	ND	ND	ND
1,1-Dichloroethane (DCA)	5	1.5 J	1.5 J	1.8	ND	1.5	110	100	130	1.7	ND	1.2	1.2
1,1-Dichloroethene (DCE)	5	ND	ND	ND	ND	ND	6.4	5.3	8.6	ND	ND	ND	ND
Chloroethane (CA)	5	ND	ND	ND	ND	ND	9.3	8.6	12	ND	ND	ND	ND
Benzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,4-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,3-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Isopropyl Benzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2,4-Trichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Chlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Napthalene	50	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		1.5	1.5	1.8		1.5	139.7	125.9	173.6	1.7	0	1.2	1.2
DCA/TCA Ratio							7.9	8.3	5.7				
CA/DCA Ratio							0.08	0.09	0.09				
CA/TCA Ratio							0.66	0.72	0.52				
Dissolved Gases (μg/L)										II.			
Methane	none												
Ethane	none												
Ethene	none												
Dechlorinating Bacteria (cells/mL)										•			•
Dehalococcoides sp.	none												
Dehalobacter sp.	none												
Metals (μg/L)										•			•
Iron	300 ⁽²⁾					877							
Fe ²⁺ (Ferrous Iron)	none			1,200									
Manganese	300 ⁽²⁾					1,600							
Wet Chemistry (mg/L)										•			•
Nitrate (as N)	10												
Nitrite (as N)	1												
Chloride	250												
Sulfide	none												
TOC	none												
Water Quality Parameters										-			-
pH	none	6.10	5.64	5.95	5.60	7.12	6.52	6.61	6.05	6.15	6.27	5.78	6.51
Specific Conductivity (mS/cm)	none	0.129	0.123	0.118	0.130	0.096	0.317	0.304	0.246	0.112	0.133	0.134	0.106
Dissolved Oxygen (mg/L)	none		0	/ 0.8	1.4	0 / 1.0	0	0	0.14	0.75 / 0.60	0	1.64	0.36 / 0.20
Temperature (°C)	none	10.23	10.45	10.81	11.56	13.49	13.93	15.32	13.92	13.51	10.28	11.39	13.91
Oxygen Reduction Potential (mV)	none	-7	-56	98	65	4	-55	-92	-5	94	4	47	88
Turbidity (NTU)	none	23.3	4.70	1.96	38.5	3.38	4.19	8.47	4.67	1.06	7.75	2.1	0.46

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 4 OF 15

Purpose / Notes				Upo	gradient Monitoring We	II		
Location	NYSDOH				SA-PZ-138I 48.5-53.5 ft bgs)			
Sample Date	MCLs ⁽¹⁾	7/8/2010	7/8/2010 (duplicate)	10/12/2010	10/12/2010 (duplicate)	12/15/2010	3/8/2011	6/21/2011
VOCs (µg/L)								
1,1,1-Trichloroethane (TCA)	5	4.4 J	4.4 J	8.1	8.2	5.6	ND	1.5
1,1-Dichloroethane (DCA)	5	20 J	20 J	33	32	20	4.1	9.6
1,1-Dichloroethene (DCE)	5	1.2 J	1.0 J	1.7 J	2.0 J	1.2 J	ND	0.6 J
Chloroethane (CA)	5	ND	1.7 J	ND	ND	ND	ND	ND
Benzene	5	ND	ND	ND	ND	ND	ND	ND
1,4-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND
1,3-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND
1,2-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND
Isopropyl Benzene	5	ND	ND	ND	ND	ND	ND	ND
1,2,4-Trichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND
Chlorobenzene	5	ND	ND	ND	ND	ND	ND	ND
Napthalene	50	ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		26	27	43	42	27	4.1	12
DCA/TCA Ratio		4.5	4.5	4.1	3.9	3.6		6.4
CA/DCA Ratio			0.09					
CA/TCA Ratio			0.39					
Dissolved Gases (μg/L)		•	•	•	•	•		•
Methane	none							
Ethane	none							
Ethene	none							
Dechlorinating Bacteria (cells/mL)		_						
Dehalococcoides sp.	none							
Dehalobacter sp.	none							
Metals (μg/L)		_						
Iron	300 ⁽²⁾							ND
Fe ²⁺ (Ferrous Iron)	none						0	0
Manganese	300 ⁽²⁾							731
Wet Chemistry (mg/L)		•	•	•		•		
Nitrate (as N)	10							
Nitrite (as N)	1							
Chloride	250							
Sulfide	none							
TOC	none							
Water Quality Parameters		•	•	•	•	•		•
pH	none	5.88		5.85		6.38	5.62	5.67
Specific Conductivity (mS/cm)	none	0.134		0.099		0.089	0.114	0.094
Dissolved Oxygen (mg/L)	none			0.24			/ 1.5	0 / 0.3
Temperature (°C)	none	13.67		13.0		11.2	6.57	15.32
Oxygen Reduction Potential (mV)	none	-6.0		42		90	144	161
Turbidity (NTU)	none	0		0		0	0.3	0

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 5 OF 15

Purpose / Note	n NYSDOH			Up	gradient Monitoring W SA-PZ-138I1 (37-42 ft bgs)	Vell					Cross-gradient F SA-PZ (42.5-47.	'-139I		
Sample Dat	– MCLs ⁽¹⁾ e	7/6/2010	10/12/2010	12/15/2010	3/8/2011	6/21/2011 ⁽³⁾	6/21/2011 ⁽³⁾ (duplicate)	9/20/2011	7/8/2010	10/12/2010	12/15/2010	3/8/2011	6/10/2011	6/20/2011
VOCs (µg/L)														
1,1,1-Trichloroethane (TCA)	5	220	170 J	260	340	320	300	250	2.3 J	0.92 J	1.3 J	ND	ND	ND
1,1-Dichloroethane (DCA)	5	980	970	1,100	1,200	1,500	1,500	1,100	17	7.6	9.2	6.5	5.9 J	4.6
1,1-Dichloroethene (DCE)	5	65	60 J	63	86	100	85	65	0.94 J	ND	ND	ND	ND	ND
Chloroethane (CA)	5	210	230	320	240	250	280	150	1.8 J	ND	ND	ND	ND	ND
Benzene	5	3.4 J	4.4 J	ND	2.6	ND	ND	1.6	ND	ND	ND	ND	ND	ND
1,4-Dichlorobenzene	5	13 J	16 J	ND	7.2	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,3-Dichlorobenzene	5	3.1 J	4.0 J	ND	1.6	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dichlorobenzene	5	6.4 J	6.3 J	ND	3.7	ND	ND	1.9	ND	ND	ND	ND	ND	ND
Isopropyl Benzene	5	6.5 J	11	ND	8.2	ND	ND	2.5	ND	ND	ND	ND	ND	ND
1,2,4-Trichlorobenzene	5	5.7 J	14 J	ND	9.9	ND	ND	4.8	ND	ND	ND	ND	ND	ND
Chlorobenzene	5	ND	1.1 J	ND	0.55 J	ND	ND	ND	ND	ND	ND	ND	ND	ND
Napthalene	50	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		1475	1430	1743	1866	2170	2165	1565	22	9	10.5	6.5	5.9	4.6
DCA/TCA Ratio		4.5	4.2	4.2	3.5	4.7	5.0	4.4	7.4	8.3	7.1			
CA/DCA Ratio		0.21	0.24	0.29	0.20	0.17	0.19	0.14	0.11					
CA/TCA Ratio		0.95	1.35	1.23	0.71	0.78	0.93	0.60	0.78					
Dissolved Gases (µg/L)		Į.				I							l .	
Methane	none													
Ethane	none													
Ethene	none													
Dechlorinating Bacteria (cells/mL)						<u> </u>								
Dehalococcoides sp.	none													
Dehalobacter sp.	none													
Metals (μg/L)				l		ı								
Iron	300 ⁽²⁾					ND	ND							40.7 J
Fe ²⁺ (Ferrous Iron)	none				0							0		
Manganese	300 ⁽²⁾					5,220	5,260							172
Wet Chemistry (mg/L)		<u> </u>		l		0,220	0,200				<u> </u>			
Nitrate (as N)	10													
Nitrite (as N)	1													
Chloride	250													
Sulfide	none													
TOC	none													
Water Quality Parameters	Hone													
pH	none	6.12	5.93	5.97	5.74	6.98		6.15	5.28	6.15	5.53	5.71	5.58	6.47
Specific Conductivity (mS/cm)	none	0.12	0.146	0.139	0.181	0.135		0.153	0.099	0.101	0.087	0.108	0.126	0.083
Dissolved Oxygen (mg/L)		1.67	0.146	0.138	/ 1.0	0.135		/ 1.0	0.099	0.101	0.087	/ 0.6	1.52	0.063
Temperature (°C)	none	14.27	13.1	11.0	6.31	15.49		13.96	13.67	15.84	11.07	6.68	12.26	12.67
	none		127	120	130				13.67			127		
Oxygen Reduction Potential (mV)	none	62 0.45	0	0.24	0.31	82		50 0	1.29	183 0.08	-1 0	0.29	144 0.5	66 20
Turbidity (NTU)	none	U. 4 5	U	0.24	0.31	0		U	1.29	0.08	0	0.29	0.5	20

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 6 OF 15

Purpose / Notes	NVCDOU		Up	ogradient Monitoring W	'ell				Ir	njection/Extraction Wel	I		
Location	NYSDOH MCLs ⁽¹⁾			(32-37 ft bgs)						(34-39 ft bgs)			
Sample Date		7/8/2010	10/12/2010	12/15/2010	3/8/2011	6/20/2011	7/7/2010	10/12/2010	10/12/2010 (duplicate)	12/15/2010	3/8/2011	3/8/2011 (duplicate)	6/22/2011 ⁽³⁾
VOCs (μg/L)													
1,1,1-Trichloroethane (TCA)	5	6.6	ND	ND	ND	ND	110	36	35	32	36 J	39 J	ND
1,1-Dichloroethane (DCA)	5	40	3.6 J	6.7	18	12 J	490	180	170	190	310	310	390
1,1-Dichloroethene (DCE)	5	2.6 J	ND	0.82 J	1.7	1.3 J	33	14	13	13	20 J	22 J	24
Chloroethane (CA)	5	9.8	ND	10	18	14 J	99	91	91	140	220	220	260
Benzene	5	ND	ND	ND	ND	ND	1.1 J	1.3 J	1.2 J	1.6 J	2.1 J	2.3 J	ND
1,4-Dichlorobenzene	5	5.4	4.7 J	13	28	12 J	ND	11	11	22	23 J	26 J	ND
1,3-Dichlorobenzene	5	1.1 J	1.0 J	2.7 J	6.0	2.5 J	ND	2.5 J	2.3 J	4.0 J	5.3 J	5.8 J	ND
1,2-Dichlorobenzene	5	1.6 J	1.2 J	3.0 J	7.8	3.2 J	ND	3.6 J	3.6 J	5.8 J	6.9 J	7.5 J	ND
Isopropyl Benzene	5	0.42 J	ND	0.39 J	1.8	ND	ND	0.49 J	0.47 J	1.1 J	2.5 J	2.7 J	ND
1,2,4-Trichlorobenzene	5	ND	ND	ND	1.9	ND	ND	1.8 J	1.8 J	ND	9.6 J	11 J	ND
Chlorobenzene	5	1.3 J	ND	ND	5.1	1.5 J	ND	ND	ND	ND	2.7 J	3.0 J	ND
Napthalene	50	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		59	4	18	38	27	732	321	309	375	586	591	674
DCA/TCA Ratio		6.1					4.5	5.0	4.9	5.9	8.6	7.9	
CA/DCA Ratio		0.25		1.5	1.0	0.9	0.20	0.15	1.9	1.4	0.71	0.71	0.67
CA/TCA Ratio		1.48					0.90	2.53	2.60	4.38	6.11	5.64	
Dissolved Gases (μg/L)										<u></u>	<u></u>		
Methane	none						110	140 D	300 D	210 D	402 D	320 D	344
Ethane	none						ND	ND	ND	ND	ND	ND	ND
Ethene	none						ND	ND	ND	ND	ND	ND	ND
Dechlorinating Bacteria (cells/mL)								•		•	•		
Dehalococcoides sp.	none												
Dehalobacter sp.	none												
Metals (μg/L)										L	L		\
Iron	300 ⁽²⁾					112	1,500	1,010	1,020	1,170	214 J	225 J	612
Fe ²⁺ (Ferrous Iron)	none				200						400	400	
Manganese	300 ⁽²⁾					1,630	4,680	5,460	5,550	5,580	5,460	5,750	5,270
Wet Chemistry (mg/L)						,	,	-,	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	-,	.,	-,	
Nitrate (as N)	10												ND
Nitrite (as N)	1												ND
Chloride	250												5.02
Sulfide	none												ND
TOC	none						1.5	1.1	1.33	1.31 J	2.6 J	3.2 J	2.1
Water Quality Parameters											2.0 0	0.2	
pH	none	5.83	5.96	6.70	5.78	6.69	6.38	6.10		5.90	5.66		6.42
Specific Conductivity (mS/cm)	none	0.103	0.09	0.079	0.102	0.063	0.174	0.127		0.123	0.161		0.123
Dissolved Oxygen (mg/L)	none	0.100	0.3		/ 1.0	0 / 0.8		0.39		0.120	/ 1.0		0 / 1.2
Temperature (°C)	none	13.78	13.5	11.3	6.98	12.66	14.65	13.2		10.78	7.03		12.54
Oxygen Reduction Potential (mV)	none	42	71	69	98	18	-124	-16		-95	109		-51
Turbidity (NTU)	none	0	0	0.74	0.28	31.4	0.84	0		0.03	0.82		0

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 7 OF 15

Purpose / Notes Location	NYSDOH			,	traction Well Z-155I ft bas)					Downgradient N SA-P2 (41-46	Z-157I		
Sample Date	- MCLs ⁽¹⁾	7/7/2010	7/7/2010 (duplicate)	10/12/2010	12/15/2010	3/7/2011	6/22/2011	7/8/2010	10/11/2010	12/14/2010	3/7/2011	5/9/2011	6/21/2011
VOCs (μg/L)			, , , ,				•						
1,1,1-Trichloroethane (TCA)	5	38	36	15	16	19	7.8	46	15	17	21	31 J	9.7
1,1-Dichloroethane (DCA)	5	150	150	65	70	70	43	180	65	75	71	280 J	45
1,1-Dichloroethene (DCE)	5	12	11	3.7 J	3.4 J	5.4	2.4	13	4.2 J	4.1 J	5.2	17 J	3.4
Chloroethane (CA)	5	17	19	ND	ND	7.5	2.2	24	5.7	7.6	3.3	200 J	3.4 J
Benzene	5	0.33 J	0.31 J	ND	ND	ND	ND	0.43 J	ND	ND	ND	1.7 J	ND
1,4-Dichlorobenzene	5	0.31 J	ND	ND	ND	ND	ND	ND	ND	ND	ND	6.6 J	ND
1,3-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	1.4 J	ND
1,2-Dichlorobenzene	5	ND	0.4 J	ND	ND	ND	ND	ND	ND	ND	ND	1.9 J	ND
Isopropyl Benzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2,4-Trichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	5 J	0.85 J
Chlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	0.53 J	ND
Napthalene	50	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		217	216	84	89.4	101.9	55.4	263	90	104	101	528	61.5
DCA/TCA Ratio		3.9	4.2	4.3	4.4	3.7	5.5	3.9	4.3	4.4	3.4	9.0	4.6
CA/DCA Ratio		0.11	0.13			0.11	0.05	0.13	0.09	0.10	0.05	0.71	0.08
CA/TCA Ratio		0.45	0.53			0.39	0.28	0.52	0.38	0.45	0.16	6.45	0.35
Dissolved Gases (µg/L)													
Methane	none	9	12	3.7	2.5	8.1	ND	14	2.7	12	ND		ND
Ethane	none	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND		ND
Ethene	none	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND		ND
Dechlorinating Bacteria (cells/mL)			<u> </u>				<u>I</u>						
Dehalococcoides sp.	none							0.20 J		1.6			ND
Dehalobacter sp.	none							50.2		40.4			544
Metals (µg/L)													
Iron	300 ⁽²⁾	4,320	4,230	128 J	2,080	499 J	205	275	460 J	10,600	3,090 J		978
Fe ²⁺ (Ferrous Iron)	none				_,,	600					2,200		
Manganese	300 ⁽²⁾	302	292	571	484	340	291	293	889	1,400	533		1,050
Wet Chemistry (mg/L)			-	-	-		-			,			,
Nitrate (as N)	10						2.11	0.702		0.074 J			1.02
Nitrite (as N)	1						0.226	ND		ND			0.236
Chloride	250						7.42	8.31		4.12			7.48
Sulfide	none						ND	ND		ND			ND
TOC	none	0.83 J	0.77 J	ND	ND	0.989 J	0.662	0.73 J	ND	122 J	1.1 J	2.4	0.599
Water Quality Parameters		3.55 0	3			2.000	1 0.002	00	1,12	.22 0	0		2.000
pH	none	5.86		6.18	5.73	5.69	5.69	5.57	6.20	6.05	5.69	5.97	5.31
Specific Conductivity (mS/cm)	none	0.118		0.110	0.090	0.128	0.100	0.107	0.121	0.142	0.133	0.156	0.096
Dissolved Oxygen (mg/L)	none	0.110		0.68	0.030	/ 1.0	0.55 / 1.0	0.107	0.89	0.142	/ 0.8	0.37 /0.70, 0.80	1.99 / 1.0
Temperature (°C)	none	13.47		15.62	11.07	6.94	15.5	13.51	15.41	10.94	7.75	12.21	16.39
Oxygen Reduction Potential (mV)	none	-32		133	-51	88	54	73	79	-155	73	24	106
Turbidity (NTU)	none	5.42		0	1.69	0.56	0	1.78	0	-155	0.57	0.75	0

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 8 OF 15

Purpose / Notes					Downgradient N	•			
Location	NYSDOH MCLs ⁽¹⁾				SA-PZ (33-38 t				
Sample Date		7/7/2010	10/11/2010	12/14/2010	12/14/2010 (duplicate)	3/7/2011	5/9/2011	6/21/2011	9/21/2011
VOCs (µg/L)									
1,1,1-Trichloroethane (TCA)	5	73	48 J	20	21	20 J	16 J	23	46
1,1-Dichloroethane (DCA)	5	340	220	100	100	190	140	280	540
1,1-Dichloroethene (DCE)	5	23	17 J	7.6	7.9	14 J	13 J	19	25
Chloroethane (CA)	5	57	57 J	49	49	160 J	130	200	430
Benzene	5	0.81 J	0.84 J	ND	ND	1.7 J	1.9 J	ND	2.1
1,4-Dichlorobenzene	5	ND	6.1 J	7.3	7.4	26 J	37 J	26	19
1,3-Dichlorobenzene	5	ND	1.3 J	1.4 J	1.4 J	5.6 J	7.3 J	5.9 J	4.5
1,2-Dichlorobenzene	5	ND	2.3 J	2.1 J	2.2 J	7.4 J	9.8 J	7.4 J	5.9
Isopropyl Benzene	5	ND	ND	ND	ND	1.7 J	3.0 J	ND	ND
1,2,4-Trichlorobenzene	5	ND	ND	ND	ND	9.4 J	8.6 J	6.3 J	9.6
Chlorobenzene	5	ND	ND	0.73 J	ND	3.0 J	5.1 J	ND	1.7
Napthalene	50	ND	ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		493	342	177	177.9	384	299	522	1041
DCA/TCA Ratio		4.7	4.6	5.0	4.8	9.5	8.8	12.2	11.7
CA/DCA Ratio		0.17	0.26	0.49	0.49	1.2	0.93	0.71	0.80
CA/TCA Ratio		0.78	1.19	2.45	2.33	8.00	8.13	8.70	9.35
Dissolved Gases (μg/L)						•			
Methane	none	80	66	78 D	90 D	258 D		207	
Ethane	none	ND	ND	ND	ND	ND		ND	
Ethene	none	ND	ND	ND	ND	ND		ND	
Dechlorinating Bacteria (cells/mL)					•	•			
Dehalococcoides sp.	none								
Dehalobacter sp.	none								
Metals (μg/L)					•	•			
Iron	300 ⁽²⁾	93.4 J	82.4 J	2,610	2,580	1,150 J		776	
Fe ²⁺ (Ferrous Iron)	none					1,400			
Manganese	300 ⁽²⁾	4,430	5,210	5,540	5,510	5,580		5,200	
Wet Chemistry (mg/L)									
Nitrate (as N)	10			ND				ND	
Nitrite (as N)	1			ND				ND	
Chloride	250			6.65				4.51	
Sulfide	none			ND				ND	
TOC	none	1.3	0.94 J	107 J	ND	2.5 J	2.1	1.9	
Water Quality Parameters					<u> </u>				
pH	none	5.92	6.53	5.86		5.79	6.11	5.37	5.86
Specific Conductivity (mS/cm)	none	0.132	0.137	0.134		0.182	0.154	0.129	0.145
Dissolved Oxygen (mg/L)	none	0	0.57	0		/ 0.8	0 / 0.6	1.41 / 0.8	0.63 / 0.05
Temperature (°C)	none	13.80	15.34	10.79		7.43	12.08	15.42	13.66
Oxygen Reduction Potential (mV)	none	71	121	-116		58	42	0	51
Turbidity (NTU)	none	0.09	0	0		0.47	0.71	0.07	0.16

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 9 OF 15

Purpose / Notes Location	NYSDOH			Downgradient N SA-P2 (41-46	Z-158I					Downgradient I SA-PZ (33-38	'-158 11		
Sample Date	MCLs ⁽¹⁾	7/6/2010	10/11/2010	12/13/2010	3/7/2011	5/9/2011	6/20/2011	7/6/2010	10/11/2010	12/13/2010	3/7/2011	5/9/2011	6/20/2011
VOCs (μg/L)													
1,1,1-Trichloroethane (TCA)	5	51	7.9	9.4	11 J	14	13 J	66	39	49	21 J	6.5	ND
1,1-Dichloroethane (DCA)	5	230	43	42	43 J	71	63 J	340	160	200	170	110	190
1,1-Dichloroethene (DCE)	5	15	2.6 J	2.1 J	3.0 J	5.0	4.6 J	19	12	15	12 J	8.5	15
Chloroethane (CA)	5	26	ND	ND	1.6 J	14	11 J	52	27	62	130	130	170
Benzene	5	0.52 J	ND	ND	ND	ND	ND	0.77 J	0.51 J	0.77 J	1.4 J	1.5	ND
1,4-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	2.8 J	6.4	17 J	30	ND
1,3-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	0.69 J	1.3 J	3.5 J	6.0	ND
1,2-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	1.2 J	2.1 J	5.0 J	7.6	5.3 J
Isopropyl Benzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	4.7 J	2.2	ND
1,2,4-Trichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	1.4 J	2.0 J	6.9 J	6.6	6.8 J
Chlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	0.70 J	1.8 J	4.0	ND
Napthalene	50	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		322	54	54	58.6	104	91.6	477	238	326	333	255	375
DCA/TCA Ratio		4.5	5.4	4.5	3.9	5.1	4.8	5.2	4.1	4.1	8.1	16.9	
CA/DCA Ratio		0.11			0.04	0.20	0.17	0.15	0.17	0.31	0.76	1.18	0.89
CA/TCA Ratio		0.51			0.15	1.00	0.85	0.79	0.69	1.27	6.19	20	
Dissolved Gases (μg/L)													
Methane	none												
Ethane	none												
Ethene	none												
Dechlorinating Bacteria (cells/mL)													•
Dehalococcoides sp.	none												
Dehalobacter sp.	none												
Metals (μg/L)													•
Iron	300 ⁽²⁾						6,110						1,370
Fe ²⁺ (Ferrous Iron)	none				2,600						2,400		
Manganese	300 ⁽²⁾						708						5,450
Wet Chemistry (mg/L)													
Nitrate (as N)	10												
Nitrite (as N)	1												
Chloride	250												
Sulfide	none												
TOC	none					ND						2.7	
Water Quality Parameters													
pH	none	6.27	6.17	7.62	6.29	6.19	6.53	6.45	6.14	6.08	6.01	6.11	6.35
Specific Conductivity (mS/cm)	none	0.151	0.143	0.107	0.161	0.137	0.093	0.161	0.106	0.135	0.139	0.158	0.123
Dissolved Oxygen (mg/L)	none	1.57	0.27		/ 6.0	0 / 0.3	0 / 0.8	1.59	0.24	0	/ 2.0	0 / 0.6	0 / 1.0
Temperature (°C)	none	14.87	14.4	11.9	11.11	12.06	12.59	14.12	13.7	11.87	10.95	12.23	12.95
Oxygen Reduction Potential (mV)	none	-224	-76	-55	32	-29	-76	-224	-94	-119	69	16	-30
Turbidity (NTU)	none	0.56	0.30	0	0.63	2.44	83.3	1.20	0.13	0	0.83	4.15	220

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 10 OF 15

Purpose / Notes					Downgradient M				
Location	NYSDOH MCLs ⁽¹⁾				SA-PZ (41-46 f				
Sample Date		7/8/2010	10/12/2010	12/14/2010	3/7/2011	4/19/2011	4/20/2011	5/9/2011	6/21/2011
VOCs (μg/L)			•	•	•	•	•		•
1,1,1-Trichloroethane (TCA)	5	75	5.6	25	18	21 J	24 J	16	15
1,1-Dichloroethane (DCA)	5	300	35	100	65	89 J	100 J	90	130
1,1-Dichloroethene (DCE)	5	22	2.2 J	6.7	4.9	5.6 J	6.8 J	6.2	7.3
Chloroethane (CA)	5	35	3.3 J	9.7	3.3	10 J	14 J	28	99
Benzene	5	0.57 J	ND	ND	ND	ND	ND	ND	0.81 J
1,4-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	2.3
1,3-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	0.72 J
Isopropyl Benzene	5	ND	ND	ND	ND	ND	ND	ND	ND
1,2,4-Trichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	1.2
Chlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND
Napthalene	50	ND	ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		432	46	141	91.2	126	145	140	251
DCA/TCA Ratio		4.0	6.3	4.0	3.6	4.2	4.2	5.6	8.7
CA/DCA Ratio		0.12	0.09	0.10	0.05	0.11	0.14	0.31	0.76
CA/TCA Ratio		0.47	0.59	0.39	0.18	0.48	0.58	1.75	6.60
Dissolved Gases (μg/L)					•	•	•		
Methane	none	13	29	2.4	ND				39
Ethane	none	ND	ND	ND	ND				ND
Ethene	none	ND	ND	ND	ND				ND
Dechlorinating Bacteria (cells/mL)					_	-	_		
Dehalococcoides sp.	none								
Dehalobacter sp.	none								
Metals (μg/L)					•	•	•		
Iron	300 ⁽²⁾	ND	7,990	9,680	7,440 J				7,910
Fe ²⁺ (Ferrous Iron)	none				2,200				
Manganese	300 ⁽²⁾	388	799	1,090	707				845
Wet Chemistry (mg/L)				•	•	•	•		
Nitrate (as N)	10								ND
Nitrite (as N)	1								ND
Chloride	250								6.28
Sulfide	none								ND
TOC	none	0.69 J	116.16	4.70 J	1.5 J	ND		1.2	1.1
Water Quality Parameters		•		•	•	•	•		•
pH	none	5.79	6.58	7.96	6.12	5.73	6.34	6.30	7.54
Specific Conductivity (mS/cm)	none	0.129	0.159	0.117	0.129	0.148	0.144	0.140	0.109
Dissolved Oxygen (mg/L)	none		0		/ 1.0	/ 0.4	0 / 0.4	0 / 0.8	0 / 1.0
Temperature (°C)	none	14.03	15.57	11.1	11.02	10.99	10.87	14.19	13.41
Oxygen Reduction Potential (mV)	none	105	-32	-53	46	23	-1	-24	-60
Turbidity (NTU)	none	0.55	0	0.69	0.85	0	0.33	4.04	0.72

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 11 OF 15

Purpose / Notes					Downgradient N	Ionitoring Well			
Location	NYSDOH MCLs ⁽¹⁾				SA-PZ- (33-38 f				
Sample Date	WICES	7/8/2010	10/12/2010	12/14/2010	12/16/2010	3/8/2011	5/9/2011	6/21/2011	6/21/2011 (duplicate)
VOCs (μg/L)									
1,1,1-Trichloroethane (TCA)	5	41	44 J	38		13	9	3.2	2.8
1,1-Dichloroethane (DCA)	5	250	200	180		89 J	150	59	62
1,1-Dichloroethene (DCE)	5	18	14 J	12		8.8	13	3.6	3.7
Chloroethane (CA)	5	50	39 J	50		87	130	66	70
Benzene	5	0.64 J	0.52 J	ND		0.98 J	2.5	0.91 J	0.79 J
1,4-Dichlorobenzene	5	1.7 J	ND	5.4 J		17	68	21	22
1,3-Dichlorobenzene	5	ND	ND	ND		3.6	14	4.3	4.4
1,2-Dichlorobenzene	5	ND	ND	1.9 J		5.0	17	6.4	6
Isopropyl Benzene	5	0.29 J	ND	ND		0.63 J	7.1	2.6	2.5
1,2,4-Trichlorobenzene	5	ND	ND	ND		4.2	12	2.7	2.8
Chlorobenzene	5	ND	ND	ND		2.0	9.6	3.9	3.8
Napthalene	50	ND	ND	ND		ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		359	297	280		198	302	131.8	138.5
DCA/TCA Ratio		6.1	4.5	4.7		6.8	16.7	18.4	22.1
CA/DCA Ratio		0.20	0.20	0.28		0.98	0.87	1.12	1.13
CA/TCA Ratio		1.22	0.89	1.32		6.69	14	21	25
Dissolved Gases (μg/L)					•	•			
Methane	none	130 J	51 D	53 D		195 D		182 J	264 J
Ethane	none	ND	ND	ND		ND		ND	ND
Ethene	none	ND	ND	ND		ND		ND	ND
Dechlorinating Bacteria (cells/mL)				•		•			
Dehalococcoides sp.	none	2.70		12.3				50.2	
Dehalobacter sp.	none	649		15.4				6,010	
Metals (μg/L)			•	•	•	•			
Iron	300 ⁽²⁾	2,610	1,180	2,370		5,380 J		1,460	1,400
Fe ²⁺ (Ferrous Iron)	none					2,600			
Manganese	300 ⁽²⁾	4,150	6,430	6,480		7,910		4,690	4,560
Wet Chemistry (mg/L)									
Nitrate (as N)	10	ND			ND			ND	ND
Nitrite (as N)	1	ND			ND			ND	ND
Chloride	250	4.26			3.54 J			3.0	2.97
Sulfide	none	ND			ND			ND	ND
TOC	none	1.3	43.69	31.3 J		26 J	1.9	1.7	1.6
Water Quality Parameters	-	-			1				-
pH	none	6.67	6.54	7.37	5.85	5.84	6.13	7.30	
Specific Conductivity (mS/cm)	none	0.162	0.148	0.123	0.140	0.183	0.149	0.110	
Dissolved Oxygen (mg/L)	none		0.45		0	/ 0.6	0 / 0.5	0 / 1.0	
Temperature (°C)	none	13.78	15.72	11.2	11.31	10.55	14.07	13.09	
Oxygen Reduction Potential (mV)	none	-398	22	-9	-13	119	44	-18	
Turbidity (NTU)	none	-598	0	1.51	2.00	0.8	0.35	0.87	

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 12 OF 15

Purpose / Notes Location	111/CD 011				Monitoring Well Z-160I ft bgs)				Dow	sA-PZ-160I1 (33-38 ft bgs)	Vell	
Sample Date		7/7/2010	10/12/2010	12/13/2010	12/16/2010	3/8/2011	6/21/2011	7/6/2010	10/12/2010	12/13/2010	3/8/2011	6/21/2011
VOCs (μg/L)					<u> </u>							
1,1,1-Trichloroethane (TCA)	5	53	37	41		30 J	14	43	40 J	39	47	16
1,1-Dichloroethane (DCA)	5	210	150 J	160		130	85	250	200	180	210	190
1,1-Dichloroethene (DCE)	5	17	11	11		9.3 J	4.8	17	15 J	13	17	13
Chloroethane (CA)	5	26	13 J	21		11 J	6	34	42 J	33	55	140
Benzene	5	0.48 J	ND	ND		ND	ND	0.5 J	0.51 J	ND	0.82 J	ND
1,4-Dichlorobenzene	5	ND	ND	ND		ND	ND	ND	ND	ND	5.2	ND
1,3-Dichlorobenzene	5	ND	ND	ND		ND	ND	ND	ND	ND	1.2	ND
1,2-Dichlorobenzene	5	ND	ND	ND		ND	ND	ND	ND	ND	2.2	5.2 J
Isopropyl Benzene	5	ND	ND	ND		ND	ND	ND	ND	ND	ND	ND
1,2,4-Trichlorobenzene	5	1.9 J	ND	ND		0.63 J	ND	ND	ND	ND	2.7	ND
Chlorobenzene	5	ND	ND	ND		ND	ND	ND	ND	ND	0.66 J	ND
Napthalene	50	4.5 J	ND	ND		ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		306	211	233		180	110	344	297	265	329	359
DCA/TCA Ratio		4.0	4.1	3.9		4.3	6.1	5.8	5.0	4.6	4.5	12
CA/DCA Ratio		0.12	0.09	0.13		0.08	0.07	0.14	0.21	0.18	0.26	0.74
CA/TCA Ratio		0.49	0.35	0.51		0.37	0.43	0.79	1.05	0.85	1.17	8.75
Dissolved Gases (µg/L)										3133		
Methane	none	0.6	6.4	15		4.2	ND					
Ethane	none	ND	ND	ND		ND	ND					
Ethene	none	ND	ND	ND		ND	ND					
Dechlorinating Bacteria (cells/mL)												
Dehalococcoides sp.	none											
Dehalobacter sp.	none											
Metals (µg/L)						l.						
Iron	300 ⁽²⁾	1,520	38.7 J		3,340	8,060 J	11,800					2,300
Fe ²⁺ (Ferrous Iron)	none					2,600					2,200	
Manganese	300 ⁽²⁾	571	516		662	1,070	660					3,900
Wet Chemistry (mg/L)						,						.,
Nitrate (as N)	10						ND					
Nitrite (as N)	1						ND					
Chloride	250						7.6					
Sulfide	none						ND					
TOC	none	0.81 J	ND	16.8		2.8 J	1.1					
Water Quality Parameters		0.0.				0				l		
pH	none	6.05	5.78	7.42	5.88	6.36	7.74	6.17	6.15	6.06	6.08	5.70
Specific Conductivity (mS/cm)	none	0.133	0.093	0.106	0.118	0.155	0.119	0.115	0.110	0.124	0.157	0.106
Dissolved Oxygen (mg/L)	none		0.38		0	/ 0.3	0 / 1.0	1.71	0.24	0	/ 0.6	0.54 / 0.4
Temperature (°C)	none	14.10	13.0	11.8	10.87	10.8	13.26	13.97	13.0	11.56	11.03	15.3
Oxygen Reduction Potential (mV)	none	-111	151	-51	-18	49	-114	64	109	-75	78	-20
Turbidity (NTU)	none	3.04	0.31	0	1.98	0.82	0.71	1.56	0	0.33	0.85	0.27

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 13 OF 15

Purpose / Notes Location	NYSDOH				Downgradient I SA-P. (41-46	Z-161I				SA-I	PZ-408 2 ft bgs)	SA-TW-408 ⁽⁴⁾ (38-42 ft bgs)
Sample Date	- MCLs ⁽¹⁾	7/7/2010	10/12/2010	12/14/2010	3/8/2011	3/8/2011 (duplicate)	6/21/2011	9/19/2011	9/19/2011 (duplicate)	6/22/2011	9/20/2011	6/10/2011
VOCs (μg/L)												
1,1,1-Trichloroethane (TCA)	5	100	18	16	26	30	35 J	6.5	6.6	ND	60	19
1,1-Dichloroethane (DCA)	5	530	110	97	140	140	290 J	88	83	160	420	190
1,1-Dichloroethene (DCE)	5	31	6.9	5.9	10	10	13 J	5.9	5.6	13	25	11
Chloroethane (CA)	5	51	9.5	8	9.5	11	16 J	8	8.2	130	230	110
Benzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	1.6	1.1
1,4-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	5.2	2.9
1,3-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	1.3	0.64 J
1,2-Dichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	2	1.2
Isopropyl Benzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2,4-Trichlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	8.6	4.3
Chlorobenzene	5	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Napthalene	50	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		712	144	127	186	191	354	108.4	103.4	303	735	330
DCA/TCA Ratio		5.3	6.1	6.1	5.4	4.7	8.3	13.5	12.6		7.0	10
CA/DCA Ratio		0.10	0.09	0.08	0.07	0.08	0.06	0.09	0.10	0.81	0.55	0.58
CA/TCA Ratio		0.51	0.53	0.50	0.37	0.37	0.46	1.23	1.24		3.83	5.79
Dissolved Gases (μg/L)			. J.	<u>l</u>							<u>.</u>	<u>.</u>
Methane	none									180		
Ethane	none									ND		
Ethene	none									ND		
Dechlorinating Bacteria (cells/mL)			•			•	•	•	•		•	•
Dehalococcoides sp.	none											
Dehalobacter sp.	none											
Metals (µg/L)				<u>I</u>							l	· L
Iron	300 ⁽²⁾						11,800			1,400		
Fe ²⁺ (Ferrous Iron)	none				0	0						
Manganese	300 ⁽²⁾						2,770			5,000		
Wet Chemistry (mg/L)				<u> </u>			,			,		l
Nitrate (as N)	10									1.13		
Nitrite (as N)	1									ND		
Chloride	250									5.21		
Sulfide	none									ND		
TOC	none									1.6		
Water Quality Parameters			1				1	1			1	1
pH	none	5.65	6.07	5.14	5.72		6.76	6.49		5.99	6.17	5.87
Specific Conductivity (mS/cm)	none	0.129	0.124	0.090	0.114		0.182	0.296		0.136	0.140	0.171
Dissolved Oxygen (mg/L)	none	0	0		/ 1.0		0 / 0.2	0.75 / 0.0		0.98 / 1.0	0.41 / 0.20	2.99
Temperature (°C)	none	13.99	14.82	9.5	10.99		12.8	14.75		15.6	13.88	13.91
Oxygen Reduction Potential (mV)	none	4	168	142	128		-110	-61		14	135	29
Turbidity (NTU)	none	7.1	0	0	0.52		58.7	1.84		2.23	0.10	247

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 14 OF 15

Purpose / Notes				Cross-gradient F	Reference Well		
Location	NYSDOH MCLs ⁽¹⁾			SA-MW (36-46 f			
Sample Date		7/30/2008	9/3/2009	9/16/2010	9/16/2010 (duplicate)	3/10/2011	9/22/2011
VOCs (μg/L)							
1,1,1-Trichloroethane (TCA)	5	94	61	1.2 J	1.1	8.1	4.1
1,1-Dichloroethane (DCA)	5	470	270 J	9.1 J	9.3	93	71
1,1-Dichloroethene (DCE)	5	27	20	ND	ND	5.6	3.8
Chloroethane (CA)	5	63	29	ND	ND	26	8.5
Benzene	5	1.0	ND	ND	ND	ND	ND
1,4-Dichlorobenzene	5	13	3.8 J	ND	ND	ND	ND
1,3-Dichlorobenzene	5	3.0	ND	ND	ND	ND	ND
1,2-Dichlorobenzene	5	3.0	ND	ND	ND	ND	ND
Isopropyl Benzene	5	1.0	ND	ND	ND	ND	ND
1,2,4-Trichlorobenzene	5	4.0	2.7 J	ND	ND	ND	ND
Chlorobenzene	5	1.0	ND	ND	ND	ND	ND
Napthalene	50	ND	ND	ND	ND	ND	ND
Total Target VOCs (TCA, DCA, DCE, CA)		654	380	10.3	10.4	132.7	87.4
DCA/TCA Ratio		5.0	4.4	7.6	8.5	11.5	17.3
CA/DCA Ratio		0.13	0.11			0.28	0.12
CA/TCA Ratio		0.67	0.48			3.21	2.07
Dissolved Gases (μg/L)							
Methane	none		35	15	15	6.1 J	
Ethane	none		ND	ND	ND	ND	
Ethene	none						
Dechlorinating Bacteria (cells/mL)							
Dehalococcoides sp.	none						
Dehalobacter sp.	none						
Metals (μg/L)			-				
Iron	300 ⁽²⁾						
Fe ²⁺ (Ferrous Iron)	none						
Manganese	300 ⁽²⁾						
Wet Chemistry (mg/L)			•				
Nitrate (as N)	10						
Nitrite (as N)	1						
Chloride	250						
Sulfide	none						
TOC	none						
Water Quality Parameters			•	•			
pH	none	6.36	5.16	5.89		5.79	6.06
Specific Conductivity (mS/cm)	none	0.113	0.083	0.079		0.096	0.098
Dissolved Oxygen (mg/L)	none	0.44	0.19	0.25		/0.7	0.61 / 0.60
Temperature (°C)	none	13.6	13.07	13.0		6.09	13.85
Oxygen Reduction Potential (mV)	none	82	42	119		79	60
Turbidity (NTU)	none	1.35	0	0		1.44	0

TABLE A-1 GROUNDWATER DATA SOUTHERN AREA - OPTION ANALYSIS REPORT NWIRP CALVERTON, NEW YORK PAGE 15 OF 15

Shading indicates exceedance of the NYSDOH MCL

ft bgs - feet below ground surface

J qualifier - Estimated Value

ND - Not detected

- 1. New York State (NYS) Department of Health (NYSDOH) Maximum Contaminant Level (MCL). 10 NYCRR, Part 5, Subpart 5-1 Public Water Systems, Tables 1 through 3. http://www.health.ny.gov/pregulations/nycrr/title_10/part_5/sul
- 2. If iron and manganese are present, the total concentration of both should not exceed 500 µg/L.
- 3. Samples were diluted such that the concentrations of select chemicals (e.g., benzene, trichlorobenzenes and other aromatic compounds) may not have been detected at or above this limit and therefore were labeled as non-detects.
- 4. Vertical profile boring SA-TW-408 is located at a comparable screen depth (38-42 ft bgs) as SA-PZ-408, and is presented here to show a representative sample of the aquifer at this location and depth.
- -- / 0.6 = DO probe reading/ field test kit reading
- -- = Not Analyzed.

TABLE A-2 GROUNDWATER ANALYTICAL RESULTS - PUMPING TEST 1 SITE 6A-SOUTHERN AREA NWIRP CALVERTON, NEW YORK

	USEPA	NYSDEC		Constant	Rate Test		
Parameter (ug/L)	MCL	MCL	7/1	4/2010	7/15/2010		
	IVICL	IVICL	Initial	7-Hour	22-Hour	Final	
METALS (ug/L)							
IRON		300	753 J	735 J	725 J	770 J	
MANGANESE		300	1,270	1,200	1,150	1,130	
VOLATILES (ug/L)							
1,1,1-TRICHLOROETHANE	200	5	2.9 J	3.5 J	3.5 J	3.4 J	
1,1-DICHLOROETHANE	NA	5	16	18	18	19	
1,1-DICHLOROETHENE	7	5	1.1 J	1.1 J	1.2 J	0.99 J	
1,2,4-TRICHLOROBENZENE	70	5	0.68 J	5 U	5 U	5 U	
1,2-DICHLOROBENZENE	600	3	0.39 J	5 U	5 U	5 U	
1,4-DICHLOROBENZENE	75	3	5 U	5 U	0.42 J	0.4 J	
2-BUTANONE			13 U	13 U	13 U	13 U	
TOLUENE	1000	5	5 U	5 U	5 U	5 U	

Notes

ug/L - micrograms per liter

MCL - maximum contaminant level

NYSDEC - New York State Department of Environmental Conservation

USEPA - United States Environmental Protection Agency

J - Estimated Value

U - not detected above associated value

APPENDIX B AIR PERMITTING EVALUATION

CALCULATED MAXIMUM ANNUAL DAILY INFLUENT CONCENTRATIONS FENCELINE GROUNDWATER EXTRACTION, TREATMENT, AND DISCHARGE SYSTEM NWIRP CALVERTON, NEW YORK

Chemical	CAS No.	Current Maximum Influent Concentration (g/m³) (1)	Current Mean Influent Concentration (g/m³) (1)	Calculated Maximum Annual Concentration (g/m³) (2)
1,1,1-Trichloroethane	71-55-6	0.004	0.00017	63
1,1-Dichloroethane (3)	75-34-3	0.0169	0.00078	0.0077
1,1-Dichloroethene	75-35-4	0.001	0.00005	1
Chloroethane	75-00-3	0.0049	0.0002	122
Benzene	71-43-2	0.0001	0.000003	0.0024
1,4-Dichlorobenzene	106-46-7	0.0002	0.00002	0.0009
1,3-Dichlorobenzene	541-73-1	0.0001	0.000003	0.1974
1,2-Dichlorobenzene	95-50-1	0.0001	0.000005	3
Isopropyl Benzene	98-82-8	0.0002	0.00001	6
1,2,4-Trichlorobenzene	120-82-1	0.0002	0.00002	

Notes:

⁽¹⁾ Maximum and mean concentrations values are calculated using both maximum and mean Design Influent Concentrations, as presented in Table 3-1: Design Parameters, from the Basis of Design Report for Fenceline Groundwater Extraction, Treatment, and Discharge System at Site 6A - Southern Area.

⁽²⁾ Discharge Goals are based on a flow of 900 cfm, and are calculated from the Actual Annual % of AGCs from the DAR-1 Model Output to achieve air quality requirements. The summary of additional inputs for this model run is provided in the attached DAR-1 Model Output.

⁽³⁾ Current Maximum Influent Concentrations were used in this DAR-1 Analysis to identify contaminants that may trigger future treatment. The maximum concentrations for 1,1-Dichloroethane would trigger a need for treatment of air emissions if influent concentrations of this chemical remained at this high level for daily operation for a full year. Influent concentrations of this chemical will need to be monitored during initial operation of the treatment system, but concentrations of this chemical are expected to be significantly lower than this maximum concentration towards the end of the first year of operation. Note that the Calculated Maximum Annual Concentration for this chemical does not exceed the Current Mean Influent Concentration, and therefore treatment of air emissions is not recommended.

Tetra Tech NUS		STANDARD CALCULATION SHEET			
CLIENT:	FILE No:	BY:	PAGE:		
US CLEAN		SK	1 of		
SUBJECT: Calculation of Influ	ent Concentrations Fenceline	CHECKED BY:	DATE:		
Treatment System NWIRP Ca	Iverton, New York		3/20/2012		

1. Purpose:

To calculate loading rates for target contaminants to be treated by the Fenceline Groundwater Extraction and Treatment System, for input into the DAR-1 Analysis.

2. Approach:

From a list of standard conversion factors and the influent maximum and mean (average) concentrations, calculate the influent loading rate in pounds per hour and pounds per day for target chemicals.

3. List and Calculate Conversion Factors:

Conversions and Constants:

Feed Water Flow: 100 gal/min
Air Flow: 900 ft³/min

1 Liter = 0.2642 gallons
1 microgram = 0.000000001 kilograms
1 kilogram = 2.2046 lbm
1 hr = 60 minutes
1 year = 525,600 minutes

4. Calculate loading rates in pounds per hour:

Chemical	CAS No.	Influent Concentration - Maximum (µg/L)	Influent Concentration - Mean (µg/L)	Influent Loading Rate - Maximum (lb/hr)	Influent Loading Rate - Mean (lb/hr)
1,1,1-Trichloroethane	71-55-6	260	11	0.013	0.0006
1,1-Dichloroethane	75-34-3	1,100	51	0.055	0.0026
1,1-Dichloroethene	75-35-4	65	3	0.003	0.0002
Chloroethane	75-00-3	320	13	0.016	0.0007
Benzene	71-43-2	4.4	0.2	0.0002	0.00001
1,4-Dichlorobenzene	106-46-7	16	1	0.001	0.0001
1,3-Dichlorobenzene	541-73-1	4	0.2	0.0002	0.00001
1,2-Dichlorobenzene	95-50-1	6.4	0.3	0.0003	0
Isopropyl Benzene	98-82-8	11	0.4	0.001	0
1,2,4-Trichlorobenzene	120-82-1	14	1	0.001	0.0001

Tetra Tech NUS		STANDARD CALCULATION SHEET			
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SUBJECT: Calculation of Influ Treatment System NWIRP Ca		CHECKED BY:	DATE: 3/20/2012		

4. Calculate loading rates in pounds per year:

Chemical	CAS No.	Influent Concentration - Maximum (µg/L)	Influent Concentration - Mean (µg/L)	Influent Loading Rate - Maximum (lb/year)	Influent Loading Rate - Mean (lb/year)
1,1,1-Trichloroethane	71-55-6	260	11	114	4.82
1,1-Dichloroethane	75-34-3	1,100	51	482.4	22.37
1,1-Dichloroethene	75-35-4	65	3	28.5	1.32
Chloroethane	75-00-3	320	13	140.3	5.7
Benzene	71-43-2	4.4	0.2	1.9	0.09
1,4-Dichlorobenzene	106-46-7	16	1	7	0.44
1,3-Dichlorobenzene	541-73-1	4	0.2	1.8	0.09
1,2-Dichlorobenzene	95-50-1	6.4	0.3	2.8	0.13
Isopropyl Benzene	98-82-8	11	0.4	4.8	0.18
1,2,4-Trichlorobenzene	120-82-1	14	1	6.1	0.44

Tetra Tech NUS		STANDARD CALCULATION SHEET			
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US CLEAN		SK	3 of		
SUBJECT: Calculation	of Influent Concentrations Fenceline	CHECKED BY:	DATE:		
Treatment System NW	IRP Calverton, New York		3/20/2012		

1. Purpose:

To calculate influent concentrations for target contaminants to be treated by the Fenceline Groundwater Extraction and Treatment System, to verify previous analysis.

2. Approach:

From a list of standard conversion factors and the influent maximum and mean (average) concentrations, calculate the influent concentrations in parts per million by volume of air for target chemicals.

3. List and Calculate Conversion Factors:

Feed Water Flo Air Flow:	DW:		100 gal/min 900 ft ³ /min		=	23 m ³ /hr 1500 m ³ /hr
1	cubic meter	=	26	64.17	gallons	
1	hour	=		60	minutes	
1	day	=		1440	minutes	
1	microgram	=	0.00	00001	grams	
1	cubic foot	=	0.	.0283	cubic meters	
1	cubic meter	=	•	1,000	L	
	R	=	0.000	0821	m ³ atm/mole ^o K	
Т	_ =		50 °F		=	283.15 °K
	Р	=		1	atmosphere	

4. Convert Influent concentrations in μg/L to g/m³

Chemical	CAS No.	Influent Concentration - Maximum (µg/L)	Influent Concentration - Mean (µg/L)	Influent Concentration - Maximum (g/m³)	Influent Concentration - Mean (g/m ³)
1,1,1-Trichloroethane	71-55-6	260	11	0.004	0.00017
1,1-Dichloroethane	75-34-3	1,100	51	0.0169	0.00078
1,1-Dichloroethene	75-35-4	65	3	0.001	0.00005
Chloroethane	75-00-3	320	13	0.0049	0.0002
Benzene	71-43-2	4.4	0.2	0.0001	0.000003
1,4-Dichlorobenzene	106-46-7	16	1	0.0002	0.00002
1,3-Dichlorobenzene	541-73-1	4	0.2	0.0001	0.000003
1,2-Dichlorobenzene	95-50-1	6.4	0.3	0.0001	0.000005
Isopropyl Benzene	98-82-8	11	0.4	0.0002	0.00001
1,2,4-Trichlorobenzene	120-82-1	14	1	0.0002	0.00002

Tetra Tech NUS		STANDARD CALCULATION SHEET		
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SUBJECT: Calculation of Influent Concentrations Fenceline Treatment System NWIRP Calverton, New York		CHECKED BY:	DATE: 3/20/2012	

$\underline{\text{5. Calculate Chemical Concentration in Parts Per Million Volume from Concentration in } g/m^3}$

Equation: PV = nRT or V = nRT/P

Chemical	CAS No.	Molecular Mass (grams per mole)	Influent Concentration - Maximum (ppmv)	Influent Concentration - Mean (ppmv)
1,1,1-Trichloroethane	71-55-6	133.4	0.697	0.0296
1,1-Dichloroethane	75-34-3	98.96	3.97	0.1832
1,1-Dichloroethene	75-35-4	96.94	0.2398	0.012
Chloroethane	75-00-3	64.51	1.7657	0.0721
Benzene	71-43-2	78.11	0.0298	0.0009
1,4-Dichlorobenzene	106-46-7	147	0.0316	0.0032
1,3-Dichlorobenzene	541-73-1	147	0.0158	0.0005
1,2-Dichlorobenzene	95-50-1	147	0.0158	0.0008
Isopropyl Benzene	98-82-8	120.19	0.0387	0.0019
1,2,4-Trichlorobenzene	120-82-1	181.45	0.0256	0.0026

Tetra Tech NUS		STANDARD CALCULATION SHEET		
CLIENT:	FILE No:	BY:	PAGE:	
US CLEAN		SK	5 of	
SUBJECT: Calculation of Influent Concentrations Fenceline		CHECKED BY:	DATE:	
Treatment System NWIRP (Calverton, New York		3/20/2012	

1. Purpose:

To verify current discharge limits for for target contaminants to be treated by the Fenceline Groundwater Extraction and Treatment System.

2. Approach:

From the Contaminant Assessment Summary of the DAR-1 Model output for target contaminants (see DAR-1 output for analysis inputs), use the Actual Annual % of the Annual Guideline Concentration (AGC), a current average flow rate of 900 cubic feet per minute (cfm), and influent chemical emission rates in pounds per hour (lb/hour) and pounds per year (lb/year) to back calculate current discharge goals.

3. Calculation of Current Discharge Goals:

Chemical	Current Actual Annual % of AGC ⁽¹⁾	Current Maximum Concentration (g/m³) ⁽²⁾	Current Chemical Emission Rate Prior to Treatment (lb/hour) ⁽³⁾	Current Chemical Emission Rate Prior to Treatment (lb/year) ⁽³⁾	Calculated Discharge Goal (lb/hr) ⁽⁴⁾	Calculated Discharge Goal (lb/year) ⁽⁴⁾	Maximum Allowable Concentration (g/m³) ⁽⁴⁾
1,1,1- Trichloroethane	0.0064	0.0040	0.0135	118	211	1,800,000	63
1,1- Dichloroethane	215.8	0.0169	0.0569	499	0.026	231	0.0077
1,1- Dichloroethene	0.1147	0.0010	0.0034	30	3	30,000	1
Chloroethane	0.0040	0.0049	0.0165	145	413	3,600,000	122
Benzene	4.119	0.0001	0.0003	3	0.008	72	0.0024
1,4- Dichlorobenzene	21.92	0.0002	0.0007	6	0.003	27	0.0009
1,3- Dichlorobenzene	0.0507	0.0001	0.0003	3	0.665	10,000	0.1974
1,2- Dichlorobenzene	0.0039	0.0001	0.0003	3	9	100,000	3
Isopropyl Benzene	0.0034	0.0002	0.0007	6	20	200,000	6
1,2,4- Trichlorobenzene	0	0.0002	0.0007	6			

Notes:

⁽¹⁾ Actual Annual % of the AGCs is from the attached DAR-1 Model Output.

⁽²⁾Values were taken from Table 3-1: Design Parameters of the Basis of Design Report for Fence Line Groundwater Extraction, Treatment, and Discharge System at Site 6A - Southern Area.

⁽³⁾ Chemical Emission Rates were calculated from maximum concentrations and an average flow rate of 900 cfm.

⁽⁴⁾Discharge Goals are based on a flow of 900 cfm, and calculated from the Actual Annual % of the AGCs from the DAR-1 Model Output to achieve air quality requirements. The summary of additional inputs for this model run is provided in the DAR-1 Model Output. Stack height is 20 feet, and the property line was evaluated at a distance of 75 feet.

CALVERTON FENCELINE GROUNDWATER EXTRACTION, TREATMENT, AND DISCHARGE SYSTEM AIR STRIPPER STACK EMISSIONS DAR-1 MODEL OUTPUT, POINT SOURCE (STACK EMISSIONS) TYPE

I. Summary of Inputs for Model Run to Nearest Property Line (75 feet), worst case scenario (highest contaminant concentrations in groundwater)

Chemical	CAS No.	Influent Loading Rate - Maximum (lb/hr)	Influent Loading Rate - Maximum (lb/year)	Maximum Concentration of Untreated Off Gas ⁽¹⁾ (g/m³)
1,1,1-Trichloroethane ⁽²⁾	71-55-6	0.013	114	0.004
1,1-Dichloroethane (2)	75-34-3	0.055	482.4	0.0169
1,1-Dichloroethene ⁽²⁾	75-35-4	0.003	28.5	0.001
Chloroethane ⁽²⁾	75-00-3	0.016	140.3	0.0049
Benzene	71-43-2	0.0002	1.9	0.0001
1,4-Dichlorobenzene	106-46-7	0.001	7	0.0002
1,3-Dichlorobenzene	541-73-1	0.0002	1.8	0.0001
1,2-Dichlorobenzene	95-50-1	0.0003	2.8	0.0001
Isopropyl Benzene	98-82-8	0.001	4.8	0.0002
1,2,4-Trichlorobenzene	120-82-1	0.001	6.1	0.0002

НА	Height Above stack/ maximum height of plume (HA, feet)	15
SH	Stack Height/Treatment Building Air Stack (SH, feet)	20
D	Stack Diameter (D, inches)	6
Т	Stack Exit Temperature (T, degrees Fahrenheit)	50
V	Stack Exit Velocity (V, ft/sec)	76.4
Q ⁽³⁾	Stack Exit Flow Rate [Q, Actual Cubic Feet per Minute (ACFM)]	900
Dpl	Shortest Distance from Source Building (Treatment Building) to Property Line (Dpl, feet) for point sources	75
BW	Building Width (BW, feet) of Source Building (Treatment Building) for point sources	25
BL	Building Length (BL, feet) of Source Building (Treatment Building)	35
Q	Actual Hourly Emission Rate (lbs/hour) for source contaminant	Chemical specific, see above
Qa	Actual Annual Emission Rate (lbs/year) for source contaminant	Chemical specific, see above

⁽¹⁾ Emission rates and maximum concentration values are calculated using both maximum and mean Design Influent Concentrations as presented in Table 3-1: Design Parameters from the Basis of Design Report for Fence Line Groundwater Extraction, Treatment, and Discharge System at Site 6A – Southern Area.

⁽²⁾Only the first four chemicals listed in the summary of inputs will have a full printout from the DAR-1 Analysis, provided in sections four through seven.

(3) "Q" is the design flow rate of 900 cubic feet per minute, but flow rates actual flow rates will be in the range of 600 to 900 cubic feet per minute.

II. Contaminant Assessment Summary of All Relevant Chemicals:

	CONTAMINANT	ASSESSMENT SU SHORT-TERM	MMARY OF DAR-1		3/23/12 Page 1 AREA SOURCE
CAS NUMBER	AGC ug∕m3	MAXIMUM (Cav.Pt.Area) % OF SGC	ACTUAL ANNUAL % OF AGC	POTENTIAL ANNUAL % OF AGC	ACTUAL ANNUAL % OF AGC
00071-43-2 $00071-55-6$ $00075-00-3$ $00075-34-3$ $00075-35-4$ $00095-50-1$ $00098-82-8$ $00106-46-7$ $00120-82-1$ $00541-73-1$	0.13000000 5000.000000000 10000.000000000 0.63000000 70.000000000 400.00000000 0.090000000	0.0111 0.1041 0.0000 0.0000 0.0000 0.0007 0.0000 0.0195 0.0000	0 . 0000 0 . 0000	3.7940 0.0064 0.0039 215.2921 0.1057 0.0037 0.0062 27.4008 0.0000	0.0064 0.0040 215.8066 0.1147 0.0039 0.0034 21.9207 0.0000
SUMMARY I	OTALS	0.1354	0.0000	246.6622	242.0296

Notes:

Current Maximum Influent Concentrations were used in this DAR-1 Analysis to identify contaminants that may trigger future treatment. The maximum concentrations for 1,1-Dichloroethane would trigger a need for treatment of air emissions if influent concentrations of this chemical remained at this high level for daily operation for a full year. Influent concentrations of this chemical will need to be monitored during initial operation of the treatment system, but concentrations of this chemical are expected to be significantly lower than this maximum concentration towards the end of the first year of operation. Note that the Calculated Maximum Annual Concentration for this chemical does not exceed the Current Mean Influent Concentration, and therefore treatment of air emissions is not recommended. See Table 1: Calculated Maximum Annual Daily Influent Concentrations for comparison.

III. Contaminant Impact Summary of All Relevant Chemicals:

III. Co	mammanı impaci Sumi	nary of All Relevant	Chemicais.		
	CONTAMIN	MNT IMPACT SUM	MARY OF DAR-1	ANALYSIS	3/23/12 Page 1
		SHORT-TERM	CAUITY	POINT or A	REA SOURCE
CAS NUMBER	AGC ug/m3	MAXIMUM (Cav.Pt.Area) ug/m3	ACTUAL ANNUAL ug/m3	POTENTIAL ANNUAL ug/m3	ACTUAL ANNUAL ug∕m3
00071-43-2 00071-55-6 00075-00-3 00075-34-3 00075-35-4 00075-50-1 00098-82-8	5000.00000000 10000.00000000 0.63000000 70.00000000 200.00000000 400.00000000	0.144143149 9.369304660 11.531451200 39.639366100 2.162147280 0.216214716 0.720715702	0.000000000 0.00000000 0.00000000 0.000000	0.004932147 0.320589572 0.394571781 1.356340530 0.073982209 0.007398221 0.024660736	0.005354903 0.321294164 0.395417292 1.359581655 0.080323541 0.007891436 0.013528175
00106-46-7 00120-82-1 00541-73-1	*****	0.720715702 0.720715702 0.144143149	0.000000000 0.000000000 0.000000000	0.024660736 0.024660736 0.004932147	0.019728589 0.017192056 0.005073066

IV. Contaminant Impact Summary Step by Step Menu for 1,1,1-Trichloroethane: ****** CALUERTON. NEW YORK NWIRP CALUERTON SUFFOLK EMISSION POINT = TOTAL CAS NUMBER = 00071-55-6 SIC = Ø 5000.000000000 ug/m3 SGC = AGC = 9000.000000 ug/m3 20., D= 6 25., BL= 6., T= 51., U= 35., ×CONTROL= 15., SH= 75., BW= 76.40, q= STACK: HA= 900.00 BUILDING: Dol= 0.0000 Reported Hourly Emission Rate (Q) is equal to 0.0130000000 lbs/hour. ** Reported Annual Emission Rate (Qa) is equal to 114.000000 lbs/year. II.B. REFINED CAUITY IMPACT METHOD (DAR-1, APPENDIX B). Shortest Distance from building to Property Line (75. feet) exceeds the cavity length, or 3 times the building height (15. feet). Therefore, this buildings cavity impacts (if they occur) are confined to on site receptors. Computer will assume the CAVITY Annual Impact equals 0.00 ug/m3. II.B.1. II.C. CAUITY Annual Impact (0.000 ug/m3) is less than AGC 5000.000 ug/m3). III.A. STANDARD POINT SOURCE METHOD (DAR-1, APPENDIX B). III.A.1.c. Buoyancy flux, F, is equal to 0.002 m(4)/sec(2). III.A.1.d. Effective stack height, he, is equal to 20.059 feet. STANDARD POINT SOURCE Actual Annual Impact is equal III.A.2. 0.803 ug/m3 for 8769. hours/year of operation. STANDARD POINT SOURCE Potential Annual Impact is equal to 0.801 ug/m3 assuming 8,760 hours/year of operation. III.A.3. Stack height to building height ratio is greater than 2.5 (GEP stack). Computer will multiply actual annual & potential annual impacts by 0.4 factor. III.A.4.b. STANDARD POINT SOURCE Short-Term Impact is calculated below using the DAR-1 SOFTWARE PROGRAM SHORT-TERM METHOD. III.A.5. STANDARD POINT SOURCE Actual Annual Impact (less than AGC (5000.000 ug/m3). III.D. 0.321 ug/m3) is STANDARD POINT SOURCE Potential Annual Impact (is less than AGC (5000.000 ug/m3). III.D. 0.321 ug/m3 >

- **** Potential Annual Impact is based upon 8760 hours/year **** operation instead of reported 8769. hours/year. *** *** DAR-1 SOFTWARE PROGRAM SHORT-TERM METHOD.
 See "Technical Reference for the Screening Procedures of the DAR-1 Software Program, Wade/Sedefian,' 1/11/94. 2.0 2.2 CAUITY Short-Term Impact is equal to 0.00 ug/m3 as the plume escaped the cavity region: hs(20. feet) > hc(5. feet). CAUITY Short-Term Impact (than SGC (9000.000 ug/m3). II.C. 0.000 ug/m3) is less 2.3 Buoyancy flux, F, is equal to 0.002 m(4)/sec(2). Effective stack height, he, is equal to 20.059 feet. 2.3 Maximum non-downwash GEP stack Short-Term Impact (CSTP) is equal to 9.369 ug/m3, for hs/hb = 4.002.4 Maximum non-cavity Short-Term Impact (CST: 9.369 ug/m3 less than the SGC (9000.000 ug/m3) for the point source. III.D. 9.369 ug/m3) is
- 2.7 Maximum Short-Term cavity, point, or area source impact
 (SHORT-TERM MAXIMUM, (Cav,Pt,Area)) equals 9.369 ug/m3
 and is reported in the ANALYSIS MENU. This value is less than
 the SGC (9000.000 ug/m3).

Contaminant Impact Summary Step by Step Menu for 1,1-Dichloroethane: NWIRP CALUERTON CALUERTON, NEW YORK SUFFOLK TOTAL CAS NUMBER = 00075-34-3 Ø EMISSION POINT = SIC = AGC = 0.630000000 ug/m3 SGC = 0.000000 ug/m3 STACK: HA= BUILDING: Dp1= 15., SH= 75., BW= 20., D= 6., T= 51., U= 76.40, q= 25., BL= 35., \times CONTROL= 0.0000 900.00 0.055000000 lbs/hour. ** Reported Hourly Emission Rate (Q) is equal to ** Reported Annual Emission Rate (Qa) is equal to 482.400000 lbs/year. II.B. REFINED CAUITY IMPACT METHOD (DAR-1, APPENDIX B). Shortest Distance from building to Property Line (75. feet) exceeds the cavity length, or 3 times the building height (15. feet). Therefore, this buildings cavity impacts (if they occur) are confined to on site receptors. Computer will assume the CAVITY Annual Impact equals 0.00 ug/m3. II.B.1. II.C. CAUITY Annual Impact (0.000 ug/m3) is less than AGC 0.630 ug/m3).

III.A. STANDARD POINT SOURCE METHOD (DAR-1, APPENDIX B). Buoyancy flux, F, is equal to III.A.1.c. И.ИИ2 m(4)/sec(2). III.A.1.d. Effective stack height, he, is equal to 20.059 feet. STANDARD POINT SOURCE Actual Annual Impact is equal to 3.399 ug/m3 for 8771. hours/year of operation. III.A.2. STANDARD POINT SOURCE Potential Annual Impact is equal to 3.391 ug/m3 assuming 8,760 hours/year of operation. III.A.3. Stack height to building height ratio is greater than 2.5 (GEP stack). Computer will multiply actual annual & potential annual impacts by 0.4 factor. III.A.4.b. STANDARD POINT SOURCE Short-Term Impact is calculated below using the DAR-1 SOFTWARE PROGRAM SHORT-TERM METHOD. III.A.5. STANDARD POINT SOURCE Potential Annual Impact (is greater than AGC (0.630 ug/m3). III.D. 1.356 ug/m3) **** Potential Annual Impact is based upon 8760 hours/year **** operation instead of reported 8771. hours/year. *** DAR-1 SOFTWARE PROGRAM SHORT-TERM METHOD.
See "Technical Reference for the Screening Procedures of the DAR-1 Software Program, Wade/Sedefian,' 1/11/94. 2.0 2.2 CAUITY Short-Term Impact is equal to 0.00 ug/m3 as the plume escaped the cavity region: hs(20. feet) > hc(5. feet). CAUITY Short-Term Impact is equal to There is no SGC for this contaminant. II.C. 0.000 ug/m3. 2.3 Buoyancy flux. F. is equal to 0.002 m(4)/sec(2). 2.3 Effective stack height, he, is equal to 20.059 feet. Maximum non-downwash GEP stack Short-Term Impact (CSTP) is equal to 39.639 ug/m3, for hs/hb = 4.00 2.4 Maximum non-cavity Short-Term Impact (CST) equals 39.6 for the point source. There is no SGC for this contaminant. III.D. 39.639 ug/m3

Maximum Short-Term cavity, point, or area source impact (SHORT-TERM MAXIMUM, (Cav.Pt.Area)) equals 39.639 and is reported in the ANALYSIS MENU.

39.639 ug/m3

2.7

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VI.
            Contaminant Impact Summary Step by Step Menu for 1,1-Dichloroethene:
 NWIRP CALUERTON
                                               CALUERTON, NEW YORK
                                                                                             SUFFOLK
EMISSION POINT =
                                       TOTAL
                                                      CAS NUMBER = 00075-35-4
                                                                                               SIC =
    AGC =
                            70.000000000 ug/m3
                                                                  SGC =
                                                                                          0.000000 ug/m3
                         15., SH= 20., D= 6., T= 51., U= 75., BW= 25., BL= 35., ×CONTROL=
                                                                                     76.40, q=
0.0000
STACK: HA=
BUILDING: Dp1=
                                                                                                          900.00
** Reported Hourly Emission Rate (Q) is equal to
                                                                                    0.003000000 1bs/hour.
** Reported Annual Emission Rate (Qa) is equal to
                                                                                    28.500000 lbs/year.
II.B.
           REFINED CAUITY IMPACT METHOD (DAR-1. APPENDIX B).
                   Shortest Distance from building to Property Line ( 75. feet ) exceeds the cavity length, or 3 times the building height ( 15. feet ). Therefore, this buildings cavity impacts (if they occur) are confined to on site receptors. Computer will assume the CAVITY Annual Impact equals 0.00 ug/m3.
II.B.1.
           CAVITY Annual Impact ( 70.000 ug/m3 ).
                                                     0.000 ug/m3 ) is less than AGC
II.C.
III.A. STANDARD POINT SOURCE METHOD (DAR-1, APPENDIX B).
III.A.1.c.
                          Buoyancy flux, F, is equal to
                                                                              0.002 m(4)/sec(2).
III.A.1.d.
                           Effective stack height, he, is equal to
                                                                                           20.059 feet.
                   STANDARD POINT SOURCE Actual Annual Impact is equal to 0.201 ug/m3 for 9500. hours/year of operation.
III.A.2.
III.A.3.
                   STANDARD POINT SOURCE Potential Annual Impact is equal
                               0.185 ug/m3 assuming 8,760 hours/year of operation.
                   to
                          Stack height to building height ratio is greater than 2.5 (GEP stack). Computer will multiply actual annual & potential annual impacts by 0.4 factor.
III.A.4.b.
                   STANDARD POINT SOURCE Short-Term Impact is calculated below using the DAR-1 SOFTWARE PROGRAM SHORT-TERM METHOD.
III.A.5.
           STANDARD POINT SOURCE Actual Annual Impact ( less than AGC ( 70.000 ug/m3 ).
III.D.
                                                                                      0.080 \text{ ug/m}3 ) is
            STANDARD POINT SOURCE Potential Annual Impact ( is less than AGC ( 70.000 ug/m3 ).
                                                                                          0.074 ug/m3 >
III.D.
```

- **** Potential Annual Impact is based upon 8760 hours/year
 **** operation instead of reported 9500. hours/year. DAR-1 SOFTWARE PROGRAM SHORT-TERM METHOD.
 See "Technical Reference for the Screening Procedures of the DAR-1 Software Program, Wade/Sedefian,' 1/11/94. 2.0 CAUITY Short-Term Impact is equal to 0.00 ug/m3 as the plume escaped the cavity region: hs(20. feet) > hc(5. feet). 2.2 CAUITY Short-Term Impact is equal to There is no SGC for this contaminant. II.C. 0.000 ug/m3. 2.3 Buoyancy flux, F, is equal to 0.002 m(4)/sec(2). 2.3 Effective stack height, he, is equal to 20.059 feet. Maximum non-downwash GEP stack Short-Term Impact (CSTP) is equal to 2.162 ug/m3, for hs/hb = 4.002.4 Maximum non-cavity Short-Term Impact (CST) equals 2.1 for the point source. There is no SGC for this contaminant. III.D. 2.162 ug/m3
- 2.7 Maximum Short-Term cavity, point, or area source impact (SHORT-TERM MAXIMUM, (Cav.Pt.Area)) equals 2.162 ug/m3 and is reported in the ANALYSIS MENU.

Contaminant Impact Summary Step by Step Menu for Chloroethane: VII. NWIRP CALUERTON CALUERTON, NEW YORK SUFFOLK EMISSION POINT = TOTAL CAS NUMBER = 00075-00-3 SIC = AGC = 10000.0000000000 ug/m3 SGC = 0.000000 ug/m3 STACK: HA= BUILDING: Dp1= 15., SH= 20., D= 6., T= 51., V= 76.40, q= 75., BW= 25., BL= 35., %CONTROL= 0.0000 900.00 ** Reported Hourly Emission Rate (Q) is equal to 0.016000000 lbs/hour. ** Reported Annual Emission Rate (Qa) is equal to 140.300000 lbs/year. REFINED CAUITY IMPACT METHOD (DAR-1, APPENDIX B). II.B. Shortest Distance from building to Property Line (75. feet) exceeds the cavity length, or 3 times the building height (15. feet). Therefore, this buildings cavity impacts (if they occur) are confined to on site receptors. Computer will assume the CAVITY Annual Impact equals 0.00 ug/m3. II.B.1. II.C. CAVITY Annual Impact (0.000 ug/m3) is less than AGC (10000.000 ug/m³).

- III.A. STANDARD POINT SOURCE METHOD (DAR-1, APPENDIX B). III.A.1.c. Buoyancy flux, F, is equal to 0.002 m(4)/sec(2). III.A.1.d. Effective stack height, he, is equal to 20.059 feet. STANDARD POINT SOURCE Actual Annual Impact is equal to 0.989 ug/m3 for 8769. hours/year of operation. III.A.2. STANDARD POINT SOURCE Potential Annual Impact is equal III.A.3. 0.986 ug/m3 assuming 8,760 hours/year of operation. Stack height to building height ratio is greater than 2.5 (GEP stack). Computer will multiply actual annual & potential annual impacts by 0.4 factor. III.A.4.b. STANDARD POINT SOURCE Short-Term Impact is calculated below using the DAR-1 SOFTWARE PROGRAM SHORT-TERM METHOD. III.A.5. STANDARD POINT SOURCE Actual Annual Impact (less than AGC (10000.000 ug/m3). III.D. 0.395 ug/m3) is STANDARD POINT SOURCE Potential Annual Impact (is less than AGC (10000.000 ug/m3). III.D. 0.395 ug/m3 >
- **** Potential Annual Impact is based upon 8760 hours/year **** operation instead of reported 8769. hours/year. *** DAR-1 SOFTWARE PROGRAM SHORT-TERM METHOD.
 See "Technical Reference for the Screening Procedures of the DAR-1 Software Program, Wade/Sedefian,' 1/11/94. 2.0 CAUITY Short-Term Impact is equal to 0.00 ug/m3 as the plume escaped the cavity region: hs(20. feet) > hc(5. feet). 2.2 CAUITY Short-Term Impact is equal to There is no SGC for this contaminant. II.C. 0.000 ug/m3. 2.3 Buoyancy flux, F, is equal to 0.002 m(4)/sec(2). 2.3 Effective stack height, he, is equal to 20.059 feet. Maximum non-downwash GEP stack Short-Term Impact (CSTP) is equal to 11.531 ug/m3, for hs/hb = 4.002.4 Maximum non-cavity Short-Term Impact (CST) equals 11.5 for the point source. There is no SGC for this contaminant. III.D. 11.531 ug/m3
- 2.7 Maximum Short-Term cavity, point, or area source impact (SHORT-TERM MAXIMUM, (Cav.Pt.Area)) equals 11.531 ug/m3 and is reported in the ANALYSIS MENU.

VIII. Contaminant Summary AGCs and SGCs for All Relevant Chemicals:

	AGCs & SGCs			Pag	3/23/ ge	12 1
CAS NUMBER CONTAMINANT NAME 90071-43-2 BENZENE 90071-55-6 METHYL CHLOROFORM 90075-00-3 ETHYL CHLORIDE 90075-35-4 UINYLIDENE CHLORIDE 90095-50-1 DICHLOROBENZENE, O- 90098-82-8 CUMENE 90106-46-7 DICHLOROBENZENE, P- 90120-82-1 TRICHLOROBENZENE, M-	ug/m3 1300.00000 9000.00000 0.00000 0.00000 30000.00000 0.00000 0.00000	W*DE Z	0.130000000 5000.000000000 10000.000000000 0.634400000 200.000000000 200.000000000 400.000000000 0.090000000	W PE	CODE H U HA L HI L HI I HI I H I U HI	

IX. Contaminant Emissions Summary All Relevant Chemicals:

171.	ontaminant Emissions Cam	mary 7 m r tolo	vant Onomicalo.	
	CONTAI	MINANT EMI	SSIONS SUMMARY	3/23/12 Page 1
CAS NUMBER	CONTAMINANT NAME	NUM. OF EPS PER CONTAM.	EMISSIONS (lbs/hour)	EMISSIONS (1bs/year)
00075-00-3 00075-34-3 00075-35-4 00095-50-1 00098-82-8 00106-46-7	METHYL CHLOROFORM ETHYL CHLORIDE BICHLOROETHAME, 1, 1 UINYLIDENE CHLORIDE DICHLOROBENZENE, O-	1 1 1 1 1 1 1 1	0.0002000 0.0130000 0.0160000 0.0550000 0.0030000 0.0010000 0.0010000	140.30000 482.40000
00541-73-1 Summary	DICHLOROBENZENE, m- TOTALS	1 10	0.0002000 0.0907000	1.80000 789.60000

APPENDIX C
PROCESS CALCULATIONS

C-1 Hydraulic Calculations

Prepared By: SK Checked By: HKM Date: April 18, 2012

Extraction Well Self Priming Pump Calculation

Slab Elevation	39.00			
P atmos	33.00	ft (water	-)	
Static water level in well	32.00	EL		
Drawdown (during pumping)	5.00	feet		
Water level in well during pumping	27.00	EL		
Pump suction CL above slab	1.50	ft +/-		
Center line of Pump EL	40.50			
Suction Lift	13.50	ft		
Height of discharge line	10.00	ft		
Total static head	23.50	ft		
Suction Piping				
Length of suction piping	120	feet		
Number of elbows	8	K =	0.54	cameron hydraulic data
Foot valve	0		0 psi for op	ening (Chemline Footvalve)
Discharge Piping				
Length of discharge piping	30	feet		
Number of elbows	8	K =	0.54	cameron hydraulic data
Check Valve	1		1.4 psi for op	ening (Chemline Checkvalve)
Flow Throttling Valve	TBD			

Applying Hazen williams for the puspose of making calcs more automated

Mag flow meter

 $hf = 0.002083 \times L \times (100/C)^1.85 \times (q^1.85) / (d^4.8655)$

Assume plastic pipe C = 140

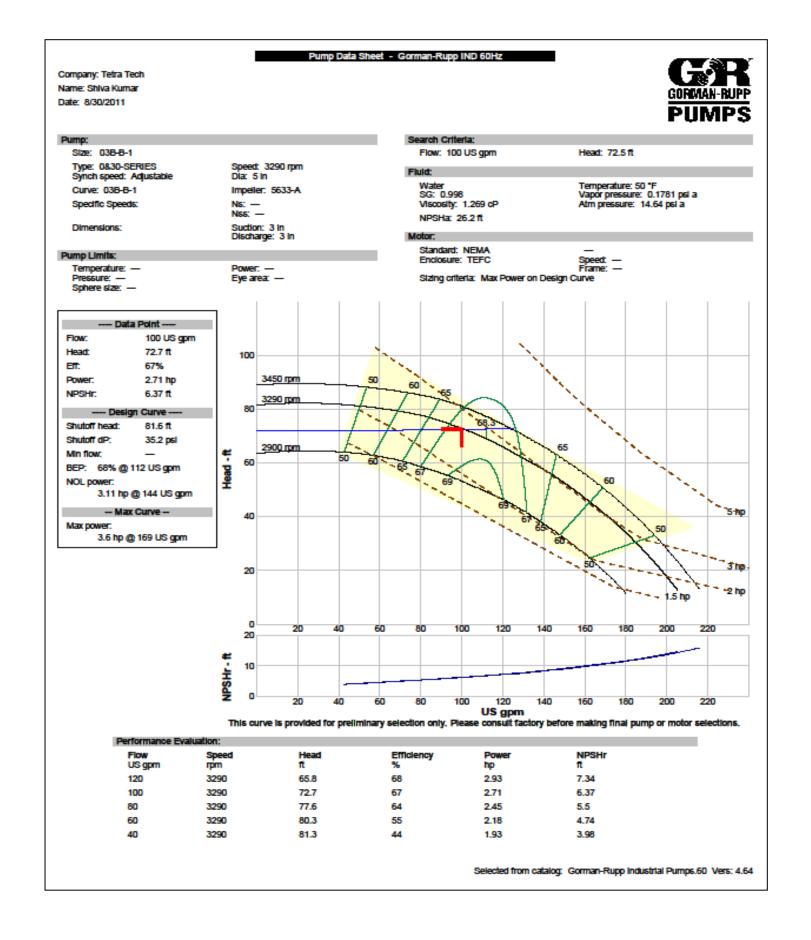
Flow Meter

Water Temperature 60 F

Vapor pressure 0.6 ft of water

The system has been setup so that one pump can operate at 100 gpm OR two pumps will operate so that each pump's output is 70 gpm.

Schedule 40 PVC		Suction Pipe							<u>Discharge Pipe</u>						
Flow; gpm	Pipe dia, inch	Velocity, ft/sec	Friction loss of straight pipe (ft)		Foot Valve (3-inch)	Total Friction Loss, ft	NPSHA	NPSHR	Pipe dia, inch	Velocity, ft/sec	Int straight	Friction loss for elbows	Check Valve (3- inch)	Total Friction Loss, ft	TDH, ft
70	3.068	3.0	1.5	0.6	0.00	2.1	16.79	5	3.068	3.0	0.4	0.6	3.23	4.2	29.8
100	3.068	4.3	2.9	1.3	0.00	4.1	14.76	7	3.068	4.3	0.7	1.3	3.23	5.2	32.9



Prepared By: SK Checked By: HKM Date: April 18, 2012

Injection Well Pump Calculation

Slab Elevation	39.00			
P atmos	33.00	ft (water)		
Static water level in well	32.00	EL		
Water rise (during pumping)	3.00	feet		
Water level in well during pumping	35.00	EL		
Water Level above slab	1.50	ft +/-		
Water Level above slab	40.50			
Total static head	-5.50	ft	-ve since	water is pumped downgradient;
Suction Piping				
Length of piping	20	feet		
Number of elbows	4	K =	0.54	cameron hydraulic data
Discharge Piping				
Length of discharge piping	600	feet		
Number of elbows	20	K =	0.54	cameron hydraulic data
Check Valve	1		1.4 psi for op	ening (Chemline checkvalve)
Pressure drop across dirty bag filter	10	psi		
pressure drop across clean filter	3	psi		

Applying Hazen williams for the puspose of making calcs more automated

hf = 0.002083 x L x (100/C)^1.85 x (q^1.85) / (d^4.8655)

Assume plastic pipe C = 140

Water Temperature 60 F

Vapor pressure 0.6 ft of water

Two injection pumps (1 duty + 1 standby) will be provided so that each can operate at 100 to 140 gpm.

The pumps will be provided with a VFD to maintain a constat level in the A/S sump.

Prepared By: SK Checked By: HKM Date: April 18, 2012

Schedule 80 PVC	Suction Pipe					Discharge Pipe							
Flow; gpm	Pipe dia, inch	Velocity, ft/sec	ot straight	Friction loss for elbows	Total Friction Loss, ft	Pipe dia, inch	Velocity, ft/sec		Friction loss for elbows	Check Valve (3-	Bag filter pressure loss (max), ft	Total Friction Loss, ft	TDH, ft
70	2.9	3.4	0.3	0.4	0.7	2.9	3.4	9.8	1.9	3.23	23.03	38.0	33.2
100	2.9	4.9	0.6	0.8	1.4	2.9	4.9	18.9	4.0	3.23	23.03	49.1	45.1
140	2.9	6.8	1.2	1.6	2.7	2.9	6.8	35.2	7.8	3.23	23.03	69.3	66.5

Schedule 80 PVC	Suction Pipe					Discharge Pipe							
Flow; gpm	Pipe dia, inch	Velocity, ft/sec	Friction loss of straight pipe (ft)	Friction loss for elbows	Total Friction Loss, ft	Pipe dia, inch	Velocity, ft/sec		Friction loss for elbows	Check Valve (3-	pressure	Total Friction Loss, ft	TDH, ft
70	2.9	3.4	0.3	0.4	0.7	2.9	3.4	9.8	1.9	3.23	6.91	21.9	17.1
100	2.9	4.9	0.6	0.8	1.4	2.9	4.9	18.9	4.0	3.23	6.91	33.0	28.9
140	2.9	6.8	1.2	1.6	2.7	2.9	6.8	35.2	7.8	3.23	6.91	53.1	50.4

C-2 Bag Filter Dirt Holding Capacity

Checked By: DB Date: April 18, 2012

Prepared By: SK

Dirt Holding Capacity of Filter

LR-6		
Number of housings	2	
Number of filters	6	
Dirt holding capacity of one filter	1.75	kg/filter
Net dirt holding capacity per housing	10.5	kg/housing
Fe(III)	1200	ug/l
Fe(OH)3	2.29	mg/l
Flow	100	gpm
Fe(OH)3 removed in a day	1.25	kg/day
Number of days Filter will last	16.8	days

	MW
Fe	56
0	16
Н	1
Mn	55



Multi-Round

Liquid BAG HOUSINGS

Multi-Round Liquid Bag Housings effectively remove dirt, pipe scale, and other contaminants from process liquids. Quality construction and design assure clean effluent and protection for all downstream equipment.

APPLICATIONS

- Chemical
- General Industrial
- Oil and Gas
- Water

HOUSING OPERATION

Unfiltered liquid enters the housing above the filter bags or strainer baskets, fills the interior of the housing and continues through the bag or strainer basket. Solids are trapped inside the filter bags or strainers and easily removed when the housing is serviced. Our standard o-ring seal between the baskets and the housing ensures a positive seal to prevent bypass.

HOUSING OPTIONS

- 300 PSI pressure rating
- Mesh-lined strainer baskets
- · Alternative o-ring materials
- Heavy-duty support legs

FEATURES

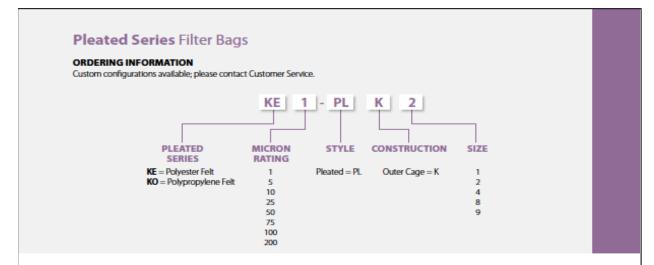
- Flow rates up to 3500 gpm
- Two basket to 17 basket housing designs, depending upon the required surface area and volume of fluid to be filtered
- Carbon steel and 304, or 316 Stainless Steel material
- Each vessel is factory hydro-tested
- Low pressure drop
- Swing bolts with bearing-assisted davit closure
- Buna-N^o seals lid and basket
- Differential, drain, and vent ports
- 316 Stainless Steel strainer baskets
- Two-part epoxy finish on carbon vessels
- Accepts #2-size bag filters
- Hydraulic lid lift

SPECIFICATIONS

Model	Maximum Dimensions
Pressure Rating	150 PSI at 300°F (up to 300 PSI aptional)
Connections	2-, 3-, 4-, 6-, 8-, 10- of 12-inch RF RG
Housing Lid	Swing bolts with davit cover life
Lid & Basket Scals	Bura-N*
Pressure Ports	Two differential ports measure pressure across filter bag
Construction/Finish	Carbon steel w/two-part epoxy finish; 304 or 316 Stainless Steel w/satin finish
Basket Material	316 Stainless Steel with 9/64-inch perforations
Bags Sizes	#2 liquid bags accepted
Base	Heavy duty support legs



Prepared By: SK Checked By: DB Date: April 18, 2012



LIQUID BAG SQUARE FOOTAGE

Size	Pleated	Standard
#1	9.0	2.0
#2	19.0	4.4
#4	25	1.0
#8	8.0	2.0
#9	13.0	3.4



502 Indiana Avenue, Sheboygan, WI 53082-1047 800.869.0325 574.278.7161 FAX 574.278.7115 support@pentairindustrial.com www.pentairindustrial.com

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C-3 Polyphosphate Dosing Requirements

Naval Facilities Engineering Command ~ Mid-Atlantic TETRA TECH, INC.

Grumman Rd Calverton NY Suffolk County, New York

Polyphosphate Dosing

Checked By: DB

Prepared By: SK

Date: April 18, 2012

Design Fe + Mn conc. 2.7 mg/L Calcium Conc 6 mg/L

Plant Flow 100 gpm 378.5 Plant Flow lpm Dose 4.5 mg/l mg/min Polyphosphate Mass Flc 1703.25

Specific Gravity 1.37

Density 1.37 kg/l Solution (%) 35 % Polyphosphate Flow 479.5 mg/ml

Polphosphate Flow 3.6 ml/min Polphosphate Flow 1.4 GPD

Monthly Usage 41 Monthly usage rate (gal)



CARUSTM 341040 WATER TREATMENT CHEMICAL

EC-SAFETY DATA SHEET according to EC directive 2001/58/EC MATERIAL SAFETY DATA SHEET

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MSDS# CP-356

Revision Date: October 2007

Supercedes: June 2006

Section 1 Chemical Product and Company Identification

Product Name:	CARUS™ 8100 Water Treatment Chemical						
Frade Name:	CARUS™ 8100 Water Treatmer	nt Chemical					
Synonyms:	Blended Phosphate solution						
Manufacturer's l	Name:	Information: (815) 223-1500 (815) 224-6816 (FAX)					
Carus Phosphates,	Phosphates, Inc. www.caruschem.com (Web) salesmkt@caruschem.com						
Manufacturer's A	Address:	Emergency Telephone:					
Carus Phosphates,	Inc.	(800) 435 -6856 (USA) (815) 223-1500 (Other countries)					
315 Fifth Street		CHEMTREC® (800) 424-9300 (USA)					
Peru, IL 61354, U	JSA	(703) 527-3887 (Other countries)					

Section 2 Ingredients Information

Material	PEL	TLV	CAS.NO.	EC. NO.	%
Triphosphoric acid, pentasodium salt	No Data	No Data	7758-29-4	231-838-7	l-15
Non-hazardous ingredients	No Data	No Data	N/A	N/A	85-99

This product contains no toxic chemicals subject to the reporting requirements of Section 313 - Title III of the Superfund Amendments and Reauthorization Act of 1986 and 40 CFR Part 372. All the components in this product are generally considered to be safe and none could be classified as hazardous according to the WHMIS system. None are listed on the Canadian Ingredient Disclosure List. Not listed by NTP Carcinogenicity: Hazard Symbols: None

Risk Phrases: 22 Harmful if swallowed. 38 Irritating to skin

Safety Phrases: Keep out of reach of children 61 Avoid releases to the environment.

Section 3 Hazards Identification

Hazardous Materials Identification System (HMIS) Ratings:

Health: 1 - Slight

Flammability: 0 - None Reactivity: 0 - None

Personnel Protective Equipment: goggles, face shield, apron, respirator and proper gloves.

Inhalation:

May cause irritation to the respiratory tract. Symptoms may include coughing and shortness of breath.

Ingestion:

Phosphates are slowly and incompletely absorbed when ingested, and seldom result in systemic effects. Such effects, however, have occurred. Symptoms may include vomiting, lethargy, diarrhea, blood chemistry effects, heart disturbances and central nervous system effects. The toxicity of phosphates is due to their ability to sequester calcium.

Skin Contact:

May cause irritation. May cause inflammation and pain on prolonged contact, especially with moist skin.

Eve Contact:

May cause irritation, redness and pain.

Chronic Exposure:

May sequester calcium and cause calcium phosphate deposits in the kidneys.

Aggravation of Pre-existing Conditions:

No information found.



CARUSTM 3 100 WATER TREATMENT CHEMICAL

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MATERIAL SAFETY DATA SHEET

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Section 4 First Aid Measures

Eyes:

Immediately flush eyes with large amounts of water for at least 15 minutes holding lids apart to ensure flushing of the entire surface.

Skin:

Immediately wash contaminated areas with water. Remove contaminated clothing and footwear. Wash clothing and decontaminate footwear before reuse.

Inhalation:

Remove person from contaminated area to fresh air.

Ingestion:

Never give anything by mouth to an unconscious or convulsing person. If person is conscious, give large quantities of water or milk. Seek medical attention immediately.

Section 5 Fire Fighting Measures

NFPA* Hazard Ratings:

Health:

=

Materials which under fire conditions would give off irritating combustion products (less

than I hour exposure). Materials which on the skin could cause irritation.

Flammability:

0 =

Materials that will not burn.

Reactivity: and

- N

Materials which in themselves are normally stable, even under fire exposure conditions,

which are not reactive with water.

Special Hazard: None

*National Fire Protection Association 704

First Responders:

Wear protective gloves, boots, goggles, and respirator. In case of fire, wear positive pressure breathing apparatus. Approach incident with caution.

Flash Point

None

Flammable or Explosive Limits

Lower: Nonflammable Upper: Nonflammable

Extinguishing Media

Use large quantities of water, Dike to contain.

Section 6 Accidental Release Measures

Steps To Be Taken If Material Is Released Or Spilled:

Contain spill by collecting the liquid in a pit or holding behind a dam (sand or soil). Absorb with inert media and dispose of properly. Disposal of all materials shall be in full and strict compliance with all federal, state, and local regulations pertaining to phosphates. Flush area with large amounts of water.

Personnel Precautions:

Personnel should wear protective clothing suitable for the task.

Section 7 Handling and Storage

Work/Hygiene Practices:

Wash hands thoroughly with soap and water after handling phosphate solution, and before eating or smoking. Wear proper protective equipment. Remove clothing, if it becomes contaminated.

Ventilation Requirements:

Provide sufficient mechanical and/or local exhaust.

Conditions For Safe Storage:



CARUSTM 3110 WATER TREATMENT CHEMICAL

EC-SAFETY DATA SHEET according to EC directive 2001/58/EC
MATERIAL SAFETY DATA SHEET

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Protect containers from physical damage. Store in a cool, dry area in closed containers.

Section 8 Exposure Controls and Personal Protection

Respiratory Protection:

In cases where overexposure to mist may occur, use an approved NIOSH-MSHA mist respirator (N-95 or better). Engineering or administrative controls should be implemented to control mist.

Eve:

pH:

Face shield, goggles, or safety glasses with side shields should be worn. Provide eyewash in working area.

Gloves:

Rubber or plastic gloves should be worn.

Other Protective Equipment:

Normal work clothing covering arms and legs, and rubber, or plastic apron should be worn. Caution: If clothing becomes contaminated, wash off immediately.

Section 9 Physical and Chemical Properties

Appearance And Odor: Colorless solution, odorless

Boiling Point, 760 mm Hg: >101 °C Freezing Point: <0 °C

Vapor Pressure (mm Hg): N/A

Solubility In Water % By Solution: Miscible in all proportions

Percentage Volatile By Volume:55% (as water)Evaporation Rate:Same as waterSpecific Gravity: 1.37 ± 0.03

Section 10 Stability and Reactivity

Stability: Under normal conditions, the material is stable.

Conditions To Avoid: Do not expose to extreme temperatures.

Incompatible Materials Soluble calcium salt solutions and hydrofluoric or hydrofluosilicic

acid could cause precipitations.

Hazardous Decomposition: When involved in a fire, the material may form toxic fumes of

 4.5 ± 0.5

phosphorous oxides.

Condition Contributing To Material is not known to polymerize.

Hazardous Polymerization:

Section 11 Toxicological Information

Acute Overexposure:

Irritating to body tissue with which it comes into contact.

Chronic Overexposure:

No known cases of chronic poisoning due to phosphate solutions have been reported. May sequester calcium and cause calcium phosphate deposits in the kidneys.

Carcinogenicity:

None of the components have been classified as a carcinogen by OSHA, NTP, and IARC.

Medical Conditions Generally Aggravated by Exposure:

Phosphate solution will cause further irritation of tissue, open wounds, burns or mucous membranes.



CARUSTM 8 100 WATER TREATMENT CHEMICAL

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MATERIAL SAFETY DATA SHEET

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Section 12 Ecological Information

None

Section 13 Disposal Considerations

Waste Disposal:

Disposal of all materials shall be in full and strict compliance with all federal, state, and local regulations pertaining to phosphates. Chemical waste generators must determine whether a discarded chemical is classified as a hazardous waste. US EPA guidelines for the classification determination are listed in 40 CFR Parts 261.3.

RCRA P-Series: None listed.

RCRA U-Series: None listed.

Section 14 Transport Information

Not regulated by US DOT, Canada TDG, UN, IMDG, IATA regulations

Section 15 Regulatory Information

US Federal Regulations

TSCA:

All components in this product are listed on the TSCA inventory.

Health & Safety Reporting List:

None of the chemicals in this product are on the Health & Safety Reporting List.

Chemical Test Rules:

None of the chemicals in this product are under a Chemical Test Rule.

Section 12b:

None of the chemicals in this product are listed under TSCA Section 12b.

TSCA Significant New Use Rule:

None of the chemicals in this product have a SNUR under TSCA.

CERCLA Hazardous Substances and corresponding ROs:

None of the chemicals in this product have an RO.

SARA Section 302 Extremely Hazardous Substances:

None of the chemicals in this product have a TPQ.

SARA Codes:

Acute

Section 313:

None of chemicals in this product are reportable under Section 313.

Clean Air Act:

This material does not contain any hazardous air pollutants.

This material does not contain any Class 1 or Class 2 Ozone depletors.

Clean Water Act:

None of the chemicals in this product are listed as Hazardous Substances under the CWA.

None of the chemicals in this product are listed as Priority Pollutants under the CWA.

None of the chemicals in this product are listed as Toxic Pollutants under the CWA.

OSHA:

None of the chemicals in this product are considered highly hazardous by OSHA.

State:

None of the chemicals in this product are present on state lists from CA, PA, WI, MA, or NJ.



CARUSTM 3 100 WATER TREATMENT CHEMICAL

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California Prop 65:

California No Significant Risk Level: None of the chemicals in this product are listed.

European/International Regulations

European Labeling in Accordance with EC Directives:

Hazard Symbols:

None

2

Risk Phrases:

22 Harmful if swallowed.

38 61

8 Irritating to skin

Safety Phrases:

Keep out of reach of children

Avoid

Avoid releases to the environment.

WGK (Water Danger/Protection): None

Canada - DSL/NDSL:

All components are listed on Canada's DSL List

Canada - WHMIS:

None of the components in this product could be classified as hazardous in accordance with the hazard criteria of the Controlled Products Regulations.

Canadian Ingredient Disclosure List:

None of the components in this product are listed on the Canadian Ingredient Disclosure List.

Section 16 Other Information

NIOSH: National Institute for Occupational Safety and Health

MSHA: Mine Safety and Health Administration

OSHA: Occupational Safety and Health Administration

NTP: National Toxicology Program

IARC: International Agency for Research on Cancer

PEL: Permissible Exposure Limit

DSL/NDSL: The Domestic Substances and the Non-Domestic Substances List (Canada)

TLV-TWA: Threshold Limit Value-Time Weighted Average

CAS: Chemical Abstract Service

EINECS: Inventory of Existing Chemical Substances (European) (EC. No.)

The information contained herein is accurate to the best of our knowledge. However, data, safety standards and government regulations are subject to change and, therefore, holders and users should satisfy themselves that they are aware of all current data and regulations relevant to their particular use of product. CARUS PHOSPHATES, INC. DISCLAIMS ALL LIABILITY FOR RELIANCE ON THE COMPLETENESS OR ACCURACY OR THE INFORMATION INCLUDED HEREIN. CARUS PHOSPHATES, INC. MAKES NO WARRANTY, EITHER EXPRESS OR IMPLIED, INCLUDING, BUT NOT LIMITED TO, ANY WARRANTIES OF MERCHANTIABILITY OR FITNESS FOR PARTICULAR USE OR PURPOSE OF THE PRODUCT DESCRIBED HEREIN. All conditions relating to storage, handling, and use of the product are beyond the control of Carus Phosphates, Inc., and shall be the sole responsibility of the holder or user of the product.

CARUS PHOSPHATES, INC. IS A SUBSIDIARY OF CARUS CORPORATION, 315 FIFTH STREET, PERU, IL



Chithambarathanu Pillai

October 2007



CARUS™ 3 100 WATER TREATMENT CHEMICAL

EC-SAFETY DATA SHEET according to EC directive 2001/58/EC MATERIAL SAFETY DATA SHEET

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C-4 Treatment Building Heating Requirements



Rev.: A Date : 11/17/11

	Treatment Building Hea	ting Requirements
Design Indoor temp Design Outdoor temp	59 F 9 F	ASHRAE ASHRAE (97.5% for Bridgeport, CT)
	outside wall	
outside wall	roof inside	outside wall
	outside wall	
Peak Height Width (1 sidewall) Length (1 end wall)	14 ft 25 ft 35 ft	
Exposed Wall Area U, wall Wall Subtotal	1680 ft2 0.113 btu/hi 9,492 Btu/h	
Roof Area U, roof Roof subtotal	875 0.167 btu/hi 7306	r-ft2-F (R-13)
Ventilation Rate Floor area Room air turnovers (minutes/cha	NA ft2 nge) 20	2 floor
Ventilation Make-up rate Ventilation Subtotal Heat Require	613 cfm ed 33,688 Btu/h	Make-up air from outside building Heat Required =1.1 x cfm exhausted x (design inside T - design outside T)
Total Building Heat Required	50,486 Btu/h	ır
Prepared by WLS		Checked By: 7/2011
DDB	B 5/	9/2012

C-5 Electrical Load List & Short Circuit Calculation



Proj. No.: 112G02750

Customer: Naval Facilities Engineering Command ~ Mid-Atlantic

Date:

Revision: B

4/18/2012

Project: **Groundwater Treatment Plant**

Location: Grumman Rd Calverton NY Suffolk County, New York

Purpose: **Preliminary Short Circuit Calculation**

SHORT CIRCUIT CALCULATION (PRELIMINARY)

T-1 TRANSFORMER

150KVA 480/277 VAC Secondary 3 Phase

STEP 1: Determine transformer full-load amperes.

$$I_{FLA} = \frac{KVA \times 1000}{E_{L-L} \times 1.732}$$

$$E_{L-L} = 480$$

$$I_{FLA} = \underline{180} A$$

STEP 2: Find transformer multiplier.

Multiplier =
$$\frac{100}{\text{Transf. }\%Z}$$

%Z = 1.20 Assumed %Z of "1.2" (150kVA Transformer impedance) for calculation.

Reference COOPER Bussman Bulletin EPR-1 "Electrical Plan Review"

Table 5 Short-Circuit Currents Available from Various Size Transformers Multiplier = 83.33

STEP 3: Determine transformer let-through short circuit current for 3 Phase faults.

$$I_{SCA (L-L-L)} = I_{FLA} x Multiplier$$
 $I_{FLA} from STEP 1$, Multiplier from STEP 2

$$I_{SCA (L-L-L)} = 15,036 \text{ Amps}$$

* Utility voltages may vary +/- 10% for power; therefore for worst case condition multiply by 1.1

$$I_{SCA \text{ with voltage variance}} = \underline{16,539} \text{ Amps}$$

** Add in motor short-circuit contribution; for practical estimate multiply the total motor full-load amperes by 4

$$I_{SCA motor contribution} = 50 \times 4 = 200$$
 A

$$I_{SCA total} = 16,739 \text{ Amps}$$



Proj. No.: 112G02750

Customer: Naval Facilities Engineering Command ~ Mid-Atlantic

Project: Groundwater Treatment Plant

Location: Grumman Rd Calverton NY Suffolk County, New York

Purpose: Preliminary Short Circuit Calculation

STEP 4: Calculate "f" factor for 3 Phase faults.

$$f = \frac{1.732 \times L \times I_{L-L-L}}{C \times n \times E_{L-L}}$$

Where:

L = length (feet) of conduit to fault.

C = conductor constant. *Obtained from COOPER Bussman Bulletin EPR-1 "Electrical Plan Review", Table 2 "C" values for conductors

n = number of conductors per phase (Adjusts C value for parallel runs)

I = available short-circuit current in amperes at beginning of circuit.

L = 100 ft.

For prelim. short circuit calculation; length (L) to fault is assumed to be 100 feet

Date:

Revision: B

4/18/2012

C = 8,925

3 single conductors, 600V, steel conduit, #1/0 AWG

n = 1

1 set of conductors per phase

I = 16,739 A E = 480 V I_{SCA total} from STEP 3

Then:

en: f = 0.677

STEP 5: Calculate "M" (multiplier).

$$M = \frac{1}{1 + f}$$

M = 0.596

STEP 6: Calculate the available short-circuit current (RMS symmetrical).

 $I_{SCA (at fault)} = I_{SCA (at beginning of circuit)} \times M$

I_{SCA total} from STEP 3, M from STEP 5

 $I_{SCA (at fault)} = _____9,983$ Amps

NOTES:

- 1. Short circuit calculation assumes unlimited primary short-circuit current (infinite bus).
- 2. Utility Company transformer not selected, therefore a transformer impedance (%Z) of "1.2" was assumed for calculation.
- 3. Utility Company transformer location not set, therefore length of service entrance conductors in STEP 4 above are approximate.

Prepared by:		Checked by:		Approved by:		
Bill Stonebraker	4/18/2011					
Name	Date	Name	Date	Name	Date	



					MOTOR						POWER	R DEVICES			kWH SUBTO	TALS		
ITEM	DESCRIPTION	VOLT	ø	НР	ВНР	FLA	FEEDER FLA	kVA	kW	STARTER	MCP	DRIVE (VFD) BREAKER (80% rated type)	% DEMAND	24Hr	MONTH	YEAR	NOTES	MINIMUM FEEDER (Reference Only - Installing Contractor to Verify)
	DEGGMI HON	460	3		51		, .	NVA .	, , ,	O PARTEIX			70 2 2 1117 1112	2	1	12/11	110120	motaming contractor to comy,
CP-AS200	Air Stripper System Control Panel (Vendor Pkg)	460	3				40	31.87	27.09			150/50	100	500.6	15,017.9	182,717.2	2 - 5HP, 1 - 7.5HP & Control Powe	r 3/4"C, 3-#8, 1-#10G
- B 440	One washing to a Forting of the Downs	460	3	_	0.0	0.00		4.00	4.04	_	454		400		0.040.0	00 500 5		0/480 4 440
	Groundwater Extraction Pump Groundwater Extraction Pump (SPARE)	460 460	3	5 5	3.9	6.26		4.99	4.24	1	15A 15A		100 100	78.3	2,349.9	28,590.5	SPARE	3/4"C, 4-#12
1-120	Ordinawater Extraction Fump (or AIL)	460	3	, , , , , , , , , , , , , , , , , , ,						•	134		100				OF AIRE	
	Roll-up Door	460	3				1.6	1.27	1.08			150/15	100	20.0	600.7	7,308.7		3/4"C, 4-#12
F-1	Treatment Building Exhaust Fan	460	3	1	0.8	1.25		1.00	0.85	1	3A		100	15.7	470.0	5,718.1		3/4"C, 4-#12
T-1 1	15kVA Transformer 480-240/120 1 Phase	460 460	3				31.2	24.86	21.13			150/40	100	390.5	11,713.9	142,519.4		3/4"C, 3-#8, 1-#10G
	TORVA Transformer 400-240/120 T Friase	460	3				31.2	24.00	21.13			130/40	100	390.5	11,713.9	142,519.4		3/4 0, 3-#0, 1-#100
H-1	Treatment Building Heater (15KW Unit)	460	3				18	14.34	12.19			150/30	100	225.3	6,758.0	82,222.7		3/4"C, 4-#10
		460	3															
	SPARE Breaker	460	3				15	11.95	10.16			150/20					SPARE Breaker	3/4"C, 4-#12
	FUTURE Motor - Size 1 FVNR Starter	460 460	3	5	3.9	6.26		4.99	4.24	1	15A						SPARE Starter	3/4"C, 4-#12
	. C. C. C. Motor GLO I I VIII Glario	460	3		0.0	5.20		7.00	7.27	•							S. FIRE Startor	5, 1 5, 1 m 12
		460	3															
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		460	3															
TŁ.	Tetra Tech, NUS		LOW VOL	TAGE MOT	OP LIST				MAINS FFF	EDER (Installing Cont	trootor to Vorife	1 1/4"C, 3-#2, 1-#40	C		1 1/2"C, 3-1/0,	1 #46	.259/ PA	GE 1/1
BDQ JEST T	Colverton Treetment Plant Design	E: MCC-TB Moto				Apr. 40.0040	0.05	PF			u actor to verify	BALANCED kVA				1-#40		YEAR
		E: MCC-1B Moto		ISSUE: REV:		Apr. 19 2012 B		PF EFF	95.26	3Ø KVA 1Ø KVA		BALANCED KVA BALANCED AMPS			+25% +25%	TOTAL Kwi		449,076.6
	MCC-TB (Treatment Building)			NEV.	J	J		COST/kWH		CONNECTED KVA	4	MAIN, FRAME/TRIP (80%)			+25%	TOTAL		1.0,010.0

FORMULAS USED IN THIS SPREADSHEET

FLA = HP x 746 E x %EFF x PF x 1.732 kVA = E x I x 1.732

kW = <u>E x I x PF x 1.732</u> 1000

GENERAL:

- 1. DO NOT enter two values (HP and FEEDER FLA) on the same line as both will calculate
- 2. Valid voltage range is 440-480V, user-selected
- 3. Power factor (PF), efficiency (EFF), COST/kWH, % DEMAND and phase (Ø) are user-defined. Some of these have typical or default values inserted
- 4. All single phase equipment is placed on the same phase and balanced on the other two phases
- 5. Feeder breaker sizing is based on 100% FLA and 80% trip
- 6. Main breaker sizing is based on 100% (standard) and 125% (+25%) BALANCED AMPS and 80% trip. If the amp are less than 100 or more than 1600, UNDER or OVER, respectively, appears in the MAIN BREAKER cell
- 7. MINIMUM feeder sizing is based on 125% FLA and type THHN cabling

ADDING MOTORS: enter horsepower value into HP column

- 1. Valid entries are 1/4 400HP 3-phase only
- 2. Motor BHP, FLA, kVA, kW, NEMA starter size, MCP amps and MINIMUM FEEDER sizing is calculated for each entry
- 3. If the controller is a drive, softstart or similar device instead of a starter, enter VFD, IGBT, SOFT etc into the DRI column located under the POWER DEVICES heading. This will cause the STARTER and MCP cells for that item blank

ADDING FEEDERS: enter amp value into FEEDER FLA column

- 1. Valid for feeds to 320A (equivalent to 400A 80% breaker)
- 2. Select 1 or 3Ø
- 3. KVA, kW, required feeder BREAKER and MINIMUM FEEDER sizing will be calculated for each entry

BLOCKING an item from calculation

1. Deleting the value in the Ø column for a given item will exclude that load from the calculated total while allowing the required starter, MCP, breaker etc to remain. An application for this would be the installed spare or standby unit in a pair of pumps. Optional to clearing the Ø value, a description such as SPARE or SBY may be used with the same result.

kWH TOTALS:

- 1. Enter a run-time percentage for each item into the % DEMAND column
- 2. A daily, monthly and yearly kWH SUBTOTAL will be calculated for each item
- 3. Daily, monthly and yearly TOTAL kWH will be calculated
- 4. If kWH costing information is desired, enter a cost/kWH into the COST/kWH cell; total daily, monthly and yearly operating costs will be calculated



Rev.: C Date : 4/19/12

Treatment Building Miscellaneous Loads for 120/240V Distribution Panel PDP-1

Lighting Loads: Ref. NEC, 2011, Article 220.12, Table 220.12

Equip.	Description	Length (ft)	Width (ft)	Area (ft²)	Occupancy Unit Load (VA / ft ²)		Connected Load (KVA)		Demand in KVA
	Buiding Interior	35	25	875	2.00		1.75	1.0	1.75
	Building Exterior						0.50	0.6	0.30
					·		0.00	1.0	0.00
	_					Subtotal	2.25		2.05

Non-Lighting Loads: Ref. NEC, 2011, Article 220.14 (A) thru (L)

				Connected		
				Load	Demand	Demand
				(KVA)	Factor	in KVA
Recpt.						
Type	Qty.	VA (each)				
Duplx.	4	180		0.72	1.0	0.72
Quad.	2	360		0.72	1.0	0.72
					I - T - I - I	4 4 4

| Receptacle Total | 1.44 | Up to 1st 10 KVA @ 100% | 1.44 | Overage | 0.00 |

Overage @ 50% 0.00 Subtotal 1.44

<u>Specifi</u>	c Loads and Motors:	Connected Load (KVA)	Demand Factor	Demand in KVA				
Equip.				,				
#	Description	Volts	Amps	Phase				
P-500	Sump Pump (1/2 HP)	120	9.8	1		1.18	0.6	0.71
P-510	Dosing Pump #1 (1/6 HP)	120	4.4	1		0.53	0.6	0.32
P-520	Dosing Pump #2 (1/6 HP)	120	4.4	1		0.53	0.6	0.32
	Control Panel Power	120	16	1		1.92	1.0	1.92
	Misc. Equipment	120	16	1		1.92	1.0	1.92
	Emergency Lights	120	1	1		0.12	1.0	0.12
			·			0.00	0.6	0.00
				Single Pha	se Subtotal	6 19		5 30

Totals 10 KVA 7 KVA

Amps @ 480V 12 9

Transformer T-1: Size 15.0 KVA 15.0 KVA % Loaded 66% 49%

C-6 Stormwater Design Calculations

Abbreviated Stormwater Management Report for the proposed

Calverton Fenceline Groundwater Treatment Facility

Grumman Blvd, Calverton, New York

Prepared by: Tetra Tech, April 2012, CSG/YL

The Navy is proposing a small groundwater treatment plant size and minor land improvements (mainly a gravel driveway). The majority of property (168.9 acres) remains the same except the minor disturbance of the subject project area. The site disturbance is 0.16 acres (6,800 s.f.) and the increase of impervious area within the disturbance area is approximately 30%.

The stormwater design for this site meets the intent of the Town of Riverhead's stormwater management (SWM) regulations, which, in general, refer to New York State DEC SWM guidelines. Therefore, the site stormwater management practices (SMP) design is based on New York State Stormwater Management Design Manual (August 2010) for stormwater quality. The SMP design parameters constitute the removal efficiency equivalent to the Department's performance criteria (80% TSS removal and 40% phosphorus removal). The site incurs less than 1 acre of disturbance, therefore the stormwater quantity control was not considered for the site development.

Infiltration practices were considered on this site to capture and temporarily store the WQv before allowing it to infiltrate into the soil. According to the USDA Soil Survey of Suffolk County, New York, the project site is located in a "CpC- Carver and Plymouth sands" Area, Hydrologic Soil Group (HSG) "A" and the capacity of the most limiting layer to transmit water (Ksat) is moderately high to high (0.20 to 5.95 in/hr), which is good for infiltration practices and the test borings confirmed the soil type. However, stormwater infiltration testing was not performed for the site.

During the test borings for foundation, the groundwater was encountered at approximately 4.5 to 5.0 feet below existing ground surfaces. Groundwater elevations fluctuate seasonally and are subject to variations of precipitation. It was assumed that the ground water is at 4.0 below the ground surface. Infiltration trench and dry well are not feasible on site due to the shallow ground water location.

Shallow Infiltration Basin is designed to store the WQv in a shallow depression area. A depression area (210 cubic feet, 35' long x 6' wide x 1' deep) is proposed adjacent to the existing wetlands.

Lined channels with a check dam at the end are planned for pretreatment measure from the roof drains to the infiltration basin. Vegetative cover similar to the existing conditions (turf grass mixed with brush/clump grass) will be established between the contributing pervious drainage area and the infiltration facility.

See attached excel work sheet for the Water Quality Volume (WQv) calculations

Infiltration Practices must be 25' from Structures

Infiltration Basin:

Note:

NYS Stormwater Management Design Manual Method (August 2003):

Find Req'd Volume:

$$WQ_{v} = \frac{(P)(R_{v})(A)}{12}; R_{v} = 0.05 + 0.009 (I)$$

P 1.25 (Figure 4.1, NYS Stormwater Management Design Manual)

I 100% (impervious area)

Rv 0.95

A 0.0489 (acres) WQv 0.0048 (acre-feet)

WQv 211 (cubic feet, storage required)

Basin Sizing:

Length 35 (feet)
Width 6 (feet)
Depth 1 (feet)
Actual Volume: 210 (cubic feet)

Pre-Treatment:

Use a plunge pool (or similar) due to surface and groundwater constraints

C-7 Infiltration Trench Calculations

Sizing of Infiltration Gallery

<u>Parameter</u>	<u>Value</u>	<u>Unit</u>
Hydraulic Conductivity - Horizontal	221	feet/day
Hydaulic Conductivity - Vertical	102	feet/day
Hydraulic Gradient of Aquifer (foot-V/foot-H)	0.003	3-ft/1,000-ft
Hydraulic Gradient - Assuming deep groundwater:	1	1-ft/1-ft
Aquifer Thickness	45	feet
Groundwater rise allowed	2	feet
Specific Capacity of Injection Well	21	GPM/foot
Treated water flowrate (influent to infiltration gallery)	100	gpm
Quantity of groundwater to be infiltrated on a daily basis:	144,000	Gal/day
	19,251	Cubic Ft/day
Capacity of 200 foot trench:		
Vertical Infiltration Area required	0.94	feet
Vertical Gradient Required at Edge of Trench (south only)	0.009	foot/foot
Vertical Gradient Required at a distance of 100 feet (east/west/south)	0.005	foot/foot
Vertical Gradient Required at a distance of 200 feet (east/west/south)	0.003	foot/foot
Capacity of Injection Well	42	GPM

APPENDIX D SOIL TESTING REPORT



Tetra Tech NUS, Inc.

BORING LOG

Page _1_ of _1_

PROJECT NAME: PROJECT NUMBER: DRILLING COMPANY: NWIRP Calverton 112G02750 Delta Well and Pump

BORING No.: CA-SAFL-SB01 10/17/2011

GEOLOGIST: Robert Sok Failing F-10 **DRILLING RIG:** DRILLER: **Bob Devine**

6	D					I.	/ATE	RIAL DESCRIPTION			PID/FI	D Rea	ding	(ppm)
Sampl e No. and Type or RQD	Depth (Ft.) or Run No.	Blows / 6" or RQD (%)	Standard Penetratio n Resistance (SPR) Number	Sample Recovery / Sample Length	Lithology Change (Depth/Ft.) or Screened Interval	Soil Density/ Consistency or Rock Hardness	Color	Material Classification	U S C S *	Remarks	Sample	Sampler BZ	Borehole**	Drifter BZ**
	1	6 8					Dk Brn	Topsoil 0-6"; to Clayey F. sand, little			١.	-	_	Ţ
S-1	2	7	16	11/24		very stiff	Org Brn	clay, trace silt		moist	-	_		
	3	10 9						2" - F to Med gravel zone at 2.3-2.5 ft		moist	_	-	-	_
S-2	4	11 12	20	17/24		Med-Dense	Lt Bm	Silty Sand, F. to Med Sand, some silt,			-	-	-	-
	5	6 9			\sqsubseteq			trace F. gravel			-	-	-	
S-3	6	9 7	18	8/24		Med-Dense				water at ~5' BGS	_	- 1		-
	7	5 7					Brn Tan	F. to Med Sand, trace C. Sand and			_	-	1	_
S-4	8	66	13	8/24		Med-Dense		gravel, trace silt, wet		wet saturated	-	-		-
	9	14								poor recovery	T -	-	-	_
S-5	10	**	12	3/24		Med-Dense	Tan Brn	F. to Med Sand, little silt, wet		wet saturated	-	1	-	-
	11	\angle												
	12	\angle												
	13	\leq												
S-6	14	5 5					Tan Bm	Same as above; except less silt		poor recovery	_	1		-
	15	10	12	2/24		Med-Dense		,		wet saturated	_	-	-	_
-	16	\leq												
	17	\leq												
	18	-					Brn							
S-7	19	4		•••			Tan	Same as above		poor recovery	_	-		
	20	5	8	2/24		Loose				wet saturated		_	-	_
	21													
$\vdash \vdash$	22													
	23	7					Brn			·	<u>L</u> .			
S-8	24	4			2		Tan	Assumed same as above			-	-	-	
11/5	25	/ 7	9	NR		L.oose			-	no recovery	-	_	_	-

25 7 9 NI	IR Lo	oose			no recovery	_	-	-	-
When rock coring, enter rock brokene	ess.						_	_	_
* Include monitor reading in 6 foot inter	ervals @ borehole. In	crease reading frequenc	v if elevated reponse read	L	Drillin	na Ar	ea		
Remarks: 2' x 2' stainless split spo	oon. 3.25" ID Hollow	Stem Auger	,	•	Background			ΝΔ	
No heaving observed du	luring drilling, poor red	coveries below water tab	le		Dacinground	(pp	11). <u>[3</u>	- N/N	
· · ·			·						
Converted to Well:	Yes _	No	X	/ell I.D. #:					-



Tetra Tech NUS, Inc.

BORING LOG

Page _1_ of _1_

Drilling Area

Background (ppm): NA

PROJECT NAME: PROJECT NUMBER: DRILLING COMPANY:

DRILLING RIG:

NWIRP Calverton 112G02750 Delta Well and Pump

Failing F-10

BORING No.: <u>CA-SAFL-SB02</u> DATE: <u>10/17/2011</u>

DATE: 10/17/2011
GEOLOGIST: Robert Sok

DRILLER: Bob Devine

		·	l		raming		AATE	RIAL DESCRIPTION		DOD Devine				
Sampl e No. and Type	Depth (Ft.) or Run	Blows / 6" or RQD (%)	Standard Penetratio n Resistance	Sample Recovery / Sample	Lithology Change (Depth/Ft.) or	Soil Density/ Consistency		HIAL DESCRIPTION	U S C	Remarks	PID/FI			
or RQD	No.		(SPR) Number	Length	Screened Interval	or Rock Hardness	Color	Material Classification	\$ *	Homarks	Sample	Sampler BZ	Borehole**	Driller 82**
	1	5 5					Dk Brn	Topsoll 0-7"; Silty Clay,some silt, trace			1.	1	-	
S-1	2	7 8	12	22/24		stiff	Вгл	VF. To F. sand			-	_	_	-
	3	8 7					Brn			moist	<u> _</u>	_	-	_
S-2	4	7 6	14	18/24		stiff	Org Brn	2" - F to Med gravel zone at 3.5-3.7 ft			1_	-	-	-
	5	5 4			\sqsubseteq			F-C Sand, trace to little silt and clay, trace gravel		poor recovery	-	-	_	-
S-3	6	8 10	12	1/24		Med-Dense	Tan Brn			water at ~4-5' BGS	_			-
	7	7 8						F. to Med Sand, some silt and clay, wet					_	-
S-4	8	8	18	8/24		Med-Dense	Tan Brn			wet saturated	-	_	-	-
	9	6 7									<u> </u>	_		-
S-5	10		15	9/24		Med-Dense	Tan Brn	F. to Med Sand, trace silt and clay, wet		wet saturated		-	-	-
	11	/		_				-		 				
	12	$\langle \cdot \rangle$									<u> </u>			
	13	5									<u> </u>			_
S-6	14	4					Tan	No Sample		no recovery	<u> -</u>	-	-	-
	15		8	NR		Loose					 -	1	-	_
	16										- 			
	17 18					,		· · · · · · · · · · · · · · · · · · ·			+-			-
S-7	19	3 4					Tan				╁┈			
0-,	20	4,	8	14/24				F. to Med Sand, trace silt and clay, wet			 - -	~		-
	21		<u> </u>	7164		Loose				wet saturated	+-	-	-	-
	22							· · · · · · · · · · · · · · · · · · ·			+			
	23									*****	 			\dashv
S-8	24	7/8					Tan				<u> </u>		_	
	25	9 11	17	12/24		Med-Dense		F. Sand, trace Med sand and silt, wet		wet saturated	-	_	-	_
* When	rock co	ring, ente	r rock broke	eness.										

No X

Well I.D. #:

** Include monitor reading in 6 foot intervals @ borehole. Increase reading frequency if elevated reponse read.

Yes

Remarks: 2' X 2' stainless split spoon. 3.25" ID Hollow Stem Auger

Converted to Well:

Bob Devine

Calverton Geotech Sampling Breakdown Southern Area Treatment Building October 17, 2011

	_			_	70.	_					+								_,
Attenberg Limits												×			,,,,,,				
% passing 200		×	×		×		×		×			×	×	×	8/	×			×
Moisture Content		×	×	×	X	×	×	0.00	×			×	×	X	×	X		×	×
Grain size				×		×	- 500 March								×			×	
Time		1215	1217	1220	1224	1227	1234	No Sample	1250	No Sample		1410	1412	1416	1418	7422	No Sample	1440	1455
	from	7	က	4	9	ω	은	5	ଯ	82	斯 斯斯克	က	4	ဖ	∞	10	15	20	25
Depth	2	-	2	3	4	9	8	13	18	g		-	3	4	9	8	13	18	83
BORING		CA-SAFL-SB01		CA SAFL SB02	CA-SAFI SB02	CA-SAFL-SB02	CA-SAFI SB02	CA-SAFI SB02	CA SAFI SB02	CA SAFT SB02	CA SAFI SB02								



125 Nagog Park Acton, MA 01720 978 635 0424 Tel 978 635 0266 Fax

Tra	ns	m	iit	ta
-----	----	---	-----	----

David Brayack	DATE: 10/28/2011	GTX NO: 11233
Tetra Tech NUS, Inc.	RE: NWIRP Calverton	Geotech, CTO WE63
Twin Oaks I, Suite 309		
5700 Lake Wright Drive		
Norfolk, Virginia 23502		

COPIES	DATE	DESCRIPTION
	10/28/2011	October 2011 Laboratory Test Report
		·

EMARKS:	
INIANIO.	
	SIGNED:
C:	Joe Tomei, Laboratory Manager
	5 - 7

Nancy Hubbard, Project Månager

APPROVED BY:



www.geotesting.com



October 28, 2011

David Brayack Tetra Tech NUS, Inc. Twin Oaks I, Suite 309 5700 Lake Wright Drive Norfolk, Virginia 23502

RE: Contract Task Order (CTO) WE63

NWIRP Calverton Geotech, Calverton, NY (GTX-11233)

Dear David:

Enclosed are the test results you requested for the above referenced project. GeoTesting Express, Inc. (GTX) received 14 samples from you on 10/19/2011. These samples were labeled as follows:

CA-SAFL-SB01-0102
CA-SAFL-SB01-0203
CA-SAFL-SB01-0304
CA-SAFL-SB01-0406
CA-SAFL-SB01-0608
CA-SAFL-SB01-0810
CA-SAFL-SB01-1820
CA-SAFL-SB02-0103
CA-SAFL-SB02-0406
CA-SAFL-SB02-0406
CA-SAFL-SB02-0608
CA-SAFL-SB02-0810
CA-SAFL-SB02-1820
CA-SAFL-SB02-2325

GTX performed the following tests on these samples:

10 ASTM D 1140 - Percent Finer Than #200 Sieve
14 ASTM D 2216 - Moisture Contents
4 ASTM D 422 - Grain Size Analyses (sieve only)
1 ASTM D 4318 - Atterberg Limits

Moisture Content (ASTM D 2216)

Moisture content testing was performed in general accordance with ASTM D 2216. This test determines the water (moisture) content of a material by oven drying. The loss of mass caused by drying is due to the loss of water. The water content is defined as the ratio of the mass of water contained in the pore spaces of soil or rock material, to the mass of solid particles in that material, which is expressed as a percentage. A standard temperature of $110 \pm 5^{\circ}$ C was used to determine the dry mass of the material.



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Percent Passing No. 200 Sieve (ASTM D 1140)

Percent Passing No. 200 Sieve testing was performed in general accordance with ASTM D 1140. The test measures the percent of the soil sample which is finer than the No. 200 sieve size (75 μ m). The sample is oven-dried and then washed over a No. 200 sieve until the wash water is clear. The material retained on the No. 200 sieve is then oven-dried and the percent of the original dry weight passing the No. 200 sieve is then calculated.

Grain Size Analysis (ASTM D 422)

Grain Size Analysis testing was performed in general accordance with ASTM D 422. The test measures the distribution of particle sizes in soils. The distribution of particle sizes larger than 75 μ m (retained on the No. 200 sieve) is determined by sieving, while the distribution of particle sizes smaller than 75 μ m is determined by a sedimentation process, using a hydrometer.

Atterberg Limits (ASTM D 4318)

Atterberg Limits testing was performed in general accordance with ASTM D 4318. The test includes the determination of the liquid limit, plastic limit, and the plasticity index of soils. The liquid limit represents the water content of a soil at the boundary between the semi-liquid and plastic states of a soil. The plastic limit is the water content of a soil at the boundary between the plastic and semi-solid states. The plasticity index is the range of water content over which a soil behaves plastically. Numerically, it is the difference between the liquid limit and the plastic limit.

Atterberg limit samples were prepared using the wet preparation method on specimens that were processed to remove any material coarser than a No. 40 sieve.

The liquid limit is determined by spreading a portion of the specimen in a brass cup, divided in two by a grooving tool, and then allowed to flow together from the shocks caused by repeatedly dropping the cup in a standard mechanical device.

Liquid limits were performed using Method A, the multipoint test, which requires three or more trials over a range of water contents to be performed and the data from the trials plotted to make a relationship from which the liquid limit is determined.

When requested, the oven-dried liquid limit was also determined. This test follows the same procedures as listed above for liquid limits. The difference is that the material is oven dried and then re-wet before the test is performed. If this value of liquid limit is less than 75% of the original liquid limit, the sample is considered to be organic.

The plastic limit is determined by rolling a small portion of soil into a thread and working the thread until its water content is reduced to a point at which a 1/8 in. diameter thread crumbles and can no longer be pressed together and re-rolled. The water content of the soil at this point is reported as the plastic limit.



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A copy of your test request is attached.

The results presented in this report apply only to the items tested. This report shall not be reproduced except in full, without written approval from GeoTesting Express. The remainder of these samples will be retained for a period of sixty (60) days and will then be discarded unless otherwise notified by you. Please call me if you have any questions or require additional information. Thank you for allowing GeoTesting Express the opportunity of providing you with testing services. We look forward to working with you again in the future.

Respectfully yours,

Joe Tomei

Laboratory Manager



125 Nagog Park Acton, MA 01720 978 635 0424 Tel 978 635 0266 Fax

Geotechnical Test Report

10/28/2011

GTX-11233 NWIRP Calverton Geotech

Calverton, NY

Client Project No.: 112G02750; CTO WE63

Prepared for:

Tetra Tech NUS, Inc.



Client: Tetra Tech NUS, Inc.

Project: NWIRP Calverton Geotech

Location:Calverton, NYProject No:GTX-11233Boring ID: ---Sample Type: ---Tested By:jefSample ID:---Test Date:10/28/11Checked By:jdt

Depth: --- Sample Id: ---

Moisture Content of Soil - ASTM D 2216-05

Boring ID	Sample ID	Depth	Description	Moisture Content,%
	CA-SAFL- SB01-0102		Moist, dark brown silty sand	17.5
	CA-SAFL- SB01-0203	-	Moist, brownish yellow silty sand	11.7
777	CA-SAFL- SB01-0304		Moist, brownish yellow sand with silt	10.7
	CA-SAFL- SB01-0406		Moist, yellowish brown sand	24
	CA-SAFL- SB01-0608		Moist, yellowish brown sand with silt	22.2
	CA-SAFL- SB01-0810	 -	Moist, brownish yellow sand with gravel	26.5
	CA-SAFL- SB01-1820		Moist, light brown sand	29.3

Notes: Temperature of Drying : 110° Celsius



Client: Tetra Tech NUS, Inc.

Project: NWIRP Calverton Geotech Location: Calverton, NY

Location:Calverton, NYProject No:GTX-11233Boring ID: ---Sample Type: ---Tested By:jefSample ID:---Test Date:10/28/11Checked By:jdt

Depth: --- Sample Id: ---

Moisture Content of Soil - ASTM D 2216-05

Boring ID	Sample ID	Depth	Description	Moisture Content,%
	CA-SAFL- SB02-0103		Moist, olive yellow clayey sand	14.3
** ** ·*	CA-SAFL- SB02-0304		Moist, brownish yellow sand with silt and gravel	11.5
	CA-SAFL- SB02-0406		Moist, brownish yellow sand with silt	30.4
	CA-SAFL- SB02-0608		Moist, brownish yellow sand with silt	18.7
	CA-SAFL- SB02-0810	n	Moist, light yellow sand	21.7
	CA-SAFL- SB02-1820		Moist, light yellowish brown sand	23.2
r: rr an	CA-SAFL- SB02-2325	en en en	Moist, light gray sand with gravel	21.7

Notes: Temperature of Drying: 110° Celsius



Client: Tetra Tech NUS, Inc.
Project: NWIRP Calverton Geotech

Boring ID: ---

Sample ID:---

Project: NWIRP Calverton Geotect
Location: Calverton, NY

Project No: GTX-11233

Sample Type: --- Tested By: jbr

Test Date: 10/24/11 Checked By: jdt

Depth: --- Test Id: 221006

Percent Passing #200 Sieve - ASTM D 1140-00

Boring ID	Sample ID	Depth	Visual Description	Fines, %
	CA-SAFL- SB01-0102	5	Moist, dark brown silty sand	38
	CA-SAFL- SB01-0203		Moist, brownish yellow silty sand	32
	CA-SAFL- SB01-0406		Moist, yellowish brown sand	3.6
	CA-SAFL- SB01-0810		Moist, brownish yellow sand with gravel	1.8
	CA-SAFL- SB01-1820		Moist, light brown sand	2.9
	CA-SAFL- SB02-0103		Moist, olive yellow clayey sand	37.4
	CA-SAFL- SB02-0304		Moist, brownish yellow sand with silt and gravel	. 8
# # · ·	CA-SAFL- SB02-0406		Moist, brownish yellow sand with silt	8.8
	CA-SAFL- SB02-0810		Moist, light yellow sand	1.5
	CA-SAFL- SB02-2325	355	Moist, light gray sand with gravel	1.7



Tetra Tech NUS, Inc. Client:

Project: NWIRP Calverton Geotech

Location: Calverton, NY

Project No: Sample Type: bag Tested By:

jbr

GTX-11233

Sample ID:CA-SAFL-SB01-0304

Test Date: Test Id: 221007

Checked By: jdt 10/24/11

Depth:

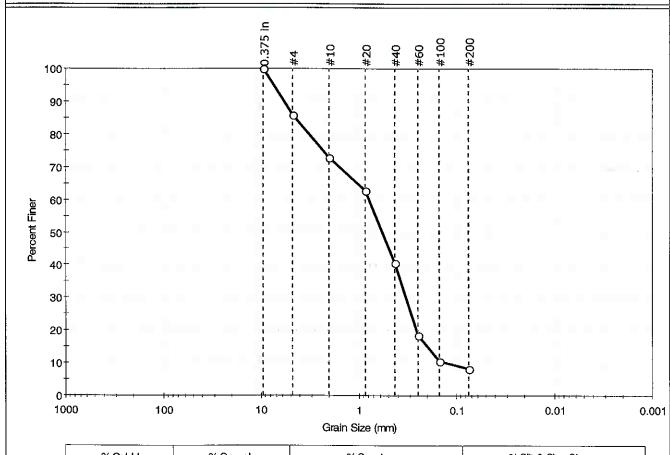
Boring ID: ---

Test Comment:

Sample Description: Moist, brownish yellow sand with silt

Sample Comment:

Particle Size Analysis - ASTM D 422-63 (reapproved 2002)



% Cobble	%Gravel	%Sand	% Silt & Clay Size
	14.1	77.7	8.2

Sieve Name	Sieve Size, mm	Percent Finer	Spec. Percent	Complies
0.375 in	9.50	100		177.70
#4	4.75	86		,
#10	2.00	73		
#20	0.85	63		*****
#40	0.42	41		
#60	0.25	19		
#100	0.15	10		
#200	0.075	8		

<u>Coefficients</u>			
D ₈₅ =4.4817 mm	$D_{30} = 0.3282 \text{ mm}$		
D ₆₀ = 0.7787 mm	$D_{15} = 0.1990 \text{ mm}$		
D ₅₀ = 0.5681 mm	$D_{10} = 0.1301 \text{ mm}$		
Cu =5.985	C _c =1.063		

Classification **ASTM** N/A

<u>AASHTO</u> Stone Fragments, Gravel and Sand (A-1-b(0))

<u>Sample/Test Description</u> Sand/Gravel Particle Shape: ROUNDED

Sand/Gravel Hardness: HARD



Client: Tetra Tech NUS, Inc. Project: **NWIRP Calverton Geotech**

Location: Calverton, NY

Boring ID: ---Sample ID:CA-SAFL-SB01-0608

Sample Type: bag Test Date: 10/24/11

221008

Tested By: jbr

Project No:

GTX-11233

Checked By: jdt

Depth: Test Comment:

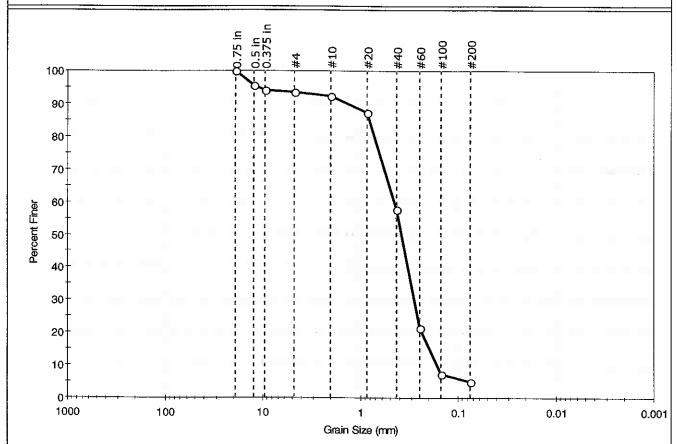
Sample Description:

Moist, yellowish brown sand with silt

Test Id:

Sample Comment:

Particle Size Analysis - ASTM D 422-63 (reapproved 2002)



% Cobble	%Gravel	%Sand	% Silt & Clay Size
	6.3	88.6	5.1

Sieve Name	Sieve Size, mm	Percent Finer	Spec. Percent	Complies
0.75 in	19.00	100		···-
0.5 in	12.50	96		
0.375 in	9.50	94		
#4	4.75	94		
#10	2.00	92		
#20	0.85	87		
#40	0.42	58		
#60	0.25	22		
#100	0.15	7		
#200	0.075	5		

<u>Coefficients</u>			
D ₈₅ =0.8044 mm	$D_{30} = 0.2825 \text{ mm}$		
D ₆₀ = 0.4466 mm	D ₁₅ = 0.1974 mm		
D ₅₀ =0.3786 mm	$D_{10} = 0.1654 \text{ mm}$		
Cu =2.700	$C_c = 1.080$		

Classification **ASTM** N/A AASHTO Fine Sand (A-3 (0))

<u>Sample/Test Description</u> Sand/Gravel Particle Shape: ROUNDED

Sand/Gravel Hardness: HARD



Client: Tetra Tech NUS, Inc. Project: **NWIRP Calverton Geotech**

Location: Calverton, NY

Sample ID:CA-SAFL-SB02-0608

Sample Type: bag

Test Id:

Project No: GTX-11233

Tested By: jbr Test Date: 10/24/11 Checked By: jdt

221009

Depth:

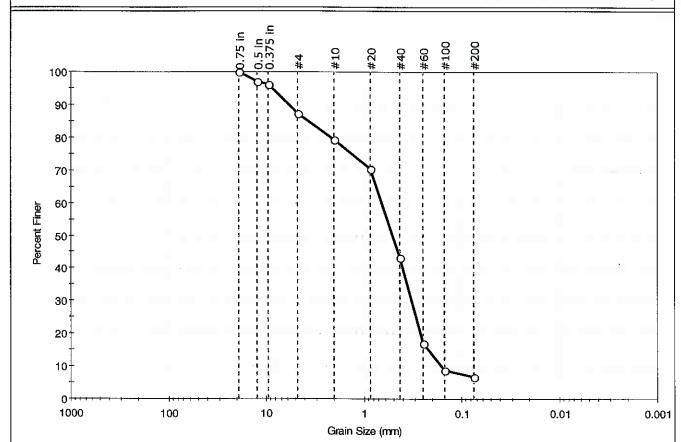
Boring ID: ---

Test Comment:

Sample Description: Moist, brownish yellow sand with silt

Sample Comment:

Particle Size Analysis - ASTM D 422-63 (reapproved 2002)



% Cobble	%Gravel	%Sand	% Silt & Clay Size
	12.7	80.6	6.7

Sieve Name	Sieve Size, mm	Percent Finer	Spec. Percent	Complies
0.75 in	19.00	100		
0.5 in	12.50	97		4.0 V
0.375 in	9.50	96		
#4	4.75	87		· · · · · · · · · · · · · · · · · · ·
#10	2.00	79		.,
#20	0.85	70		
#40	0.42	43		
#60	0.25	17		
#100	0.15	9	<u> </u>	
#200	0.075	7 7		

<u>Coefficients</u>		
D ₈₅ = 3.7141 mm	$D_{30} = 0.3240 \text{ mm}$	
$D_{60} = 0.6510 \text{ mm}$	D ₁₅ =0.2180 mm	
D ₅₀ = 0.5039 mm	$D_{10} = 0.1605 \text{ mm}$	
Cu =4.056	$C_c = 1.005$	

Classification **ASTM** N/A

Stone Fragments, Gravel and Sand (A-1-b(0))

Sample/Test Description
Sand/Gravel Particle Shape: ROUNDED

Sand/Gravel Hardness: HARD



Client: Tetra Tech NUS, Inc.

Project: **NWIRP Calverton Geotech** Location: Calverton, NY

Boring ID: ---

Project No: Tested By:

GTX-11233

Sample ID:CA-SAFL-SB02-1820

Sample Type: bag Test Date:

Test Id:

10/24/11

221010

jbr Checked By: jdt

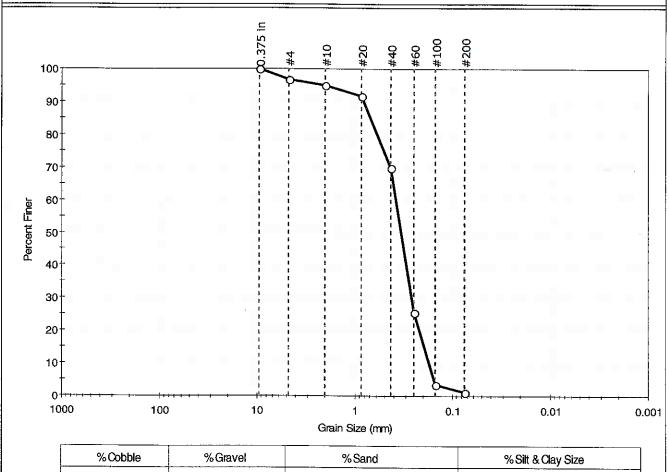
Depth:

Test Comment:

Sample Description: Moist, light yellowish brown sand

Sample Comment:

Particle Size Analysis - ASTM D 422-63 (reapproved 2002)



% Cobble	%Gravel	% Sand	% Silt & Clay Size
	3.3	95.4	1.3

Sieve Name	Sieve Size, mm	Percent Finer	Spec. Percent	Complies
0.375 in	9.50	100	1	
#4	4.75	97		
#10	2.00	95		
#20	0.85	92		····
#40	0.42	70		
#60	0.25	26		
#100	0.15	4		
#200	0.075	1		

<u>Coefficients</u>		
D ₈₅ ≃0.6877 mm	$D_{30} = 0.2637 \text{ mm}$	
D ₆₀ = 0.3779 mm	$D_{15} = 0.1954 \text{ mm}$	
D ₅₀ = 0.3352 mm	$D_{10} = 0.1739 \text{ mm}$	
$C_u = 2.173$	$C_{c} = 1.058$	

<u>Classification</u> Poorly graded sand (SP) <u>ASTM</u>

AASHTO Fine Sand (A-3 (0))

Sample/Test Description
Sand/Gravel Particle Shape: ---

Sand/Gravel Hardness: ---



Client: Tetra Tech NUS, Inc. **NWIRP Calverton Geotech** Project:

Location: Calverton, NY

Sample ID:CA-SAFL- SB02-0103

Project No: Sample Type: bag Tested By: Test Date: Checked By: jdt 10/26/11

GTX-11233

cam

Test Id: 221011

Test Comment:

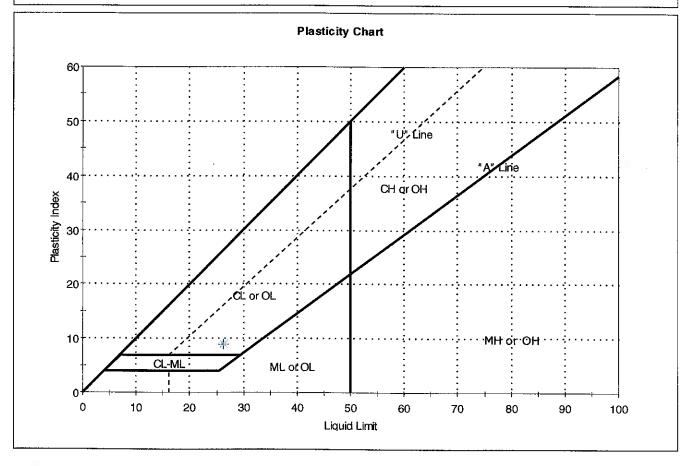
Boring ID: ---

Depth:

Sample Description: Moist, olive yellow clayey sand

Sample Comment:

Atterberg Limits - ASTM D 4318-05



Symbol	Sample ID	Boring	Depth	Natural Moisture Content,%	Liquid Limit	Plastic Limit	Plasticity Index	Liquidity Index	Soil Classification
**	CA-SAFL- SB02-0103			14	26	17	9	0	

Sample Prepared using the WET method

Dry Strength: HIGH Dilentancy: RAPID Toughness: LOW

CHAIN OF CUSTODY

(2)

11

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GeoTesting Express, Inc. 125 Nagog Park Acton, MA 01720 800-434-1062 Toll Free

978-635-0424 Phone

Sales Order No.:

Turn-Around Time Requested: Comments 978-635-0266 Fax Analysis Date: 101 Time: Elipa Tropics GTX No.: X X × × メ X X Container Type X Received By: 1. Bucket 4. Tube 2. Bag 3. Jar 5. Roll X 2. Geosynthetic Sample Type Sample 4. Concrete Type 10/18/11 4 3. Rock 5. Other Time: 1660 1. Soil T. C. C. Date: 2/2/2/2 1327 234 83, Size Type Date Time 44 B Ž, B iddress: 5700 fake Wrightor, Suite 309 Sampling roject Name: NWIRP Calverton Geotech Company Name: Letter Tech NULS roject Location: Calverton, NF hone Number: 757-466-4904 iontact: Robert Suk -mail: Pobsok@ totactech, com Container 4 roject Number: 11 2603750 14-54FL-5861-0102 241 1-54FL-5802-0304 elinquished By: 4-SAFL-5861-0303 A-SAFL-5801-0304 9-5/HEL-5801-1820 4-59-163-0163 9-54FL-5851-0816 A-5461-5801-0406 4-54FL 5801-0608 Identification Sample ax Number:

No. of Business Days:

Date:
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Received By:

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CHAIN OF CUSTODY

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GeoTesting Express, Inc. 125 Nagog Park Acton, MA 01720

800-434-1062 Toll Free 978-635-0424 Phone 978-635-0266 Fax

978-635-0266 Fax			\	\ \ \	\		\		Comments									Turn-Around Time Requested:	No. of Business Days:	Special Instructions:		
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WARRANTY and LIABILITY

GeoTesting Express (GTX) warrants that all tests it performs are run in general accordance with the specified test procedures and accepted industry practice. GTX will correct or repeat any test that does not comply with this warranty. GTX has no specific knowledge as to conditioning, origin, sampling procedure or intended use of the material.

GTX may report engineering parameters that require us to interpret the test data. Such parameters are determined using accepted engineering procedures. However, GTX does not warrant that these parameters accurately reflect the true engineering properties of the *in situ* material. Responsibility for interpretation and use of the test data and these parameters for engineering and/or construction purposes rests solely with the user and not with GTX or any of its employees.

GTX's liability will be limited to correcting or repeating a test which fails our warranty. GTX's liability for damages to the Purchaser of testing services for any cause whatsoever shall be limited to the amount GTX received for the testing services. GTX will not be liable for any damages, or for any lost benefits or other consequential damages resulting from the use of these test results, even if GTX has been advised of the possibility of such damages. GTX will not be responsible for any liability of the Purchaser to any third party.

Commonly Used Symbols

A	pore pressure parameter for $\Delta \sigma_1 - \Delta \sigma_3$	T	temperature
В	pore pressure parameter for Δσ ₃	ť	time
CIU	isotropically consolidated undrained triaxial shear test	u, uc	unconfined compression test
CR	compression ratio for one dimensional consolidation	UU, Q	unconsolidated undrained triaxial test
C_c	coefficient of curvature, $(D_{30})^2/(D_{10} \times D_{60})$		
$C_{\mathbf{u}}$	coefficient of uniformity, D ₆₀ /D ₁₀	u _a	pore gas pressure
C _c	compression index for one dimensional consolidation	u _e	excess pore water pressure
C_{α}	coefficient of secondary compression	u, u _w	pore water pressure
C _v	coefficient of consolidation	V	total volume
C	cohesion intercept for total stresses	\mathbf{v}_{g}	volume of gas
c'	cohesion intercept for effective stresses	V_s	volume of solids
D	diameter of specimen	$\mathbf{v}_{\mathbf{v}}$	volume of voids
\mathbf{D}_{10}	diameter at which 10% of soil is finer	$\mathbf{V}_{\mathbf{w}}$	volume of water
	diameter at which 15% of soil is finer	V_{o}	initial volume
D ₁₅		v	velocity
D_{30}	diameter at which 30% of soil is finer	\mathbf{w}	total weight
D_{50}	diameter at which 50% of soil is finer	\mathbf{W}_{s}	weight of solids
D_{60}	diameter at which 60% of soil is finer	$\mathbf{W_w}$	weight of water
D_{85}	diameter at which 85% of soil is finer	w	water content
d ₅₀	displacement for 50% consolidation	w_c	water content at consolidation
d ₉₀	displacement for 90% consolidation	$\mathbf{w_f}$	final water content
d_{100}	displacement for 100% consolidation	Wı	liquid limit
E	Young's modulus	Wn	natural water content
e	void ratio	W_p	plastic limit
ec	void ratio after consolidation	W_s	shrinkage limit
e _o	initial void ratio	Wo, Wi	initial water content
G	shear modulus	α	slope of q _f versus p _f
G_s	specific gravity of soil particles	α,	slope of qf versus pf'
H	height of specimen	Υt	total unit weight
PΙ	plasticity index	γα	dry unit weight
i	gradient	γ̈́s	unit weight of solids
K_o	lateral stress ratio for one dimensional strain	γ̈́w	unit weight of water
k	permeability	°°	strain
LI	Liquidity Index	ε _{vol}	volume strain
$\mathbf{m}_{\mathbf{v}}$	coefficient of volume change	ε _h , ε _ν	horizontal strain, vertical strain
n	porosity	μ	Poisson's ratio, also viscosity
PΙ	plasticity index	Q.	normal stress
P_c	preconsolidation pressure	e,	effective normal stress
p	$(\sigma_1 + \sigma_3)/2$, $(\sigma_v + \sigma_h)/2$	σ _α , σ' _ε	consolidation stress in isotropic stress system
p'	$(\sigma'_1 + \sigma'_3)/2$, $(\sigma'_v + \sigma'_h)/2$		horizontal normal stress
p'e	p' at consolidation	σ _h , σ' _h	vertical normal stress
Q	quantity of flow	σ _ν , σ' _ν	
q	$(\sigma_1.\sigma_3)/2$	σ 1	major principal stress
q_f	q at failure	თ 2	intermediate principal stress
q _o , q _i	initial q	♂ 3	minor principal stress
	q at consolidation	τ	shear stress
q _c S	degree of saturation	φ,	friction angle based on total stresses
SL	shrinkage limit	φ',	friction angle based on effective stresses
	undrained shear strength	ϕ_r	residual friction angle
Su T	<u> </u>	ϕ_{ult}	φ for ultimate strength -
T	time factor for consolidation		



